RECEIVE

7-23 2013



EPA REGION 6 ENFORCEMENT DIVISION Air/Toxics & Inspection Goordination Branch

6EN-A

				OCIA-Y
FRS #:	110000460901			
Media #:	48-201-00037	***************************************		
Permit #:	O-3049			
Inspection Type:	Clean Air Act, Partial C	Compl	iance Evaluation	
Inspection Date:	4/22-24/13			
Company Name:	RHODIA INC.			
Facility Name:	RHODIA, HOUSTON I	PLAN	T	
Physical Location:	8615 Manchester Street			
Mailing Address:	Houston, Texas 77012 8615 Manchester Street Houston, Texas 777012			
County/Parish:	Harris County			
SIC Code:	2819			
NAICS Code:	211112			
Reg. Programs:	RMP & 112(r)			
Facility Representatives:	Floyd Dickerson		Environmental Manager	(713) 924-1408
	William McConnell		Plant Manager	(713) 924-1484
	Jim Cesen		Operations Manager	(713) 924-1433
EPA Inspectors:	Sherronda Martin- 6EN Phelps	N-AS	Environmental Engineer	(281) 983-2122
State Inspectors:	N/A			
EPA Lead Inspector Signature/Date:	Sheuondu Main	liw-	Phelyn	7/16/13
The state of the s	Sherronda Martin-Phelps, E	inviron	mental Engineer	Date
Peer Reviewer Signature/Date:	Caclo BFU	2	\supset	7/23/13
	Carlos Flores, Life Scientis	<u>t</u>		Date
Supervisor Signature/Date:	Samuel 1sts	<u> </u>		7/23/2013
	Samuel Tates, Section Chie	I Air S	urveillance	Date



Section I - INTRODUCTION

PURPOSE OF THE INSPECTION

One of the goals of the U.S. Environmental Protection Agency (EPA) is to protect the public and the environment from exposure to extremely hazardous chemicals. A Risk Management Plan (RMP) inspection was conducted at Rhodia-Houston Plant (Rhodia) from April 22-24, 2013 to achieve this goal. The objectives of this inspection included working with the facility (both management and employees) to improve their chemical safety management program and to determine their compliance with the Clean Air Act (CAA) Section 112(r) and 40 C.F.R. Part 68 – Chemical Accident Prevention Provisions. EPA Region 6 selected Rhodia for inspection due to the amount of flammable and toxic substances at the facility, the number of people residing within the worst case scenario endpoints, and the facility's accident history.

I arrived at Rhodia at 9:30 am on April 22, 2013. I met with Floyd Dickerson (Environmental Manager), William McConnel (Plant Manager), and Jim Cesen (Operations Manager). I presented my credentials to William McConnell, who is responsible for 40 C.F.R. Part 68 implementation and informed him that this was an EPA inspection to evaluate compliance with the CAA Section 112(r) and 40 C.F.R. Part 68. Rhodia does not have union representation onsite.

FACILITY DESCRIPTION

Rhodia is owned by its parent company, Rhodia Inc., which operates a sulfuric acid manufacturing plant in Houston, Harris County, Texas. Rhodia is a major producer of sulfuric acid with production estimates of about 2,600 tons per day. The production of sulfuric acid occurs by two processes: combusting elemental sulfur and regenerating spent sulfuric acid. Rhodia is also a producer of liquid sulfur dioxide and commercially incinerates liquid hazardous wastes. The Houston Plant currently operates under Air Operating Permit No. O-3049.

Section II - OBSERVATIONS

This inspection concentrated on the following units: Regeneration 2, Unit No. 8, and Logistics. General Process Overviews and the corresponding Process Flow Diagrams have been provided for each of these units (Attachment 1).

40 C.F.R. § 68.10 Applicability

As reported in their November 8, 2012 RMP submittal (**Attachment 2**), Rhodia is a stationary source that handles or stores more than a threshold quantity of the following regulated substances: oleum, sulfur trioxide, carbon disulfide, vinyl acetate, toluene di-isocynate, propionitrile, acrylonitrile, methyl mercaptan, ethyl mercaptan, acetaldehyde, allyl alcohol, propylene oxide, hydrazine, hydrogen sulfide, isopropylamine, 1-butene, propylene, cis butene-2, trans butene-2, isobutylene, 1,3 butadiene, isopentane, ethyl chloride, dimethylamine, ethylamine, methylamine, trimethylamine, and propane in a process. Therefore, 40 C.F.R. Part 68 – Chemical Accident Prevention Provisions are applicable to Rhodia.

40 C.F.R. § 68.12 General Requirements

Rhodia has submitted a single RMP that reflects five (5) covered processes, which are subject to the Program 3 Prevention Program requirements. For these processes, Rhodia is required to do the following: develop and implement a management system, conduct a hazard assessment, implement the prevention requirements of 40 C.F.R. § 68.65 through § 68.87, develop and implement an emergency response program, and submit the data elements required by 40 C.F.R. § 68.175 in their RMP (Attachment 2).

40 C.F.R. § 68.15 Management

As required by 40 C.F.R. § 68.15(c), "when responsibility for implementing individual requirements of this part is assigned to persons other than the person identified under paragraph (b) of this section, the names or positions of these people shall be documented and the lines of authority defined through an organization chart or similar document." See **Attachment 3** for a copy of this information.

Subpart B - Hazard Assessment

Rhodia operates five (5) processes that meet the criteria of Program 3 Prevention Program. At this program level, certain Offsite Consequence Analyses are to be conducted. Rhodia uses several regulated flammable and toxic substances. For these substances, one (1) worst-case scenario and at least one (1) alternative scenario should be analyzed and reported in their RMP for both flammable and toxic substances. This information was provided by the facility in the RMP (Attachment 2).

Subpart D - Program 3 Prevention Program

40 C.F.R. § 68.65 Process Safety Information

I reviewed documentation of this information at Rhodia.

40 C.F.R. § 68.67 Process Hazard Analysis

I requested the corresponding Process Hazard Analyses (PHAs) for the following units: Regeneration 2, Unit No. 8, and Logistics. Rhodia revalidated all the PHAs for the units in question within at least five (5) years, as required by the RMP.

40 C.F.R. § 68.69 Operating Procedures

According to 40 C.F.R. § 68.69(c), "The operating procedures shall be reviewed as often as necessary to assure that they reflect current operating practice, including changes that result from

changes in process chemicals, technology, and equipment, and changes to stationary sources. The owner or operator shall certify annually that these operating procedures are current and accurate."

During the inspection, I reviewed the operating procedures for the following units: Regeneration 2, Unit No. 8, and Logistics. For the units in question, the last five (5) years of annual certifications were requested. For Regeneration 2, the only annual certifications that were provided were from 2009 through 2012. For Unit No. 8, the only annual certification that was provided was from 2012. For Logistics, the only annual certifications that were provided were from 2008 through 2012. See Attachment 4 for a copy of the annual certifications provided by Rhodia.

According to 40 C.F.R. § 68.69(a)(3), "The owner or operator shall develop and implement written operating procedures that provide clear instructions for safely conducting activities involved in each covered process consistent with the process safety information and shall address at least the following elements: ... (3) Safety and health considerations: (i) Properties of, and hazards presented by, the chemicals used in the process; (ii) Precautions necessary to prevent exposure, including engineering controls, administrative controls, and personal protective equipment; (iii) Control measures to be taken if physical contact or airborne exposure occurs; (iv) Quality control for raw materials and control of hazardous chemical inventory levels; and, (v) Any special or unique hazards."

During the inspection, I reviewed operating procedures for the units in question. Of the procedures reviewed, it appears these units all lacked information regarding the following Safety and health considerations: (iii) Control measures to be taken if physical contact or airborne exposure occurs; (iv) Quality control for raw materials and control of hazardous chemical inventory levels; and, (v) Any special or unique hazards. When asked about this particular information the Personal Protective Equipment (PPE) Matrix was referenced; however, after reviewing the PPE Matrix, it failed to address the specific considerations mentioned above. Rhodia then explained that this information could be found in the General Plant Safety Rules, which were not referenced in the operating procedures. I recommended that Rhodia consider linking these documents for easier accessability. See **Attachment 4** for a copy of the PPE Matrix and the operating procedures provided for Regeneration 2, Unit No. 8, and Logistics.

40 C.F.R. § 68.71 Training

According to 40 C.F.R. § 68.71(c), "The owner or operator shall ascertain that each employee involved in operating a process has received and understood the training required by this paragraph. The owner or operator shall prepare a record which contains the identity of the employee, the date of training, and the means used to verify that the employee understood the training."

During the inspection, I reviewed the training records provided for operators in Regeneration 2, Unit No. 8, and Logistics. From the information provided, it appears that refresher training may have not been conducted in all the units in question. The documentation provided lacks the information to determine whether each entry is an initial training or a refresher training. No

historical records were provided to show refresher training was given prior to the dates shown on the documents. Likewise, the means used to verify that the employees understood the training has no consistency. Some entries noted a number grade and others entries simply circled Pass or Fail. See **Attachment 5** for the operator training records.

40 C.F.R. § 68.73 Mechanical Integrity

I requested the mechanical integrity inspection records for both fixed and rotating equipment for the units in question: Regeneration 2, Unit No. 8, and Logistics. Random components were selected and the corresponding inspection documents were reviewed.

40 C.F.R. § 68.75 Management of Change

I reviewed documentation of this process and how it is implemented at the Rhodia.

40 C.F.R. § 68.77 Pre-startup Review

I reviewed documentation of this process and how it is implemented at the Rhodia.

40 C.F.R. § 68.79 Compliance Audits

Rhodia has completed a compliance audit at least once every three years. I was provided with compliance audits for 2009 and 2012. See **Attachment 6** for copies of these documents.

40 C.F.R. § 68.81 Incident Investigations

Two (2) incident investigations were conducted for incidents reported in the accident history of the RMP, which occurred on November 29, 2008 and June 9, 2012. I reviewed the documentation for both incidents.

40 C.F.R. § 68.83 Employee Participation

I reviewed the documentation of this process and how it is implemented at Rhodia.

40 C.F.R. § 68.85 Hot Work Permits

I reviewed hot work permits from different operating areas in the units in question to check for accuracy and detail on the jobs being conducted. Hot work permits are kept for seven (7) days after the job is completed. Monthly audits of the hot work permits are conducted thereafter. See **Attachment 8** for copies of the hot work permits.

40 C.F.R. § 68.87 Contractors

I reviewed documentation of this process and how it is implemented at Rhodia.

Subpart E - Emergency Response

I reviewed records for the Emergency Response Plan in place at Rhodia. James Shaw, Safety Specialist, provided me with information regarding the Emergency Response Plan in place at Rhodia. Based on the information provided, it appears that Rhodia personnel are informed of the plan and what steps to take in such an instance. Training records for several personnel were reviewed and the records provided were current. Inspection records for selected components were reviewed and the records provided were current.

Subpart G - Risk Management Plan

40 C.F.R. § 68.150 Submission

Rhodia submitted a single RMP on November 8, 2012, which included the majority of the information required in 40 C.F.R. § 68.150 (Attachment 2).

40 C.F.R. § 68.195 Required Corrections

40 C.F.R. § 68.195(b) requires within one (1) month of any change in the emergency contact information required under 40 C.F.R. § 68.160(b)(6), the owner or operator shall submit a correction of that information. No changes to the emergency contact information were observed at Rhodia that required an update of the RMP.

Title V Deviation Reporting

During the inspection, Title V deviation reporting was discussed. The findings in the RMP Audits or potential 40 C.F.R. Part 68 deviations were not reported in the deviation reports. Rhodia has plans to implement such reporting in the future.

Closing

A closing conference was held on April 24, 2013. I presented the areas of concern discovered during my inspection. The Rhodia employees that were present can be found in **Attachment 7**.

Section III – AREAS OF CONCERN

The following areas of concern were discovered during my inspection and discussed with the Rhodia employees during the closing conference:

1. According to 40 C.F.R. § 68.15(c), "When responsibility for implementing individual requirements of this part is assigned to persons other than the person identified under paragraph (b) of this section, the names or positions of these people shall be documented and the lines of authority defined through an organization chart or similar document."

Based of my review of the information in **Attachment 3**, it appears that Rhodia may not be in compliance with 40 C.F.R. § 68.15(c).

- 2. According to 40 C.F.R. § 68.69(c), "The operating procedures shall be reviewed as often as necessary to assure that they reflect current operating practice, including changes that result from changes in process chemicals, technology, and equipment, and changes to stationary sources. The owner or operator shall certify annually that these operating procedures are current and accurate." Based on my review of the information in **Attachment 4**, it appears that Rhodia may not be in compliance with 40 C.F.R. § 68.69(c).
- 3. According to 40 C.F.R. § 68.69(a)(3), "The owner or operator shall develop and implement written operating procedures that provide clear instructions for safely conducting activities involved in each covered process consistent with the process safety information and shall address at least the following elements. Safety and health considerations: Properties of, and hazards presented by, the chemicals used in the process; Precautions necessary to prevent exposure, including engineering controls, administrative controls, and personal protective equipment; Control measures to be taken if physical contact or airborne exposure occurs; Quality control for raw materials and control of hazardous chemical inventory levels; and, Any special or unique hazards." Based on my review of the information in **Attachment 4**, it appears that Rhodia may not be in compliance with 40 C.F.R §68.69(a)(3).
- 4. According to 40 C.F.R. § 68.71(c), "The owner or operator shall ascertain that each employee involved in operating a process has received and understood the training required by this paragraph. The owner or operator shall prepare a record which contains the identity of the employee, the date of training, and the means used to verify that the employee understood the training." Based on my review of the information in **Attachment 5**, it appears that Rhodia may not be in compliance with 40 C.F.R § 68.71(c).

Section III – ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5. Operator Training Records
- 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

RN	RMP Program Level 3 Process Checklist Facility Name: Rhodia – Houston Plant			
Sec	ction A – Management [68.15]			
Management system developed and implemented as provided in 40 CFR 68.15?		ЭМ	U	□n/a
Has	the owner or operator:			
1.	Developed a management system to oversee the implementation of the risk management program elements? [68.15(a)]	□Y	ΠN	□N/A
2.	Assigned a qualified person or position that has the overall responsibility for the development, implementation, and integration of the risk management program elements? [68.15(b)] George Baran	ΠY	ΠN	□N/A
3.	Documented other persons responsible for implementing individual requirements of the risk management program and defined the lines of authority through an organization chart or similar document? [68.15(c)] An organizational chart is in place but as to defining specific lines of authority and their responsibilities with implementing the RMP has not been created nor was presented. Rhodia should look into creating such a document.	ПΥ	N	□N/A
Sec	ction B: Hazard Assessment [68.20-68.42]			
	rard assessment conducted and documented as provided in 40 CFR 68.20-68.42?	ЭМ	□U	□N/A
Ha	zard Assessment: Offsite consequence analysis parameters [68.22]			
1.	Used the following endpoints for offsite consequence analysis for a worst-case scenario: [68.22(a)]	Y	ΠN	□N/A
	For toxics: the endpoints provided in Appendix A of 40 CFR Part 68? [68.22(a)(1)]			
	For flammables: an explosion resulting in an overpressure of 1 psi? [68.22(a)(2)(i)]; or			
	☐ For flammables: a fire resulting in a radiant heat/exposure of 5 kw/m² for 40 seconds? [68.22(a)(2)(ii)]			
	For flammables: a concentration resulting in a lower flammability limit, as provided in NFPA documents or other generally recognized sources? [68.22(a)(2)(iii)]			
2.	Used the following endpoints for offsite consequence analysis for an alternative release scenario: [68.22(a)]	Y	$\square N$	□N/A
	For toxics: the endpoints provided in Appendix A of 40 CFR Part 68? [68.22(a)(1)]			
	For flammables: an explosion resulting in an overpressure of 1 psi? [68.22(a)(2)(i)]			
	For flammables: a fire resulting in a radiant heat/exposure of 5 kw/m² for 40 seconds? [68.22(a)(2)(ii)]			
	For flammables: a concentration resulting in a lower flammability limit, as provided in NFPA documents or other generally recognized sources? [68.22(a)(2)(iii)]			
3.	Used appropriate wind speeds and stability classes for the release analysis? [68.22(b)]	Y	ΠN	□N/A
4.	Used appropriate ambient temperature and humidity values for the release analysis? [68.22(c)]	Y	ΠN	□N/A
5.	Used appropriate values for the height of the release for the release analysis? [68.22(d)]	Y	□N	□N/A
6.	Used appropriate surface roughness values for the release analysis? [68.22(e)]	Y	ΠN	□N/A
7.	Do tables and models, used for dispersion analysis of toxic substances, appropriately account for dense or neutrally buoyant gases? [68.22(f)]	Y	ΠN	□N/A
8.	Were liquids, other than gases liquefied by refrigeration only, considered to be released at the highest daily maximum temperature, based on data for the previous three years appropriate for a stationary source, or at process temperature, whichever is higher? [68.22(g)]	M Y	□N	□N/A

RMP Program Level 3 Process Checklist Facility Name: Rhodi		ia – F	lousto	n Plant
Hazar	d Assessment: Worst-case release scenario analysis [68.25]			
en	nalyzed and reported in the RMP one worst-case release scenario estimated to create the greatest distance to an dpoint resulting from an accidental release of a regulated toxic substance from covered processes under worst-case nditions? [68.25(a)(2)(i)]	Y	ΠN	□N/A
en	nalyzed and reported in the RMP one worst-case release scenario estimated to create the greatest distance to an dpoint resulting from an accidental release of a regulated flammable substance from covered processes under worst-se conditions? [68.25(a)(2)(ii)]	Y	ΠN	□N/A
fro po	Analyzed and reported in the RMP additional worst-case release scenarios for a hazard class if the worst-case release from another covered process at the stationary source potentially affects public receptors different from those potentially affected by the worst-case release scenario developed under 68.25(a)(2)(i) or 68.25(a)(2)(ii)? [68.25(a)(2)(iii)]		ΠN	N/A
12. Ha	as the owner or operator determined the worst-case release quantity to be the greater of the following: [68.25(b)]	Y	□и	□N/A
	If released from a vessel, the greatest amount held in a single vessel, taking into account administrative controls that limit the maximum quantity? [68.25(b)(1)]			
	If released from a pipe, the greatest amount held in the pipe, taking into account administrative controls that limit the maximum quantity? [68.25(b)(2)]			
13.a.	Has the owner or operator for toxic substances that are normally gases at ambient temperature and handled as a gas of	or liquic	l under	pressure:
13.a.(1)	Assumed the whole quantity in the vessel or pipe would be released as a gas over 10 minutes? [68.25(c)(1)]	ΠY	ΠN	N/A
13.a.(2)	Assumed the release rate to be the total quantity divided by 10, if there are no passive mitigation systems in place? [68.25(c)(1)]	Шγ	ΠN	N/A
13.b.	Has the owner or operator for toxic gases handled as refrigerated liquids at ambient pressure:			
13.b.(1	Assumed the substance would be released as a gas in 10 minutes, if not contained by passive mitigation systems or if the contained pool would have a depth of 1 cm or less? [68.25(c)(2)(i)]	ΩY	□N	N/A
13.b.(2) If released substance would be contained by passive mitigation systems in a pool with a depth > 1 cm;	ΠY	ΠN	N/A
	Assumed the quantity in the vessel or pipe (as determined per 68.25(b)) would be spilled instantaneously to form a liquid pool? [68.25(c)(2)(ii)]			
	Calculated the volatility rate at the boiling point of the substance and at the conditions specified in 68.25(d)? [68.25(c)(2)(ii)]			
13.c.	Has the owner or operator for toxic substances that are normally liquids at ambient temperature:			
13.c.(1)	Assumed the quantity in the vessel or pipe would be spilled instantaneously to form a liquid pool? [68.25(d)(1)]	Y	□N	□N/A
13.c.(2)	Determined the surface area of the pool by assuming that the liquid spreads to 1 cm deep, if there is no passive mitigation system in place that would serve to contain the spill and limit the surface area, or if passive mitigation is in place, was the surface area of the contained liquid used to calculate the volatilization rate? [68.25(d)(1)(i)]	Y	ΠN	□N/A
13.c.(3)	Taken into account the actual surface characteristics, if the release would occur onto a surface that is not paved or smooth? [68.25(d)(1)(ii)]	Y	□N	□N/A
13.c.(4)	Determined the volatilization rate by accounting for the highest daily maximum temperature in the past three years, the temperature of the substance in the vessel, and the concentration of the substance if the liquid spilled is a mixture or solution? [68.25(d)(2)]	Y	□N	□N/A
13.c.(5)	Determined the rate of release to air from the volatilization rate of the liquid pool? [68.25(d)(3)]	Υ	ΠN	□N/A

RMP Program Level 3 Process Checklist Facility Name: Rhodia – I	m, 0 0 m 0 0	n Plant
13.c.(6) Determined the rate of release to air by using the methodology in the RMP Offsite Consequence Analysis Guidance, any other publicly available techniques that account for the modeling conditions and are recognized by industry as applicable as part of current practices, or proprietary models that account for the modeling conditions may be used provided the owner or operator allows the implementing agency access to the model and describes model features and differences from publicly available models to local emergency planners upon request? [68.25(d)(3)]	□N	□N/A
What modeling technique did the owner or operator use? [68.25(g)] EPA RMP COMP		
13.d. Has the owner or operator for <u>flammables</u> :		
13.d.(1) Assumed the quantity in a vessel(s) of flammable gas held as a gas or liquid under pressure or refrigerated gas released to an undiked area vaporizes resulting in a vapor cloud explosion? [68.25(e)]	ΠN	□N/A
13.d.(2) For refrigerated gas released to a contained area or liquids released below their atmospheric boiling point, assumed the quantity volatilized in 10 minutes results in a vapor cloud? [68.25(f)]	ΠN	M/A
13.d.(3) Assumed a yield factor of 10% of the available energy is released in the explosion for determining the distance to the explosion endpoint, if the model used is based on TNT-equivalent methods? [68.25(e)]	ΠN	□N/A
14. Used the parameters defined in 68.22 to determine distance to the endpoints? [68.25(g)]	□N	□N/A
15. Determined the rate of release to air by using the methodology in the RMP Offsite Consequence Analysis Guidance, any other publicly available techniques that account for the modeling conditions and are recognized by industry as applicable as part of current practices, or proprietary models that account for the modeling conditions may be used provided the owner or operator allows the implementing agency access to the model and describes model features and differences from publicly available models to local emergency planners upon request? [68.25(g)]	□N	□N/A
What modeling technique did the owner or operator use? [68.25(g)] RMP COMP		
16. Ensured that the passive mitigation system, if considered, is capable of withstanding the release event triggering the scenario and will still function as intended? [68.25(h)] □Y	□N	N/A
17. Considered also the following factors in selecting the worst-case release scenarios: [68.25(i)]	$\square N$	□N/A
Smaller quantities handled at higher process temperature or pressure? [68.25(i)(1)]		
☐ Proximity to the boundary of the stationary source? [68.25(i)(2)]		
Hazard Assessment: Alternative release scenario analysis [68.28]		
18. Identified and analyzed at least one alternative release scenario for each regulated toxic substance held in a covered process(es) and at least one alternative release scenario to represent all flammable substances held in covered processes? [68.28(a)]	ΠN	□N/A
19. Selected a scenario: [68.28(b)]	\square N	□N/A
That is more likely to occur than the worst-case release scenario under 68.25? [68.28(b)(1)(i)]		
☐ That will reach an endpoint off-site, unless no such scenario exists? [68.28(b)(1)(ii)]		
20. Considered release scenarios which included, but are not limited to, the following: [68.28(b)(2)]	\square N	□N/A
Transfer hose releases due to splits or sudden hose uncoupling? [68.28(b)(2)(i)]		
Process piping releases from failures at flanges, joints, welds, valves and valve seals, and drains or bleeds? [68.28(b)(2)(ii)]		
Process vessel or pump releases due to cracks, seal failure, or drain, bleed, or plug failure? [68.28(b)(2)(iii)]		
Vessel overfilling and spill, or overpressurization and venting through relief valves or rupture disks? [68.28(b)(2)(iv)]		
Shipping container mishandling and breakage or puncturing leading to a spill? [68.28(b)(2)(v)]		

21. Used the parameters defined in 68.22 to determine distance to the endpoints? [68.28(c)] September Septem	RN	MP Program Level 3 Process Checklist Facility Name: Rho	dia – I	<u> Ioustc</u>	n Plant
any other publicly available lechniques that account for the modeling conditions and are recognized by industry as applicable as part occurred practices, or proprietary model that account for the modeling conditions may be used and describes model features and differences from publicly available models to local emergency planuters upon request? (88.28(c)) 23. Ensured that the passive and active midigation systems, if considered, are capable of withstanding the release event triggering the scenario and will be functional? [68.28(d)] 24. Considered the following factors in selecting the alternative release scenarios: [68.28(e)] 25. Estimated population that would be included in the distance to the endpoint in the RMP based on a circle with the point of riclease at the center? [68.30(a)] 26. Identified the presence of institutions, parks and recreational areas, major commercial, office, and industrial buildings [av] [av] [bv] [bv] [bv] [bv] [bv] [bv] [bv] [b	21.	Used the parameters defined in 68.22 to determine distance to the endpoints? [68.28(c)]	Y	□N	□n/a
23. Ensured that the passive and active mitigation systems, if considered, are capable of withstanding the release event if geging the scenario and will be functional? (68.28(d)) 24. Considered the following factors in selecting the lateral (68.28(e)) 25. Estimated population that would be included in the distance to the endpoint in the RMP based on a circle with the point of release at the center? (68.30(a)) 26. Identified the presence of institutions, parks and recreational areas, major commercial, office, and industrial buildings in the RMP (68.30(s)) 27. Used most recent Census data, or other updated information to estimate the population? (68.30(c)) 28. Estimated the population to two significant digits? (68.30(d)) 29. Identified environmental receptors that would be included in the distance to the endpoint based on a circle with the interpretation of the control of t	22.	any other publicly available techniques that account for the modeling conditions and are recognized by industry as applicable as part of current practices, or proprietary models that account for the modeling conditions may be used provided the owner or operator allows the implementing agency access to the model and describes model features and differences from publicly available models to local emergency planners upon request? [68.28(c)]	Y	□N	□N/A
triggering the scenario and will be functional? [68.28(d)] 24. Considered the following factors in selecting the alternative release scenarios: [68.28(e)] The five-year accident history provided in 68.42? [68.28(e)(1)] Failure scenarios identified under 68.50? [68.28(e)(2)] Failure scenarios identified under 68.50? [68.28(e)(2)] 25. Estimated population that would be included in the distance to the endpoint in the RMP based on a circle with thre point of release at the center? [68.30(a)] 26. Identified the presence of institutions, parks and recreational areas, major commercial, office, and industrial buildings in the RMP? [68.30(a)] 27. Used most recent Census data, or other updated information to estimate the population? [68.30(c)] 28. Estimated the population to two significant digits? [68.30(d)] 29. Identified convironmental receptors that would be included in the distance to the endpoint based on a circle with the population of release at the center? [68.33(a)] 30. Relied on information provided on local U.S.G.S. maps, or on any data source containing U.S.G.S. data to identify point of release at the center? [68.33(a)] 31. Reviewed and update [68.36] 31. Reviewed and update (68.36) 31. Reviewed and update the off-site consequence analyses at least once every five years? [68.36(a)] 32. Completed a revised analysis and submit a revised RMP within six months of a change in processes, quantities store or handled, or any other aspect that might reasonably be expected to increase or decrease the distance to the endpoin by a factor of two or more? [68.36(b)] 33. For worst-case scenarios: a description of the vessel or pipeline and substance selected, assumptions and parameters used, the release quantity and rate? [68.39(a)] 34. Por oldernative release scenarios: a description of the scenarios identified, assumptions and parameters used, the rationale for selection, and anticipated effect of the administrative controls and parameters used, the rationale for selection, and anticipated effect of the adm			P		
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33. For worst-case scenarios: a description of the vessel or pipeline and substance selected, assumptions and parameters used, the rationale for selection, and anticipated effect of the administrative controls and passive mitigation on the release quantity and rate? [68.39(a)] 34. For alternative release scenarios: a description of the scenarios identified, assumptions and parameters used, the rationale for the selection of specific scenarios, and anticipated effect of the administrative controls and mitigation on the release quantity and rate? [68.39(b)] 35. Documentation of estimated quantity released, release rate, and duration of release? [68.39(c)] 36. Methodology used to determine distance to endpoints? [68.39(d)]	32.	or handled, or any other aspect that might reasonably be expected to increase or decrease the distance to the endpoint	Y	□N	□N/A
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36. Methodology used to determine distance to endpoints? [68.39(d)] ■Y □N □N/A	34.	rationale for the selection of specific scenarios, and anticipated effect of the administrative controls and mitigation on	Y	ΠN	□N/A
	35.	Documentation of estimated quantity released, release rate, and duration of release? [68.39(c)]	Y	□N	□N/A
37. Data used to estimate population and environmental receptors potentially affected? [68.39(e)]	36.	Methodology used to determine distance to endpoints? [68.39(d)]	Y	□N	□N/A
	37.	Data used to estimate population and environmental receptors potentially affected? [68.39(e)]	Y	ΠN	□N/A

RMP Program Level 3 Process Checklist Facility Name: Rh		dia – l	Housto	n Plant
На	zard Assessment: Five-year accident history [68.42]			
38.	Has the owner or operator included all accidental releases from covered processes that resulted in deaths, injuries, or significant property damage on site, or known offsite deaths, injuries, evacuations, sheltering in place, property damage, or environmental damage? [68.42(a)] Please see the documentation provided for the incidents that occurred on June 9, 2012 and November 29, 2008.	Y	ΠN	□N/A
39.	Has the owner or operator reported the following information for each accidental release: [68.42(b)]	Y	\square N	□N/A
	Date, time, and approximate duration of the release? [68.42(b)(1)]			
	Chemical(s) released? [68.42(b)(2)]			
	Estimated quantity released in pounds and percentage weight in a mixture (toxics)? [68.42(b)(3)]			
	NAICS code for the process? [68.42(b)(4)]			
	The type of release event and its source? [68.42(b)(5)]			
	Weather conditions (if known)? [68.42(b)(6)]			
	On-site impacts? [68.42(b)(7)]			
	Known offsite impacts? [68.42(b)(8)]			
	Initiating event and contributing factors (if known)? [68.42(b)(9)]			
	Whether offsite responders were notified (if known)? [68.42(b)(10)]			
	Operational or process changes that resulted from investigation of the release? [68.42(b)(11)]			
Se	ction C: Prevention Program			
Implemented the Program 3 prevention requirements as provided in 40 CFR 68.65 - 68.87?			B U	□N/A
Pre	evention Program- Safety information [68.65]			
1.	Has the owner or operator compiled written process safety information, which includes information pertaining to the hazards of the regulated substances used or produced by the process, information pertaining to the technology of the process, and information pertaining to the equipment in the process, before conducting any process hazard analysis required by the rule? [68.65(a)]	Y	□N	□N/A
	Does the process safety information contain the following for hazards of the substances: [68.65(b)]			
	Material Safety Data Sheets (MSDS) that meet the requirements of the OSHA Hazard Communication Standard [29 CFR 1910.1200(g)]? [68.48(a)(1)]			
	Toxicity information? [68.65(b)(1)]			
	Permissible exposure limits? [68.65(b)(2)]			
	Physical data? [68.65(b)(3)]			
	Reactivity data? [68.65(b)(4)]			
	Corrosivity data? [68.65(b)(5)]			
	Thermal and chemical stability data? [68.65(b)(6)]			
	Hazardous effects of inadvertent mixing of materials that could foreseeably occur? [68.65(b)(7)]			

RI	RMP Program Level 3 Process Checklist Facility Name: Rhodi		lousta	n Plant
2.	Has the owner documented information pertaining to technology of the process? A block flow diagram or simplified process flow diagram? [68.65(c)(1)(i)]	Y	□N	□N/A
	Process chemistry? [68.65(c)(1)(ii)]			
	Maximum intended inventory? [68.65(c)(1)(iii)]			
	Safe upper and lower limits for such items as temperatures, pressures, flows, or compositions? [68.65(c)(1)(iv)]			
	An evaluation of the consequences of deviation? [68.65(c)(1)(iv)]			
3.	Does the process safety information contain the following for the equipment in the process: [68.65(d)(1)]	Y	□N	□n/a
	Materials of construction? 68.65(d)(1)(i)]			
	Piping and instrumentation diagrams [68.65(d)(1)(ii)]			
	Electrical classification? [68.65(d)(1)(iii)]			
	Relief system design and design basis? [68.65(d)(1)(iv)]			
	Ventilation system design? [68.65(d)(1)(v)]			
	Design codes and standards employed? [68.65(d)(1)(vi)]			
	☐ Material and energy balances for processes built after June 21, 1999? [68.65(d)(1)(vii)]			
	Safety systems? [68.65(d)(1)(viii)]			
4.	Has the owner or operator documented that equipment complies with recognized and generally accepted good engineering practices? [68.65(d)(2)]	Y	□N	□N/A
5.	Has the owner or operator determined and documented that existing equipment, designed and constructed in accordance with codes, standards, or practices that are no longer in general use, is designed, maintained, inspected, tested, and operating in a safe manner? [68.65(d)(3)]	Υ	□N	□N/A
Pro	evention Program- Process Hazard Analysis [68.67]			
6.	Has the owner or operator performed an initial process hazard analysis (PHA), and has this analysis identified, evaluated, and controlled the hazards involved in the process? [68.67(a)]	Y	□N	□N/A
7.	Has the owner or operator determined and documented the priority order for conducting PHAs, and was it based on an appropriate rationale? [68.67(a)]	Y	□N	□N/A
8.	Has the owner used one or more of the following technologies to conduct process PHA: [68.67(b)]	Y	ΠN	□N/A
	What-if? [68.67(b)(1)]			
	Checklist? [68.67(b)(2)]			
	□ What-if/Checklist? [68.67(b)(3)]			
	Hazard and Operability Study (HAZOP) [68.67(b)(4)]			
	☐ Failure Mode and Effects Analysis (FMEA) [68.67(b)(5)]			
	☐ Fault Tree Analysis? [68.67(b)(6)]			
	An appropriate equivalent methodology? [68.67(b)(7)] -Layers of Protection			

RN	AP Program Level 3 Process Checklist Facility Name: Rhod	lia – H	lousto	n Plant
9.	Did the PHA address:	Y	ΠN	□N/A
	The hazards of the process? [68.67(c)(1)]			
	Identification of any incident that had a likely potential for catastrophic consequences? [68.67(c)(2)]			
	Engineering and administrative controls applicable to hazards and interrelationships?[68.67(c)(3)]			
	Consequences of failure of engineering and administrative controls? [68.67(c)(4)]			
	Stationary source siting? [68.67(c)(5)]			
	Human factors? [68.67(c)(6)]			
	An evaluation of a range of the possible safety and health effects of failure of controls? [68.67(c)(7)]			
10.	Was the PHA performed by a team with expertise in engineering and process operations and did the team include appropriate personnel? [68.67(d)]	Y	□N	□N/A
11.	Has the owner or operator established a system to promptly address the team's findings and recommendations; assured that the recommendations are resolved in a timely manner and documented; documented what actions are to be taken; completed actions as soon as possible; developed a written schedule of when these actions are to be completed; and communicated the actions to operating, maintenance, and other employees whose work assignments are in the process and who may be affected by the recommendations? [68.67(e)] Action Tracking has been in place since 2006.	Y	ΠN	□n/a
12.	Has the PHA been updated and revalidated by a team every five years after the completion of the initial PHA to assure that the PHA is consistent with the current process? [68.67(f)]	Y	□N	□N/A
13.	Has the owner or operator retained PHAs and updates or revalidations for each process covered, as well as the resolution of recommendations for the life of the process? [68.67(g)]	¥Υ	□N	□N/A
Prevention Program- Operating procedures [68.69]				
14.	Has the owner or operator developed and implemented written operating procedures that provide instructions or steps for conducting activities associated with each covered process consistent with the safety information? [68.69(a)]	Y	ΠN	□N/A

RN	AP Pro	ogram Level 3 Process Checklist Facility	y Name: <u>Rhodia -</u>	– Hoi	ısto	n Plant
15	Do the	procedures address the following: [68.69(a)]		Υ	N	□N/A
	Steps fo	or each operating phase: [68.69(a)(1)]				
		Initial Startup? [68.69(a)(1)(i)]				
		Normal operations? [68.69(a)(1)(ii)]				
		Temporary operations? [68.69((a)(1)(iii)]				
		Emergency shutdown including the conditions under which emergency shutdown is required assignment of shutdown responsibility to qualified operators to ensure that emergency shutdown a safe and timely manner? [68.69(a)(1)(iv)]				
		Emergency operations? [68.69(a)(1)(v)]				
		Normal shutdown? [68.68(a)(1)(vi)]				
		Startup following a turnaround, or after emergency shutdown? [68.69(a)(1)(vii)]				
	<u>Operati</u>	ng limits: [68.69(a)(2)]				
		Consequences of deviations [68.69(a)(2)(i)] (Critical Operating Parameters)				
	68	Steps required to correct or avoid deviation? [68.69(a)(2)(ii)] (
	Safety a	and health considerations: [68.69(a)(3)]				
		Properties of, and physical hazards presented by, the chemicals used in the process [68.69(a)	(3)(i)]			
		Precautions necessary to prevent exposure, including engineering controls, administrative copersonal protective equipment? [68.69(a)(3)(ii)] - References PPE Matrix	ntrols, and			
		annunung satuk satuan ankan di satuk satuk satuk satuan dan di satuk satuk satuk satuk satuk satuk satuk satuk				
		ominos com objecto mais del successor de la composição de la composição de la composição de la composição de l	(6) (6) (6) (6)			
		Newsphotoscientificusting acts and action and actions and actions are actions as a second action and actions are actions as a second action acts and action acts are acts and acts are acts are acts and acts are acts are acts and acts are acts and acts are acts and acts are acts are acts and acts are				
	Sa	fety systems and their functions? [68.69(a)(4)]			····	
16.		erating procedures readily accessible to employees who are involved in a process? [68.69(b)] Retwork.	Readily available	Y [N	□N/A
17.	have be	owner or operator certified annually that the operating procedures are current and accurate and en reviewed as often as necessary? [68.69(c)] The last five years of annual certifications we owing units: Logistics, Regen II, and Unit #8. 2008-2012 were provided for Logistics. 200 ed for Regen II. The year 2012 was provided for Unit#8.	re requested for	Υ	N	□N/A
18.		owner or operator developed and implemented safe work practices to provide for the control of operations, such as lockout/tagout? [68.69(d)]	of hazards during	Y C	N	□N/A
Pre	vention	Program - Training [68.71]				
19		th employee involved in operating a process, and each employee before being involved in oper d process, been initially trained in an overview of the process and in the operating procedures?		 Y [N	□N/A
20.		ial training include emphasis on safety and health hazards, emergency operations including shactices applicable to the employee's job tasks? [68.71(a)(1)]	utdown, and safe	Υ [JN	□N/A
21.	operato	of initial training for those employees already involved in operating a process on June 21, 1999 remay certify in writing that the employee has the required knowledge, skills, and abilities to see and responsibilities as specified in the operating procedures [68.71(a)(2)]		Y C	JN	□N/A
22.	in opera	resher training been provided at least every three years, or more often if necessary, to each emptaing a process to assure that the employee understands and adheres to the current operating properties? [68.71(b)]		Υ [ИС	□N/A

RN	AP Program Level 3 Process Checklist Facility Name: Rhoo	lia – H	lousto	n Plant
23,	Has owner or operator ascertained and documented in record that each employee involved in operating a process has received and understood the training required? [68.71(c)]	Y	□N	□N/A
24.	Does the prepared record contain the identity of the employee, the date of the training, and the means used to verify that the employee understood the training? [68.71(c)] With all documentation provided and reviewed on training it would appear that the facility should look into adding an identifier for the employee to the form and consistent with a number grade as opposed to just a simple PASS or FAIL listed. Also, From the information provided it would appear that refresher training has not been conducted. The documentation of such information is lacking. There were current tests provided to the necessary personnel but the document does not reference whether this is an initial or refresher training. One could not tell what type of record they were looking at. EPA recommends the facility look into updating testing record information.	ПΥ	N	□N/A
Pre	vention Program - Mechanical Integrity [68.73]			
25.	Has the owner or operator established and implemented written procedures to maintain the on-going integrity of the process equipment listed in 68.73(a)? [68.73(b)]	Y	□N	□N/A
26.	Has the owner or operator trained each employee involved in maintaining the on-going integrity of process equipment? [68.73(c)]	Y	ΠN	□N/A
27.	Performed inspections and tests on process equipment? [68.73(d)(1)]	Y	ΠN	□N/A
28.	Followed recognized and generally accepted good engineering practices for inspections and testing procedures? [68.73(d)(2)]	Y	□N	□N/A
29.	Ensured the frequency of inspections and tests of process equipment is consistent with applicable manufacturers' recommendations, good engineering practices, and prior operating experience? [68.73(d)(3)]	Y	□N	□N/A
30.	Documented each inspection and test that had been performed on process equipment, which identifies the date of the inspection or test, the name of the person who performed the inspection or test, the serial number or other identifier of the equipment on which the inspection or test was performed, a description of the inspection or test performed, and the results of the inspection or test? [68.73(d)(4)]	Y	ΠN	□N/A
31.	Corrected deficiencies in equipment that were outside acceptable limits defined by the process safety information before further use or in a safe and timely manner when necessary means were taken to assure safe operation? [68.73(e)]	Y	□N	□N/A
32.	Assured that equipment as it was fabricated is suitable for the process application for which it will be used in the construction of new plants and equipment? [68.73(f)(1)]	Y	□N	□N/A
33.	Performed appropriate checks and inspections to assure that equipment was installed properly and consistent with design specifications and the manufacturer's instructions? [68.73(f)(2)]	Y	N	□N/A
34.	Assured that maintenance materials, spare parts and equipment were suitable for the process application for which they would be used? $[68.73(f)(3)]$	iş by azı	Si Wiles	1818) 8105
Pre	vention Program - Management Of Change [68.75]		***************************************	
35.	Has the owner or operator established and implemented written procedures to manage changes to process chemicals, technology, equipment, and procedures, and changes to stationary sources that affect a covered process? [68.75(a)]	Y	□N	□N/A
36.	Do procedures assure that the following considerations are addressed prior to any change: [68.75(b)]	■ Y	$\square N$	□N/A
	The technical basis for the proposed change? [68.75(b)(1)]			
	Impact of change on safety and health? [68.75(b)(2)]			
	Modifications to operating procedures? [68.75(b)(3)]			
	Necessary time period for the change? [68.75(b)(4)]			
	Authorization requirements for the proposed change? [68.75(b)(5)]			

RN	MP Program Level 3 Process Checklist Facility Name: Rhod	lia – F	Iousta	n Plant
37.	Were employees, involved in operating a process and maintenance, and contract employees, whose job tasks would be affected by a change in the process, informed of, and trained in, the change prior to start-up of the process or affected parts of the process? [68.75(c)]	¥Υ	□N	□N/A
38.	If a change resulted in a change in the process safety information, was such information updated accordingly? [68.75(d)]	У	ΠN	□N/A
39.	If a change resulted in a change in the operating procedures or practices, had such procedures or practices been updated accordingly? [68.75(e)]	Y	□N	□N/A
Pre	vention Program - Pre-startup Safety Review [68.77]			
40.	If the facility installed a new stationary source, or significantly modified an existing source, (as discussed at 68.77(a)) did it perform a pre-startup safety review prior to the introduction of a regulated substance to a process to confirm: [68.77(b)]	Y	ΠN	□N/A
	Construction and equipment was in accordance with design specifications? [68.77(b)(1)]			
	Safety, operating, maintenance, and emergency procedures were in place and were adequate? [68.77(b)(2)]			
	For new stationary sources, a process hazard analysis had been performed and recommendations had been resolved or implemented before startup? [68.77(b)(3)]			
	Modified stationary sources meet the requirements contained in management of change? [68.77(b)(3)]			
	Training of each employee involved in operating a process had been completed? [68.77(b)(4)]			
Pre	vention Program - Compliance audits [68.79] Requested the two most recent audits.			
41.	Has the owner or operator certified that the stationary source has evaluated compliance with the provisions of the prevention program at least every three years to verify that the developed procedures and practices are adequate and being followed? [68.79(a)]	Y	ΠN	□N/A
42.	Has the audit been conducted by at least one person knowledgeable in the process? [68.79(b)]	Y	ΠN	□N/A
43.	Are the audit findings documented in a report? [68.79(c)]	Y	□N	□N/A
44.	Has the owner or operator promptly determined and documented an appropriate response to each of the findings of the audit and documented that deficiencies had been corrected? [68.79(d)] All action items are tracked in Manufacturing Solutions database. However some items have yet to be completed.	Y	□N	□N/A
45.	Has the owner or operator retained the two most recent compliance reports? [68.79(e)] EPA retrieved audits from the years 2009 and 2012.	Y	□N	□N/A
Pre	vention Program - Incident investigation [68.81]			-
46.	Has the owner or operator investigated each incident that resulted in, or could reasonably have resulted in a catastrophic release of a regulated substance? [68.81(a)]	Y	ΠN	□N/A
47.	Were all incident investigations initiated not later than 48 hours following the incident? [68.81(b)]	Y	□N	□N/A
48.	Was an accident investigation team established and did it consist of at least one person knowledgeable in the process involved, including a contract employee if the incident involved work of a contractor, and other persons with appropriate knowledge and experience to thoroughly investigate and analyze the incident? [68.81(c)]	Y	□N	□N/A
49.	Was a report prepared at the conclusion of every investigation? [68.81(d)]	Y	□N	□N/A

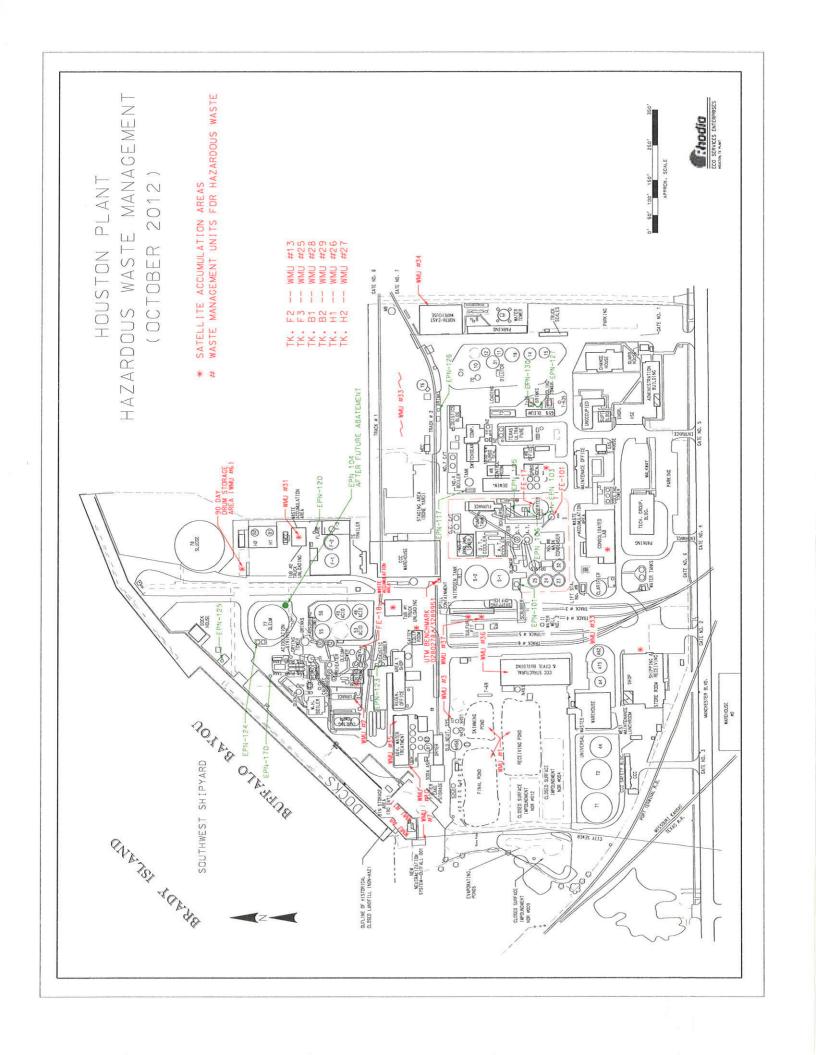
RMP Program Level 3 Process Checklist Facility Name: Rhodia – Houston Pl			n Plant	
50.	Does every report include: [68.81(d)]	Y	□N	□N/A
	Date of incident? [68.81(d)(1)]			
	Date investigation began? [68.81(d)(2)]			
	A description of the incident? [68.81(d)(3)]			
	The factors that contributed to the incident? [68.81(d)(4)]			
	Any recommendations resulting from the investigation? [68.81(d)(5)]			
51.	Has the owner or operator established a system to address and resolve the report findings and recommendations, and are the resolutions and corrective actions documented? [68.81(e)]	Y	□N	□N/A
52.	Was the report reviewed with all affected personnel whose job tasks are relevant to the incident findings including contract employees where applicable? [68.81(f)]	Y	ΠN	□N/A
53.	Has the owner or operator retained incident investigation reports for at least five years? [68.81(g)]	Y	□N	□N/A
Se	ction D - Employee Participation [68.83]	_		
1.	Has the owner or operator developed a written plan of action regarding the implementation of the employee participation required by this section? [68.83(a)]	Y	□N	□N/A
2.	Has the owner or operator consulted with employees and their representatives on the conduct and development of process hazards analyses and on the development of the other elements of process safety management in chemical accident prevention provisions? [68.83(b)]	Y	ΠN	□N/A
3.	Has the owner or operator provided to employees and their representatives access to process hazards analyses and to all other information required to be developed under the chemical accident prevention rule? [68.83(c)]	Y	ΠN	□n/a
Section E - Hot Work Permit [68.85]				
1.	Has the owner or operator issued a hot work permit for each hot work operation conducted on or near a covered process? [68.85(a)]	Y	ΠN	□N/A
2.	Does the permit document that the fire prevention and protection requirements in 29CFR 1910.252(a) have been implemented prior to beginning the hot work operations? [68.85(b)]	Y	ΠN	□N/A
3.	Does the permit indicate the date(s) authorized for hot work and the object(s) upon which hot work is to be performed? [68.85(b]	Y	□N	□N/A
4.	Are the permits being kept on file until completion of the hot work operations? [68.85(b)]	Y	□N	□N/A
Se	etion F - Contractors [68.87]			
1.	Has the owner or operator obtained and evaluated information regarding the contract owner or operator's safety performance and programs when selecting a contractor? [68.87(b)(1)]	Y	□N	□N/A
2.	Informed contract owner or operator of the known potential fire, explosion, or toxic release hazards related to the contractor's work and the process? [68.87(b)(2)]	Y	ΠN	□N/A
3.	Explained to the contract owner or operator the applicable provisions of the emergency response or the emergency action program? [68.87(b)(3)]	Y	□N	□N/A
4.	Developed and implemented safe work practices consistent with §68.69(d), to control the entrance, presence, and exit of the contract owner or operator and contract employees in the covered process areas? [68.87(b)(4)]	Y	ΠN	□N/A
5.	Periodically evaluated the performance of the contract owner or operator in fulfilling their obligations (as described at $68.87(c)(1) - (c)(5)$)? [$68.87(b)(5)$]	Ϋ́	ПИ	□N/A

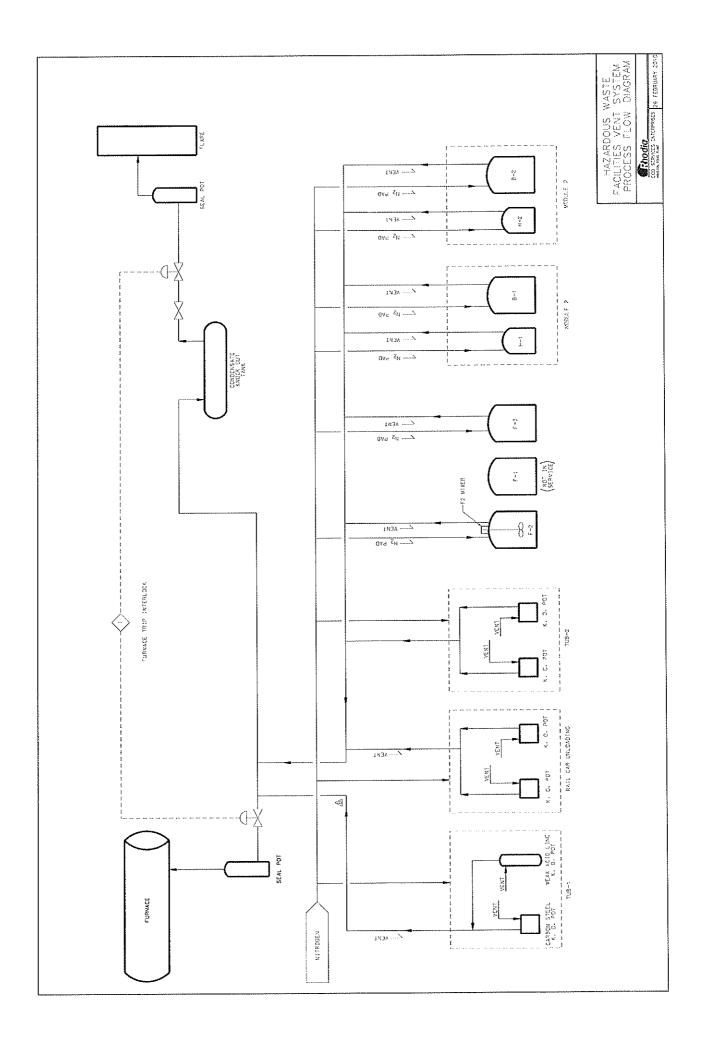
RMP Program Level 3 Process Checklist Facility Name: Rhodia - Houston Plant						
Section G - Emergency Response [68.90 - 68.95]						
Developed and implemented an emergency response program as provided in 40 CFR 68.90-68.95? Comments:	⊐M	□U	□N/A			
1. Is the facility designated as a "first responder" in case of an accidental release of regulated substances"	Y	□N	□N/A			
1.a. If the facility is not a first responder:						
1.a.(1) For stationary sources with any regulated substances held in a process above threshold quantities, is the source included in the community emergency response plan developed under 42 U.S.C. 11003? [68.90(b)(1)]	□Y	□N	™ N/A			
1.a.(2) For stationary sources with only regulated flammable substances held in a process above threshold quantities, has the owner or operator coordinated response actions with the local fire department? [68.90(b)(2)]	ПΥ	ΠN	N /A			
1.a.(3) Are appropriate mechanisms in place to notify emergency responders when there is need for a response? [68.90(b)(3)]	ΠY	ПN	® N/A			
2. An emergency response plan is maintained at the stationary source and contains the following? [68.95(a)(1)]	Y	□N	□N/A			
Procedures for informing the public and local emergency response agencies about accidental releases? [68.95(a)(1)(i)]						
Documentation of proper first-aid and emergency medical treatment necessary to treat accidental human exposures? [68.95(a)(1)(ii)]						
Procedures and measures for emergency response after an accidental release of a regulated substance? [68.95(a)(1)(iii)]						
3. The emergency response plan contains procedures for the use of emergency response equipment and for its inspection, testing, and maintenance? [68.95(a)(2)] f;	Y	□N	□N/A			
4. The emergency response plan requires, and there is documentation of, training for all employees in relevant procedures? [68.95(a)(3)]	¥Υ	ПN	□N/A			
5. The owner or operator has developed and implemented procedures to review and update, as appropriate, the emergency response plan to reflect changes at the stationary source and ensure that employees are informed of changes? [68.95(a)(4)] Annually reviewed or as necessary depending on any changes that may be required.	Y	ΠN	□N/A			
6. Did the owner or operator use a written plan that complies with other Federal contingency plan regulations or is consistent with the approach in the National Response Team's Integrated Contingency Plan Guidance ("One Plan")? If so, does the plan include the elements provided in paragraph (a) of 68.95, and also complies with paragraph (c) of 68.95? [68.95(b)]	ПΥ	ΠN	N/A			
7. Has the emergency response plan been coordinated with the community emergency response plan developed under EPCRA? [68.95(c)]	Y	ΠN	□N/A			
Section H – Risk Management Plan [40 CFR 68.190 – 68.195]						
 Does the single registration form include, for each covered process, the name and CAS number of each regulated substance held above the threshold quantity in the process, the maximum quantity of each regulated substance or mixture in the process (in pounds) to two significant digits, the five- or six-digit NAICS code that most closely corresponds to the process and the Program level of the process? [68.160(b)(7)] 	Y	ΩN	□N/A			
2. Did the facility assign the correct program level(s) to its covered process(es)? [68.160(b)(7)]	Y	ΠN	□N/A			

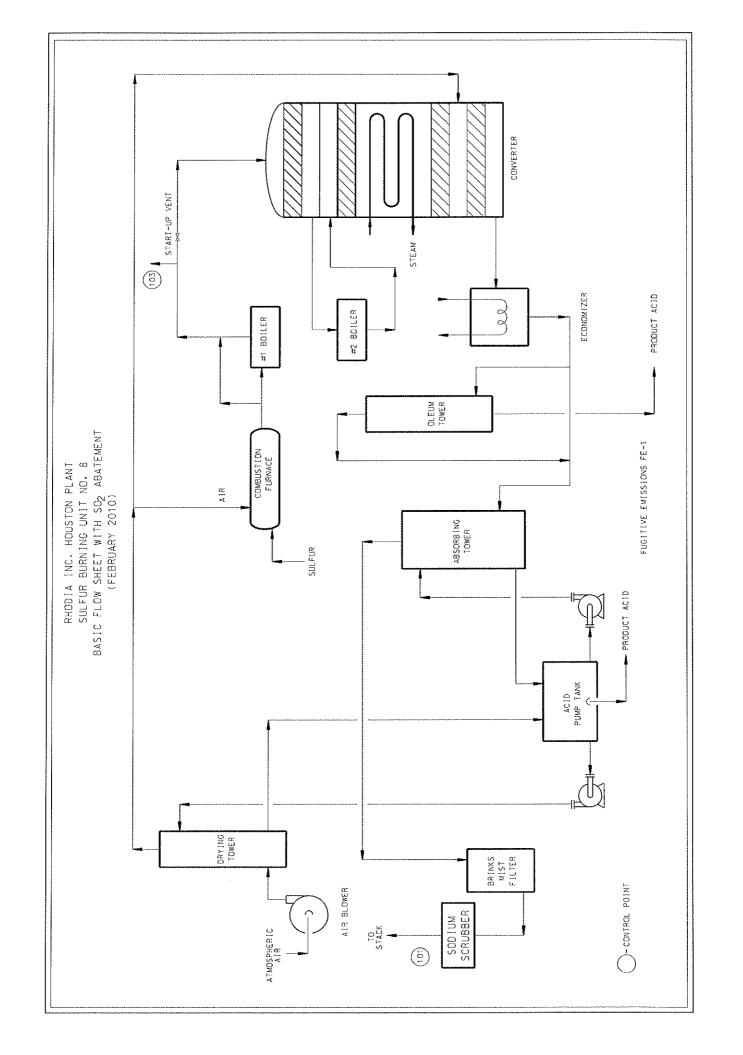
RMP Program Level 3 Process Checklist Facility Name: Rhodia – Houston Plant							
	Five-year update. [68.190(b)(1)]						
	☐ Within three years of a newly regulated substance listing. [68.190(b)(2)]						
	At the time a new regulated substance is first present in an already regulated process above threshold quantities. [68.190(b)(3)]						
	At the time a regulated substance is first present in an new process above threshold quantities. [68.190(b)(4)]						
	☐ Within six months of a change requiring revised PHA or hazard review. [68.190(b)(5)]						
	☐ Within six months of a change requiring a revised OCA as provided in 68.36. [68.190(b)(6)]						
	☐ Within six months of a change that alters the Program level that applies to any covered process. [68.190(b)(7)]	į					
4.	If the owner or operator experienced an accidental release that met the five-year accident history reporting criteria (as described at 68.42) subsequent to April 9, 2004, did the owner or operator submit the information required at 68.168, 68.170(j) and 68.175(l) within six months of the release or by the time the RMP was updated as required at 68.190, whichever was earlier. [68.195(a)]	Y	ΠN	□N/A			
5.	If the emergency contact information required at 68.160(b)(6) has changed since June 21, 2004, did the owner or operator submit corrected information within thirty days of the change? [68.195(b)]	ΝY	□N	□N/A			

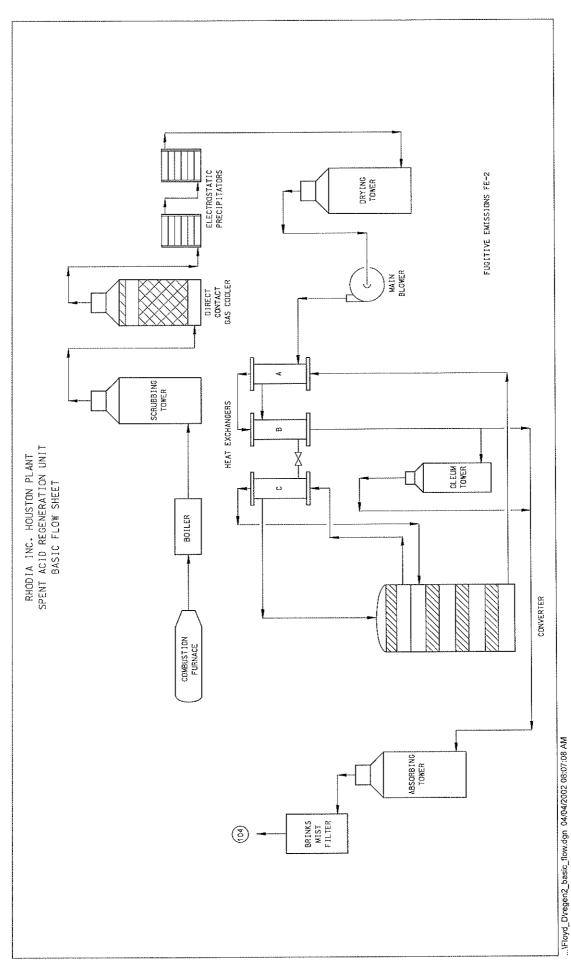
Section III – ATTACHMENTS

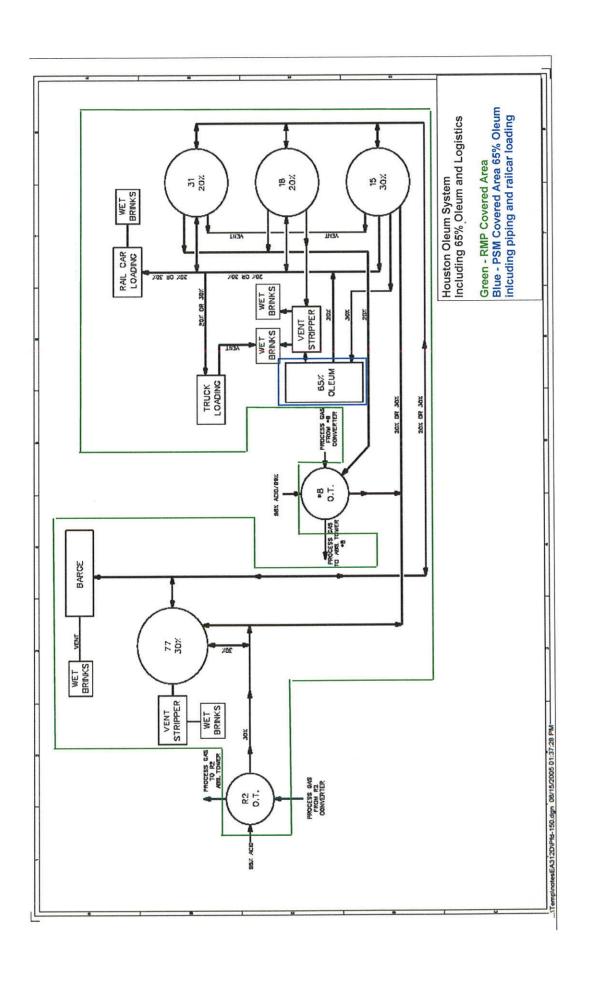
- 1. Process Description and corresponding Process Flow Diagrams
 - 2. Current RMP Submittal
 - 3. Facility Management System
 - 4. Operating Procedures and Certifications
 - 5. Operator Training Records
 - 6. Compliance Audits
 - 7. Exit Briefing Sign-In Sheet
 - 8. Hot Work Permits
 - 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)











Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5. Operator Training Records
- 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

Section 1. Registration Information

Source Identification

Facility Name:

Rhodia, Houston Plant

Parent Company #1 Name:

Parent Company #2 Name:

Rhodia Inc.

Submission and Acceptance

Submission Type:

Re-submission

Subsequent RMP Submission Reason:

Newly regulated substance above TQ in already covered process (40 CFR 68.190(b)(3))

Description:

Receipt Date:

08-Nov-2012

Postmark Date:

08-Nov-2012

Next Due Date:

08-Nov-2017

Completeness Check Date:

08-Nov-2012 Yes

Complete RMP:

De-Registration / Closed Reason:

De-Registration / Closed Reason Other Text:

De-Registered / Closed Date:

De-Registered / Closed Effective Date:

Certification Received:

Yes

Facility Identification

EPA Facility Identifier:

1000 0008 2983

Other EPA Systems Facility ID:

77012STFFR8615M

Dun and Bradstreet Numbers (DUNS)

Facility DUNS:

Parent Company #1 DUNS:

Parent Company #2 DUNS:

Facility Location Address

Street 1:

8615 Manchester Street

Street 2:

Houston

City: State:

TEXAS

ZIP:

77012

ZIP4:

HARRIS

County:

Facility Latitude and Longitude

Latitude (decimal):

29,718139

Longitude (decimal):

-095.268750

Lat/Long Method:

Interpolation - Digital map source (TIGER)

Lat/Long Description:

Facility Centroid

Horizontal Accuracy Measure:

Horizontal Reference Datum Name:

World Geodetic System of 1984

Source Map Scale Number:

Plan Sequence Number: 1000031578

Owner or Operator

Operator Name: Operator Phone:

Rhodia Inc. (609) 860-4000

Mailing Address

Operator Street 1:

8 Cedar Brook Drive

Operator Street 2:

Operator City: Operator State:

Cranbury NEW JERSEY

Operator ZIP: Operator ZIP4:

08512 7500

Operator Foreign State or Province:

Operator Foreign ZIP: Operator Foreign Country:

Name and title of person or position responsible for Part 68 (RMP) Implementation

RMP Name of Person:

William McConnell

RMP Title of Person or Position:

Plant Manager

RMP E-mail Address:

william.mcconnell@us.rhodia.com

Emergency Contact

Emergency Contact Name: Emergency Contact Title: Emergency Contact Phone: William McConnell Plant Manager (713) 924-1401

Emergency Contact 24-Hour Phone:

(713) 928-3411

Emergency Contact Ext. or PIN:

Emergency Contact E-mail Address:

william.mcconnell@us.rhodia.com

Other Points of Contact

Facility or Parent Company E-mail Address:

Facility Public Contact Phone:

Facility or Parent Company WWW Homepage

Address:

Local Emergency Planning Committee

LEPC:

Houston LEPC

Full Time Equivalent Employees

Number of Full Time Employees (FTE) on Site:

140

FTE Claimed as CBI:

Covered By

OSHA PSM:

Yes

EPCRA 302 : CAA Title V:

Yes Yes

Data displayed is accurate as of 12:00 AM (EDT) Wednesday, April 17, 2013

Plan Sequence Number: 1000031578

Air Operating Permit ID:

O-3049

OSHA Ranking

OSHA Star or Merit Ranking:

Last Safety Inspection

Last Safety Inspection (By an External Agency)

Last Safety Inspection Performed By an External

27-Aug-2008

EPA

Predictive Filing

Did this RMP involve predictive filing?:

Yes

Preparer Information

Preparer Name:

Preparer Phone:

Preparer Street 1:

Preparer Street 2:

Preparer City:

Preparer State:

Preparer ZIP:

Preparer ZIP4:

Preparer Foreign State:

Preparer Foreign Country:

Preparer Foreign ZIP:

Confidential Business Information (CBI)

CBI Claimed:

Substantiation Provided:

Unsanitized RMP Provided:

Reportable Accidents

Reportable Accidents:

See Section 6. Accident History below to determine if there were any accidents reported for this RMP.

Process Chemicals

Process ID:

1000038620

Description:

Hazardous Waste Treatment

Process Chemical ID:

1000046376

Program Level:

Program Level 3 process

Chemical Name:

Acetaldehyde

CAS Number:

75-07-0

Quantity (lbs):

37500

CBI Claimed:

Flammable/Toxic:

Flammable

Plan Sequence Number: 1000031578

Process ID:

1000038620

Description:

Hazardous Waste Treatment

Process Chemical ID:

1000046371

Program Level:

Program Level 3 process

Chemical Name:

Vinyl acetate monomer [Acetic acid ethenyl ester]

CAS Number: Quantity (lbs): 108-05-4

CBI Claimed:

384000

Flammable/Toxic:

Toxic

Process ID:

1000038620

Description:

Hazardous Waste Treatment

Process Chemical ID:

1000046372

Program Level:

Program Level 3 process

Chemical Name:

Toluene diisocyanate (unspecified isomer) [Benzene, 1,3-diisocyanatomethyl-]

26471-62-5

CAS Number: Quantity (lbs):

120000

CBI Claimed:

Flammable/Toxic:

Toxic

Process ID:

1000038620

Description:

Hazardous Waste Treatment

Process Chemical ID:

1000046375

Program Level: Chemical Name: Program Level 3 process Allyl alcohol [2-Propen-1-ol]

CAS Number:

107-18-6

Quantity (lbs):

80000

CBI Claimed:

Flammable/Toxic:

Toxic

Process ID:

1000038617

Description:

Regen 2 Unit

Process Chemical ID:

1000046365

Program Level:

Program Level 3 process

Chemical Name:

Oleum (Furning Sulfuric acid) [Sulfuric acid, mixture with sulfur trioxide]

8014-95-7

CAS Number: Quantity (lbs):

249000

CBI Claimed:

Flammable/Toxic:

Toxic

Process ID:

1000038620

Description:

Hazardous Waste Treatment

Process Chemical ID:

1000046374

Program Level:

Program Level 3 process

Chemical Name:

Ethyl mercaptan [Ethanethiol]

Facility Name: Rhodia, Houston Plant

EPA Facility Identifier: 1000 0008 2983 Plan Sequence Number: 1000031578

CAS Number: 75-08-1
Quantity (lbs): 41000

CBI Claimed:

Flammable/Toxic: Flammable

 Process ID:
 1000038618

 Description:
 No. 8 Unit

 Process Chemical ID:
 1000046366

Program Level: Program Level 3 process

Chemical Name: Oleum (Furning Sulfuric acid) [Sulfuric acid, mixture

with sulfur trioxide]

CAS Number: 8014-95-7
Quantity (lbs): 218000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046370

Program Level: Program Level 3 process

Chemical Name: Dimethylamine [Methanamine, N-methyl-]

CAS Number: 124-40-3

Quantity (lbs): 80000

CBI Claimed:

Flammable/Toxic: Flammable

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046373

Program Level: Program Level 3 process

Chemical Name: Methyl mercaptan [Methanethiol]

CAS Number: 74-93-1
Quantity (lbs): 95000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046379

Program Level: Program Level 3 process
Chemical Name: Acrylonitrile [2-Propenenitrile]

CAS Number: 107-13-1 Quantity (lbs): 68000

CBI Claimed:

Flammable/Toxic: Toxic

Plan Sequence Number: 1000031578

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046383

Program Level: Program Level 3 process
Chemical Name: Flammable Mixture

CAS Number: 00-11-11
Quantity (lbs): 540000

CBI Claimed:

Flammable/Toxic: Flammable

Flammable Mixture Chemical Components

Flammable Mixture Chemical ID: 1000038960

Chemical Name: Ethyl chloride [Ethane, chloro-]

CAS Number: 75-00-3
Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038962

Chemical Name: Ethyl mercaptan [Ethanethiol]

CAS Number: 75-08-1 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038957
Chemical Name: 2-Butene-cis
CAS Number: 590-18-1
Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038965
Chemical Name: 1-Butene
CAS Number: 106-98-9
Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038961

Chemical Name: Propylene [1-Propene]

CAS Number: 115-07-1
Flammable/Toxic: Ffammable

Flammable Mixture Chemical ID: 1000038959

Chemical Name: 2-Methylpropene [1-Propene, 2-methyl-]

CAS Number: 115-11-7 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038964

Chemical Name: Isopentane [Butane, 2-methyl-]

CAS Number: 78-78-4
Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038958

Chemical Name: 2-Butene-trans [2-Butene, (E)]

CAS Number: 624-64-6 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038963
Chemical Name: 1,3-Butadiene
CAS Number: 106-99-0
Flammable/Toxic: Flammable

Process ID: 1000038615

Description: TXUP, Sulfur Trioxide

Process Chemical ID: 1000046363

Program Level: Program Level 3 process

Chemical Name: Sulfur trioxide
CAS Number: 7446-11-9
Quantity (lbs): 27505

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038619
Description: Logistics
Process Chemical ID: 1000046367

Program Level: Program Level 3 process

Chemical Name: Oleum (Fuming Sulfuric acid) [Sulfuric acid, mixture

with sulfur trioxide]

CAS Number: 8014-95-7
Quantity (lbs): 39134000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046378

Program Level: Program Level 3 process

Chemical Name: Hydrogen sulfide
CAS Number: 7783-06-4
Quantity (lbs): 46200

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046384

Program Level: Program Level 3 process
Chemical Name: Flammable Mixture

CAS Number: 00-11-11
Quantity (lbs): 90000

CBI Claimed:

Flammable/Toxic: Flammable

Flammable Mixture Chemical Components

Flammable Mixture Chemical ID: 1000038968

Chemical Name: Isopropylamine [2-Propanamine]

CAS Number: 75-31-0 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038967

Chemical Name: Ethylamine [Ethanamine]

CAS Number: 75-04-7 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038969

Chemical Name: Methylamine [Methanamine]

CAS Number: 74-89-5 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038970

Chemical Name: Trimethylamine [Methanamine, N,N-dimethyl-]

CAS Number: 75-50-3
Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038966

Chemical Name: Dimethylamine [Methanamine, N-methyl-]

CAS Number: 124-40-3 Flammable/Toxic: Flammable

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046368

Program Level: Program Level 3 process
Chemical Name: Propionitrile [Propanenitrile]

CAS Number: 107-12-0 Quantity (lbs): 362000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046369

Program Level: Program Level 3 process

Chemical Name: Carbon disulfide

CAS Number: 75-15-0

Quantity (lbs): 230000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046377

Program Level: Program Level 3 process

Chemical Name: Hydrazine
CAS Number: 302-01-2
Quantity (lbs): 23000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046381

Program Level: Program Level 3 process

Chemical Name: Propylene oxide [Oxirane, methyl-]

CAS Number: 75-56-9
Quantity (lbs): 45000

CBI Claimed:

Flammable/Toxic: Toxic

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046380

Program Level: Program Level 3 process

Chemical Name: Isopropylamine [2-Propanamine]
CAS Number: 75-31-0

CAS Number: 75-31-0 Quantity (lbs): 345000

CBI Claimed:

Flammable/Toxic: Flammable

Process ID: 1000038620

Description: Hazardous Waste Treatment

Process Chemical ID: 1000046382

Program Level: Program Level 3 process
Chemical Name: Flammable Mixture

CAS Number: 00-11-11
Quantity (lbs): 460000

CBI Claimed:

Flammable/Toxic: Flammable

Flammable Mixture Chemical Components

Flammable Mixture Chemical ID: 1000038956

Chemical Name: Propylene [1-Propene]

CAS Number: 115-07-1 Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038954
Chemical Name: 1-Butene
CAS Number: 106-98-9

Flammable/Toxic: Flammable

Flammable Mixture Chemical ID: 1000038955
Chemical Name: Propane
CAS Number: 74-98-6

Flammable/Toxic: Flammable

Process NAICS

Process ID: 1000038615 Process NAICS ID: 1000038957

Program Level 3 process Program Level:

NAICS Code:

All Other Miscellaneous Chemical Product and Preparation Manufacturing NAICS Description:

Process ID: 1000038617 Process NAICS ID: 1000038959

Program Level 3 process Program Level:

325188 NAICS Code:

NAICS Description: All Other Basic Inorganic Chemical Manufacturing

Process ID: 1000038618 Process NAICS ID: 1000038960

Program Level: Program Level 3 process

NAICS Code: 325188

NAICS Description: All Other Basic Inorganic Chemical Manufacturing

Process ID: 1000038619 1000038961 Process NAICS ID:

Program Level: Program Level 3 process

NAICS Code: 325188

NAICS Description: All Other Basic Inorganic Chemical Manufacturing

1000038620 Process ID: Process NAICS ID: 1000038962

Program Level 3 process Program Level:

NAICS Code: 325188

All Other Basic Inorganic Chemical Manufacturing NAICS Description:

Facility Name: Rhodia, Houston Plant

EPA Facility Identifier: 1000 0008 2983

Plan Sequence Number: 1000031578

Section 2. Toxics: Worst Case

Toxic Worst ID: 1000031857

Percent Weight: 30.0
Physical State: Liquid

Model Used: EPA's OCA Guidance Reference Tables or

Equations

Release Duration (mins): 10
Wind Speed (m/sec): 1.5
Atmospheric Stability Class: F
Topography: Urban

Passive Mitigation Considered

Dikes: Enclosures: Berms: Drains: Sumps:

Other Type: Dock taken as partial secondary containment

Section 3. Toxics: Alternative Release

Toxic Alter ID: 1000033746

Percent Weight: Physical State:

100.0 Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec):

3.0

Atmospheric Stability Class:

D

Topography:

Urban

Passive Mitigation Considered

Dikes:

Enclosures:

Yes

Berms: Drains: Sumps:

Other Type:

Active Mitigation Considered

Sprinkler System: Deluge System:

Water Curtain: Neutralization:

Excess Flow Valve:

Flares:

Scrubbers:

Yes

Emergency Shutdown:

Yes

Other Type:

Toxic Alter ID: 1000033748

Percent Weight:

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec):

3.0

Atmospheric Stability Class:

D

Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Drains:

Sumps:

Yes

Other Type:

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System:

Water Curtain:

Neutralization:

Excess Flow Valve:

Flares:

Scrubbers:

Plan Sequence Number: 1000031578

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033749

Percent Weight:

50.0

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec): Atmospheric Stability Class: 3.0 D

Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Drains: Sumps:

Yes

Other Type:

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Yes

Other Type:

Toxic Alter ID: 1000033750

Percent Weight:

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec): Atmospheric Stability Class: 3.0 D

Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Berms: Drains:

Dians:

Sumps:

Other Type:

Yes

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Flares:

Facility Name: Rhodia, Houston Plant

EPA Facility Identifier: 1000 0008 2983

Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Plan Sequence Number: 1000031578

Toxic Alter ID: 1000033751

Percent Weight:

30.0 Liquid

Physical State: Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec):

3.0 D

Atmospheric Stability Class:

Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Drains: Sumps:

Other Type:

Yes

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Flares:

Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033752

Percent Weight:

10.0

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM) 3.0

Wind Speed (m/sec): Atmospheric Stability Class:

Topography:

Urban

D

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Drains: Sumps:

Other Type:

Yes

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Facility Name: Rhodia, Houston Plant

EPA Facility Identifier: 1000 0008 2983 Plan Sequence Number: 1000031578

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

0.08

Liquid

Toxic Alter ID: 1000033753

Percent Weight:
Physical State:

Model Used: EPA's RMP*Comp(TM)

Wind Speed (m/sec): 3.0
Atmospheric Stability Class: D
Topography: Urban

Passive Mitigation Considered

Dikes: Yes

Enclosures:
Berms:
Drains:

Sumps: Yes

Other Type:

Active Mitigation Considered

Sprinkler System: Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033754

Percent Weight:

Physical State: Liquid

Model Used: EPA's RMP*Comp(TM)

Wind Speed (m/sec): 3.0
Atmospheric Stability Class: D
Topography: Urban

Passive Mitigation Considered

Dikes: Yes

Enclosures: Berms: Drains:

Sumps: Yes

Other Type:

Active Mitigation Considered

Sprinkler System: Yes

Deluge System: Water Curtain: Neutralization:

Facility Name: Rhodia, Houston Plant
EPA Facility Identifier: 1000 0008 2983

Plan Sequence Number: 1000031578

Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033755

Percent Weight:

6.0

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec): Atmospheric Stability Class: 3.0 D

Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures:

Berms:

Drains:

Sumps:

Yes

Other Type:

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System: Water Curtain: Neutralization:

Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033756

Percent Weight:

Physical State:

Liquid

Model Used:

EPA's RMP*Comp(TM)

Wind Speed (m/sec):

3.0

Atmospheric Stability Class: Topography:

Urban

Passive Mitigation Considered

Dikes:

Yes

Enclosures: Berms:

Drains:

Sumps:

Yes

Other Type:

Active Mitigation Considered

Sprinkler System:

Yes

Deluge System:

Water Curtain:

Plan Sequence Number: 1000031578

Neutralization:

Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Toxic Alter ID: 1000033757

Percent Weight: Physical State:

Liquid EPA's RMP*Comp(TM) Model Used:

Wind Speed (m/sec):

Atmospheric Stability Class: D Topography: Urban

Passive Mitigation Considered

Dikes: Yes

Enclosures: Berms: Drains:

Sumps: Yes Other Type:

Active Mitigation Considered

Sprinkler System: Yes

Deluge System: Water Curtain: Neutralization: Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Yes

25.0

3.0

Toxic Alter ID: 1000033763

30.0 Percent Weight: Physical State: Liquid

Areal Locations of Hazardous Atmospheres [ALOHA(R)]Model Used:

Wind Speed (m/sec): 3.0 Atmospheric Stability Class: D Urban Topography:

Passive Mitigation Considered

Dikes: Enclosures: Berms: Drains:

Sumps: Yes

Other Type:

Active Mitigation Considered

Sprinkler System:

Facility Name: Rhodia, Houston Plant	
EPA Facility Identifier: 1000 0008 2983	

Plan Sequence Number: 1000031578

Deluge System: Water Curtain:

Neutralization:

Excess Flow Valve:

Flares: Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Yes

Toxic Alter ID: 1000033764

Percent Weight: Physical State:

Model Used:

Wind Speed (m/sec):

Atmospheric Stability Class:

Topography:

30.0

Liquid

EPA's RMP*Comp(TM)

D.0

Urban

Passive Mitigation Considered

Dikes: Enclosures: Berms: Drains:

Sumps: Other Type: Yes

Active Mitigation Considered

Sprinkler System: Deluge System: Water Curtain: Neutralization:

Excess Flow Valve:

Flares:

Scrubbers:

Emergency Shutdown:

Other Type:

Yes

Toxic Alter ID: 1000033765

Percent Weight:

ľ:

Physical State:

Model Used:

Wind Speed (m/sec):

Atmospheric Stability Class: Topography:

30.0

Liquid

EPA's RMP*Comp(TM)

3.0 D

Urban

Passive Mitigation Considered

Dikes: Enclosures: Berms: Drains:

Sumps: Other Type: Yes

Active Mitigation Considered

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983	Plan Sequence Number: 1000031578
Sprinkler System:	
Deluge System:	
Water Curtain:	
Neutralization:	Yes
Excess Flow Valve:	
Flares:	
Scrubbers:	
Emergency Shutdown:	

Other Type:

Plan Sequence Number: 1000031578

Section 4. Flammables: Worst Case

Flammable Worst ID: 1000023871

Model Used: Endpoint used: EPA's RMP*Comp(TM)

1 PSI

Passive Mitigation Considered

Blast Walls: Other Type:

Plan Sequence Number: 1000031578

Section 5. Flammables: Alternative Release

Flammable Alter ID: 1000022331

Model Used:

EPA's RMP*Comp(TM)

Passive Mitigation Considered

Dikes:

Yes

Fire Walls: Blast Walls: Enclosures: Other Type:

Active Mitigation Considered

Sprinkler System: Deluge System:

Yes

Water Curtain: Excess Flow Valve:

Other Type:

Plan Sequence Number: 1000031578

Section 6. Accident History

Accident History ID: 1000025979

Date of Accident:

09-Jun-2012

Time Accident Began (HHMM):

1111

NAICS Code of Process Involved:

325188

NAICS Description: Release Duration:

All Other Basic Inorganic Chemical Manufacturing

000 Hours 09 Minutes

Release Event

Gas Release:

Yes

Liquid Spill/Evaporation:

Yes

Fire:

Explosion:

Uncontrolled/Runaway Reaction:

Release Source

Storage Vessel:

Piping:

Yes

Process Vessel:

Transfer Hose:

Valve:

Pump:

Joint:

Other Release Source:

Weather Conditions at the Time of Event

Wind Speed:

8.4

Units:

miles/h

Direction:

NE

Temperature:

88

Atmospheric Stability Class:

D

Precipitation Present:

Unknown Weather Conditions:

On-Site Impacts

Employee or Contractor Deaths:

0

Public Responder Deaths:

0

Public Deaths:

0

Employee or Contractor Injuries:

0

Public Responder Injuries:

0

Public Injuries:

0

On-Site Property Damage (\$):

0

Known Off-Site Impacts

Deaths:

Evacuated:

0

Hospitalization:

0

Other Medical Treatments:

0 0

Facility Name: Rhodia, Houston Plant		
EPA Facility Identifier: 1000 0008 2983		Plan Sequence Number: 1000031578
Sheltered-in-Place:	8	
Off-Site Property Damage (\$):	0	
Environmental Damage		
Fish or Animal Kills:		
Tree, Lawn, Shrub, or Crop Damage:		
Water Contamination:		
Soil Contamination:		
Other Environmental Damage:		
Initiating Event		
Initiating Event:	Equipment Failure	
Contributing Factors		
England Fellow	V	
Equipment Failure:	Yes	. •
Human Error:		
Improper Procedures: Overpressurization:		
Upset Condition:		
By-Pass Condition:		
Maintenance Activity/Inactivity:		
Process Design Failure:		
Unsuitable Equipment:		
Unusual Weather Condition:		
Management Error:		
Other Contributing Factor:		
Off-Site Responders Notified		
On Old Nedponders Notified		
Off-Site Responders Notified:	Notified and Responded	
Changes Introduced as a Result of the Accident		
to a second of the second of t	V	
Improved or Upgraded Equipment:	Yes Yes	
Revised Maintenance: Revised Training:	res	
Revised Training. Revised Operating Procedures:		
New Process Controls:		
New Mitigation Systems:		
Revised Emergency Response Plan:		
Changed Process:		
Reduced Inventory:		
None:		
Other Changes Introduced:		
Confidential Business Information		
CBI Claimed:		
Chemicals in Accident History		

Facility Name: Rhodia, Houston EPA Facility Identifier: 1000 000		Plan Sequence Number: 1000031578
Accident Chemica	ID:	1000020230
Quantity Released	(lbs):	868
Percent Weight:		30.0
Chemical Name:		Oleum (Fuming Sulfuric acid) [Sulfuric acid, mixture with sulfur trioxide]
CAS Number:		8014-95-7
Flammable/Toxic:		Toxic
Accident History ID: 100)0025978	
Date of Accident:		29-Nov-2008
Time Accident Beg	ıan (HHMM):	0305
NAICS Code of Pr		325188
NAICS Description	1:	All Other Basic Inorganic Chemical Manufacturing
Release Duration:		002 Hours 42 Minutes
Release Event		
Gas Release:	. •	Yes
Liquid Spill/Evapor	ation:	Yes
Fire:		
Explosion:		
Uncontrolled/Runa	way Reaction:	
Release Source		
Storage Vessel:		
Piping:		
Process Vessel:		Yes
Transfer Hose:		
Valve:		
Pump:		
Joint:		
Other Release Sou	irce:	
Weather Conditions at t	ne Time of Event	
Wind Speed:		15.0
Units:		miles/h
Direction:		NW
Temperature:		62
Atmospheric Stabil	itv Class:	D
Precipitation Prese		_
Unknown Weather		

On-Site Impacts

Employee or Contractor Deaths:	0
Public Responder Deaths:	0
Public Deaths:	0
Employee or Contractor Injuries:	0
Public Responder Injuries:	0
Public Injuries:	0
On-Site Property Damage (\$):	0

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983 Plan Sequence Number: 1000031578 Known Off-Site Impacts Deaths: 0 0 Hospitalization: Other Medical Treatments: 0 0 Evacuated: Sheltered-in-Place: 0 Off-Site Property Damage (\$): 0 **Environmental Damage** Fish or Animal Kills: Tree, Lawn, Shrub, or Crop Damage: Water Contamination: Soil Contamination: Other Environmental Damage: Initiating Event **Equipment Failure** Initiating Event: **Contributing Factors** Yes Equipment Failure: Human Error: Improper Procedures: Overpressurization: **Upset Condition:** By-Pass Condition: Maintenance Activity/Inactivity: Process Design Failure: Unsuitable Equipment: Unusual Weather Condition: Management Error: Other Contributing Factor: Off-Site Responders Notified Off-Site Responders Notified: Notified and Responded Changes Introduced as a Result of the Accident Improved or Upgraded Equipment: Revised Maintenance: Yes

Revised Training:

Revised Operating Procedures:

New Process Controls: New Mitigation Systems:

Revised Emergency Response Plan:

Yes

Changed Process: Reduced Inventory:

None:

Other Changes Introduced:

Plan Sequence Number: 1000031578

Confidential Business Information

CBI Claimed:

Chemicals in Accident History

Accident Chemical ID:

1000020229

Quantity Released (lbs):

203

Percent Weight:

20.0

Chemical Name:

Oleum (Fuming Sulfuric acid) [Sulfuric acid, mixture with sulfur trioxide]

CAS Number:

8014-95-7

Flammable/Toxic:

Toxic

Plan Sequence Number: 1000031578

Section 7. Program Level 3

Description

TXUP Unit - Sulfur Trioxide

Program Level 3 Prevention Program Chemicals

Prevention Program Chemical ID:

1000039875

Chemical Name:

Sulfur trioxide

Flammable/Toxic:

Toxic

CAS Number:

7446-11-9

Prevention Program Level 3 ID:

1000033687

NAICS Code:

325998

Safety Information

Safety Review Date (The date on which the safety information was last reviewed or revised):

13-Mar-2012

Process Hazard Analysis (PHA)

PHA Completion Date (Date of last PHA or PHA

28-Mar-2009

update):

The Technique Used

What If:

Yes

Checklist:

What If/Checklist:

HAZOP:

Yes

Failure Mode and Effects Analysis:

Fault Tree Analysis:

Other Technique Used:

LOPA

PHA Change Completion Date (The expected or actual date of completion of all changes resulting from last PHA or PHA update): 27-May-2009

Major Hazards Identified

Toxic Release:

Yes

Fire:

Explosion:

Overfilling:

Runaway Reaction:

Polymerization:

Overpressurization: Corrosion:

Yes Yes Yes

Yes

Contamination: Equipment Failure:

Yes

Loss of Cooling, Heating, Electricity, Instrument Air:

Earthquake:

Floods (Flood Plain):

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983 Plan Sequence Number: 1000031578 Yes Tornado: Hurricanes: Yes Other Major Hazard Identified: Process Controls in Use Vents: Yes Relief Valves: Yes Check Valves: Yes Scrubbers: Yes Flares: Manual Shutoffs: Yes Automatic Shutoffs: Yes Interlocks: Yes Alarms and Procedures: Yes Keyed Bypass: Yes Emergency Air Supply: Yes **Emergency Power:** Yes Backup Pump: Yes Grounding Equipment: Yes Inhibitor Addition: Rupture Disks: Yes Excess Flow Device: Quench System: Purge System: None: Other Process Control in Use: Mitigation Systems in Use Sprinkler System: Dikes: Fire Walls: Blast Walls: Deluge System: Water Curtain: Enclosure: Yes Neutralization: None: Other Mitigation System in Use: **Building Vent Scrubber** Monitoring/Detection Systems in Use Process Area Detectors: Yes Perimeter Monitors: None: Other Monitoring/Detection System in Use:

Changes Since Last PHA Update

Reduction in Chemical Inventory: Increase in Chemical Inventory:

Change Process Parameters:

Installation of Process Controls:

Yes

Installation of Process Detection Systems:

Plan Sequence Number: 1000031578

Installation of Perimeter Monitoring Systems:

Installation of Mitigation Systems:

None Recommended:

None:

Other Changes Since Last PHA or PHA Update:

Review of Operating Procedures

Operating Procedures Revision Date (The date of the most recent review or revision of operating procedures): 08-Nov-2012

Training

Training Revision Date (The date of the most recent 05-Nov-2012 review or revision of training programs):

The Type of Training Provided

Classroom:

Yes

On the Job:

Yes

Other Training:

The Type of Competency Testing Used

Written Tests:

Yes

Oral Tests:

Yes

Demonstration:

Yes Yes

Observation:
Other Type of Competency Testing Used:

Maintenance

Maintenance Procedures Revision Date (The date of 21-Sep-2012 the most recent review or revision of maintenance procedures):

Equipment Inspection Date (The date of the most recent equipment inspection or test):

08-Oct-2012

Equipment Tested (Equipment most recently inspected or tested):

SO3 Evaporator

Management of Change

Change Management Date (The date of the most recent change that triggered management of change procedures):

02-Oct-2012

Change Management Revision Date (The date of the most recent review or revision of management of change procedures):

Pre-Startup Review

Plan Sequence Number: 1000031578

Pre-Startup Review Date (The date of the most recent pre-startup review):

18-Oct-2012

Compliance Audits

Compliance Audit Date (The date of the most recent 31-Dec-2013 compliance audit):

Compliance Audit Change Completion Date (Expected or actual date of completion of all changes resulting from the compliance audit):

03-Sep-2012

Incident Investigation

Incident Investigation Date (The date of the most recent incident investigation (if any)):

Incident Investigation Change Date (The expected or actual date of completion of all changes resulting from the investigation):

25-Apr-2012 25-Apr-2012

Employee Participation Plans

Participation Plan Revision Date (The date of the most recent review or revision of employee participation plans):

13-Apr-2012

Hot Work Permit Procedures

Hot Work permit Review Date (The date of the most 23-Oct-2012 recent review or revision of hot work permit procedures):

Contractor Safety Procedures

Contractor Safety Procedures Review Date (The date of the most recent review or revision of contractor safety procedures):

06-Sep-2012

Contractor Safety Performance Evaluation Date (The date of the most recent review or revision of contractor safety performance):

31-Oct-2012

Confidential Business Information

CBI Claimed:

Description

Regen 2 Unit - Oleum

Program Level 3 Prevention Program Chemicals

Prevention Program Chemical ID:

1000039877

Facility Name: Rhodia, Houston Plant
EPA Facility Identifier: 1000 0008 2983

Plan Sequence Number: 1000031578

Chemical Name:

Oleum (Fuming Sulfuric acid) [Sulfuric acid, mixture

with sulfur trioxide]

Flammable/Toxic: CAS Number:

Toxic 8014-95-7

Prevention Program Level 3 ID:

NAICS Code:

1000033689

325188

Safety Information

Safety Review Date (The date on which the safety information was last reviewed or revised):

01-Mar-2012

Process Hazard Analysis (PHA)

PHA Completion Date (Date of last PHA or PHA

update):

06-Jan-2009

The Technique Used

What If:

Checklist:

What If/Checklist:

HAZOP:

Yes

Failure Mode and Effects Analysis:

Fault Tree Analysis:

Other Technique Used:

LOPA

PHA Change Completion Date (The expected or actual date of completion of all changes resulting from last PHA or PHA update):

31-May-2013

Major Hazards Identified

Toxic Release:

Yes

Fire:

Yes

Explosion:

Yes

Runaway Reaction:

Polymerization: Overpressurization:

Yes

Corrosion:

Yes

Overfilling:

Yes

Contamination:

Yes

Yes

Equipment Failure:

Loss of Cooling, Heating, Electricity, Instrument Air: Yes

Earthquake:

Floods (Flood Plain):

Tornado:

Hurricanes:

Yes

Other Major Hazard Identified:

Process Controls in Use

Vents:

Yes

Relief Valves:

Yes

Check Valves:

Data displayed is accurate as of 12:00 AM (EDT) Wednesday, April 17, 2013

	Name: Rhodia, Houston Plant cility Identifier: 1000 0008 2983		Plan Sequence Number: 1000031578
	Scrubbers:	Yes	
	Flares:		
	Manual Shutoffs:	Yes	
	Automatic Shutoffs:	Yes	
	Interlocks:	Yes	
	Alarms and Procedures:	Yes	
	Keyed Bypass:	Yes	
	Emergency Air Supply:	Yes	
	Emergency Power:	Yes	
	Backup Pump:	Yes	
	Grounding Equipment:	Yes	
	Inhibitor Addition:		
	Rupture Disks:	Yes	
	Excess Flow Device:		
	Quench System:		
	Purge System:		
	None:		
	Other Process Control in Use:		
Mitiga	ition Systems in Use		
	Sprinkler System:		
	Dikes:		
	Fire Walls:		
	Blast Walls:		
	Deluge System:		
	Water Curtain:		
	Enclosure:		
	Neutralization:	Yes	
	None:		
	Other Mitigation System in Use:	Trench System	
Monite	oring/Detection Systems in Use		
	g 24,24,21,12 202		
	Process Area Detectors:		
	Perimeter Monitors:	Yes	
	None:		
	Other Monitoring/Detection System in Use:		
Chang	ges Since Last PHA Update		
	Reduction in Chemical Inventory:		
	Increase in Chemical Inventory:		
	Change Process Parameters:		
	Installation of Process Controls:		
	matanauon or i 100033 Controls.		

Installation of Process Detection Systems:

Installation of Perimeter Monitoring Systems:

Installation of Mitigation Systems:

None Recommended:

None:

Yes

Other Changes Since Last PHA or PHA Update:

Review of Operating Procedures

Plan Sequence Number: 1000031578

Operating Procedures Revision Date (The date of the most recent review or revision of operating

the most recent review or revision of opprocedures):

.

08-Nov-2012

Training

Training Revision Date (The date of the most recent 04-Sep-2012 review or revision of training programs):

The Type of Training Provided

Classroom:

Yes Yes

On the Job: Other Training:

The Type of Competency Testing Used

Written Tests:

Oral Tests:

Demonstration:

Yes Yes

Observation:

Other Type of Competency Testing Used:

Maintenance

Maintenance Procedures Revision Date (The date of 27-Jan-2012 the most recent review or revision of maintenance procedures):

Equipment Inspection Date (The date of the most recent equipment inspection or test):

15-Feb-2012

Equipment Tested (Equipment most recently inspected or tested):

Oleum Tower Internal Inspection

Management of Change

Change Management Date (The date of the most recent change that triggered management of change procedures):

12-Jun-2012

Change Management Revision Date (The date of the most recent review or revision of management of change procedures):

17-Apr-2012

Pre-Startup Review

Pre-Startup Review Date (The date of the most recent pre-startup review):

17-Jan-2011

Compliance Audits

Compliance Audit Date (The date of the most recent 31-Dec-2013 compliance audit):

Compliance Audit Change Completion Date (Expected or actual date of completion of all changes resulting from the compliance audit):

03-Sep-2012

Incident Investigation

Incident Investigation Date (The date of the most recent incident investigation (if any)):

01-Apr-2011

Incident Investigation Change Date (The expected or actual date of completion of all changes resulting from the investigation):

01-Apr-2011

Employee Participation Plans

Participation Plan Revision Date (The date of the most recent review or revision of employee participation plans):

13-Apr-2012

Hot Work Permit Procedures

Hot Work permit Review Date (The date of the most 23-Oct-2012 recent review or revision of hot work permit procedures):

Contractor Safety Procedures

Contractor Safety Procedures Review Date (The date of the most recent review or revision of contractor safety procedures):

06-Sep-2012

Contractor Safety Performance Evaluation Date (The date of the most recent review or revision of contractor safety performance):

31-Oct-2012

Confidential Business Information

CBI Claimed:

Description

No. 8 Unit - Oleum

Program Level 3 Prevention Program Chemicals

Prevention Program Chemical ID:

1000039879

Chemical Name:

Oleum (Fuming Sulfuric acid) [Sulfuric acid, mixture

with sulfur trioxide)

Flammable/Toxic:

Toxic

CAS Number:

8014-95-7

Prevention Program Level 3 ID:

1000033690

NAICS Code:

325188

Safety Information

Safety Review Date (The date on which the safety information was last reviewed or revised):

Process Hazard Analysis (PHA)

PHA Completion Date (Date of last PHA or PHA update):

19-May-2011

30-Mar-2012

The Technique Used

What If:

Checklist:

What If/Checklist:

HAZOP:

Yes

Failure Mode and Effects Analysis:

Fault Tree Analysis:

Other Technique Used:

LOPA

Yes

Yes

PHA Change Completion Date (The expected or actual date of completion of all changes resulting from last PHA or PHA update):

05-Sep-2012

Major Hazards Identified

Toxic Release:

Fire: Yes

Explosion:

Runaway Reaction:

Polymerization:

Overpressurization: Yes Corrosion: Yes Overfilling: Yes Contamination: Yes Equipment Failure: Yes

Loss of Cooling, Heating, Electricity, Instrument Air:

Earthquake:

Floods (Flood Plain):

Tornado:

Hurricanes:

Other Major Hazard Identified:

Process Controls in Use

Vents: Yes Relief Valves: Yes

Check Valves: Yes Scrubbers: Yes

Flares:

Manual Shutoffs: Yes Automatic Shutoffs: Yes Interlocks: Yes Alarms and Procedures: Yes

Keyed Bypass:

Emergency Air Supply:

-	e: Rhodia, Houston Plant Identifier: 1000 0008 2983	Plan Sequence Number: 1000031578
	Emergency Power:	
	Backup Pump:	
	Grounding Equipment:	Yes
	Inhibitor Addition:	
	Rupture Disks:	
	Excess Flow Device:	
	Quench System:	
	Purge System:	
	None:	
	Other Process Control in Use:	
Mitigation	n Systems in Use	
	Sprinkter System:	
	Dikes:	
	Fire Walls:	
	Blast Walls:	
	Deluge System:	
	Water Curtain:	
	Enclosure:	
	Neutralization:	Yes
	None:	163
	Other Mitigation System in Use:	
Monitorin	g/Detection Systems in Use	
	Process Area Detectors:	
	Perimeter Monitors:	
	None:	Yes
	Other Monitoring/Detection System in Use:	
Changes	Since Last PHA Update	
	Reduction in Chemical Inventory:	
	Increase in Chemical Inventory:	
	Change Process Parameters:	
	Installation of Process Controls:	
	Installation of Process Detection Systems:	
	Installation of Perimeter Monitoring Systems:	
	Installation of Mitigation Systems:	
	None Recommended:	
	None:	Dayland dayna tawan 40/45/40
	Other Changes Since Last PHA or PHA Update:	Replaced oleum tower 10/15/12
Review o	f Operating Procedures	
	Operating Procedures Revision Date (The date of the most recent review or revision of operating procedures):	08-Nov-2012
Training		
Hairing		
	Training Revision Date (The date of the most recent review or revision of training programs):	05-Nov-2012

Plan Sequence Number: 1000031578

The Type of Training Provided

Classroom:

Yes

On the Job:

Yes

Other Training:

The Type of Competency Testing Used

Written Tests:

Yes

Oral Tests:

Yes

Demonstration:

Yes

Observation:

Yes

Other Type of Competency Testing Used:

Maintenance

Maintenance Procedures Revision Date (The date of 27-Sep-2012 the most recent review or revision of maintenance procedures):

Equipment Inspection Date (The date of the most recent equipment inspection or test):

29-Oct-2012

Equipment Tested (Equipment most recently inspected or tested):

Oleum ClL exchanger

Management of Change

Change Management Date (The date of the most recent change that triggered management of change procedures):

12-Oct-2012

Change Management Revision Date (The date of the most recent review or revision of management of change procedures):

17-Apr-2012

Pre-Startup Review

Pre-Startup Review Date (The date of the most recent pre-startup review):

11-Oct-2012

Compliance Audits

Compliance Audit Date (The date of the most recent 31-Dec-2013 compliance audit):

Compliance Audit Change Completion Date (Expected or actual date of completion of all changes resulting from the compliance audit):

03-Sep-2012

Incident Investigation

Plan Sequence Number: 1000031578

Incident Investigation Date (The date of the most recent incident investigation (if any)):

Incident Investigation Change Date (The expected or actual date of completion of all changes resulting from the investigation):

04-Jun-2012 31-Dec-2013

Employee Participation Plans

Participation Plan Revision Date (The date of the most recent review or revision of employee participation plans):

13-Apr-2012

Hot Work Permit Procedures

Hot Work permit Review Date (The date of the most 23-Oct-2012 recent review or revision of hot work permit procedures):

Contractor Safety Procedures

Contractor Safety Procedures Review Date (The date of the most recent review or revision of contractor safety procedures):

06-Apr-2012

Contractor Safety Performance Evaluation Date (The date of the most recent review or revision of contractor safety performance):

31-Oct-2012

Confidential Business Information

CBI Claimed:

Description

Logisitics - Oleum

Program Level 3 Prevention Program Chemicals

Prevention Program Chemical ID:

1000039880

Chemical Name:

Oleum (Furning Sulfuric acid) [Sulfuric acid, mixture

with sulfur trioxide]

Flammable/Toxic:

CAS Number:

Toxic

8014-95-7

Prevention Program Level 3 ID:

1000033691

NAICS Code:

325188

Safety Information

Safety Review Date (The date on which the safety information was last reviewed or revised):

02-May-2012

Process Hazard Analysis (PHA)

Plan Sequence Number: 1000031578

PHA Completion Date (Date of last PHA or PHA

03-Mar-2011

The Technique Used

What If:

Checklist:

What If/Checklist:

HAZOP:

Yes

Failure Mode and Effects Analysis:

Fault Tree Analysis:

Other Technique Used:

LOPA

03-Mar-2014

PHA Change Completion Date (The expected or actual date of completion of all changes resulting from last PHA or PHA update):

Major Hazards Identified

Toxic Release:

Yes

Fire:

Explosion:

Runaway Reaction:

Polymerization:

Overpressurization:

Yes Yes

Corrosion: Overfilling:

Yes

Contamination:

Yes Yes

Equipment Failure: Loss of Cooling, Heating, Electricity, Instrument Air:

Earthquake:

Floods (Flood Plain):

Tornado:

Hurricanes:

Yes

Other Major Hazard Identified:

Process Controls in Use

Vents:

Yes

Relief Valves:

Yes Yes

Check Valves:

Scrubbers: Flares:

Yes

Manual Shutoffs:

Yes

Automatic Shutoffs:

Yes

Interlocks:

Yes

Alarms and Procedures:

Yes

Keyed Bypass:

Emergency Air Supply:

Yes

Emergency Power:

Yes

Backup Pump:

Grounding Equipment: Inhibitor Addition:

Yes

Rupture Disks:

Yes

Excess Flow Device:

Quench System:

Facility Name: Rhodia, Houston Plant	Plan Coguanas Number 1000024579
EPA Facility Identifier: 1000 0008 2983	Plan Sequence Number: 1000031578
Purge System: None:	
Other Process Control in Use:	
Mitigation Systems in Use	
Sprinkler System:	
Dikes:	Yes
Fire Walls:	
Blast Walls:	
Deluge System:	
Water Curtain:	
Enclosure:	
Neutralization:	
None:	
Other Mitigation System in Use:	
Monitoring/Detection Systems in Use	
Process Area Detectors:	
Perimeter Monitors:	
None:	Yes
Other Monitoring/Detection System in Use:	
Changes Since Last PHA Update	
Reduction in Chemical Inventory:	
Increase in Chemical Inventory:	Yes
Change Process Parameters:	
Installation of Process Controls:	
Installation of Process Detection Systems:	
Installation of Perimeter Monitoring Systems:	
Installation of Mitigation Systems:	
None Recommended:	
None:	
Other Changes Since Last PHA or PHA Update:	
Review of Operating Procedures	
Operating Procedures Revision Date (The date of the most recent review or revision of operating procedures):	17-Oct-2012

Training

Training Revision Date (The date of the most recent 03-Jan-2011 review or revision of training programs):

The Type of Training Provided

Classroom:

Yes

On the Job:

Yes

Other Training:

The Type of Competency Testing Used

Written Tests:

Yes

Oral Tests:

Yes

Demonstration:

Yes

Observation:

Yes

Other Type of Competency Testing Used:

Maintenance

Maintenance Procedures Revision Date (The date of 20-Apr-2012 the most recent review or revision of maintenance procedures):

Equipment Inspection Date (The date of the most recent equipment inspection or test):

20-Sep-2012

Equipment Tested (Equipment most recently inspected or tested):

Oleum Tank 15 pump

Management of Change

Change Management Date (The date of the most recent change that triggered management of change procedures):

06-Sep-2012

Change Management Revision Date (The date of the most recent review or revision of management of change procedures):

17-Apr-2012

Pre-Startup Review

Pre-Startup Review Date (The date of the most recent pre-startup review):

06-Sep-2012

Compliance Audits

Compliance Audit Date (The date of the most recent 31-Dec-2013 compliance audit):

Compliance Audit Change Completion Date (Expected or actual date of completion of all changes resulting from the compliance audit):

03-Sep-2012

Incident Investigation

Incident Investigation Date (The date of the most recent incident investigation (if any)):

11-Oct-2012

Incident Investigation Change Date (The expected or actual date of completion of all changes resulting from the investigation):

29-Mar-2013

Employee Participation Plans

Plan Sequence Number: 1000031578

Participation Plan Revision Date (The date of the most recent review or revision of employee participation plans):

13-Apr-2012

Hot Work Permit Procedures

Hot Work permit Review Date (The date of the most 23-Oct-2012 recent review or revision of hot work permit procedures):

Contractor Safety Procedures

Contractor Safety Procedures Review Date (The date of the most recent review or revision of contractor safety procedures):

06-Sep-2012

Contractor Safety Performance Evaluation Date (The date of the most recent review or revision of contractor safety performance):

26-Sep-2012

Confidential Business Information

CBI Claimed:

Description

Hazardous Waste Treatment Services - Multiple Chemicals

Program Level 3 Prevention Program Chemicals

Prevention Program Chemical ID:

1000039885

Chemical Name:

Propionitrile [Propanenitrile]

Flammable/Toxic:

Toxic

CAS Number:

107-12-0

Prevention Program Level 3 ID:

1000033692

NAICS Code:

325188

Safety Information

Safety Review Date (The date on which the safety information was last reviewed or revised):

01-Nov-2012

Process Hazard Analysis (PHA)

PHA Completion Date (Date of last PHA or PHA update):

18-Oct-2010

The Technique Used

What If:

Checklist:

Plan Sequence Number: 1000031578

What If/Checklist:

HAZOP:

Yes

Failure Mode and Effects Analysis:

Fault Tree Analysis:

Other Technique Used:

PHA Change Completion Date (The expected or actual date of completion of all changes resulting from last PHA or PHA update):

LOPA

29-Mar-2013

Major Hazards Identified

Toxic Release:

Yes

Fire:

Yes

Explosion:

Yes

Runaway Reaction:

Yes

Polymerization:

Yes

Overpressurization:

Yes

Corrosion: Overfilling: Yes

Contamination:

Yes

Yes

Equipment Failure:

Yes

Loss of Cooling, Heating, Electricity, Instrument Air:

Yes

Earthquake:

Floods (Flood Plain):

Tornado:

Hurricanes:

Yes

Other Major Hazard Identified:

Process Controls in Use

Vents:

Flares:

Yes

Relief Valves:

Yes

Check Valves:

Yes

Scrubbers:

Yes Yes

Manual Shutoffs:

Yes

Automatic Shutoffs:

Yes

Interlocks: Alarms and Procedures:

Yes

Keyed Bypass:

Emergency Air Supply:

Yes

Emergency Power:

Backup Pump:

Grounding Equipment:

Yes

Inhibitor Addition:

Rupture Disks:

Excess Flow Device:

Quench System:

Yes

Purge System:

None:

Other Process Control in Use:

Mitigation Systems in Use

Sprinkler System:

Yes

Dikes:

Yes

-	le: Rhodia, Houston Plant Identifier: 1000 0008 2983		Plan Sequence Number: 1000031578
	Fire Walls:		
	Blast Walls:		
	Deluge System:		
	Water Curtain:		
	Enclosure: Neutralization:		
	None:		
	Other Mitigation System in Use:	Flare	
Monitorir	ng/Detection Systems in Use		
	Process Area Detectors:	Yes	
	Perimeter Monitors:		
	None:		
	Other Monitoring/Detection System in Use:		
Changes	Since Last PHA Update		
	Reduction in Chemical Inventory:		
	Increase in Chemical Inventory:	Yes	
	Change Process Parameters:		
	Installation of Process Controls:	Yes	
	Installation of Process Detection Systems:		
	Installation of Perimeter Monitoring Systems:		
	Installation of Mitigation Systems:		
	None Recommended:		
	None: Other Changes Since Last PHA or PHA Update:		
	Other Changes Since East FITA of FITA Opuate.	1,	
Review o	of Operating Procedures		
	Operating Procedures Revision Date (The date of the most recent review or revision of operating procedures):	13-Sep-2012	
Training			
	Training Revision Date (The date of the most recent review or revision of training programs):	30-Oct-2012	
The Type	e of Training Provided	VALUE OF THE PARTY	
٠	Classroom:	Yes	
	On the Job:	Yes	

Other Training:

The Type of Competency Testing Used

Written Tests:

Yes

Oral Tests:

Yes

Demonstration:

Yes

Observation:

Yes

Other Type of Competency Testing Used:

Plan Sequence Number: 1000031578

Maintenance

Maintenance Procedures Revision Date (The date of 20-Apr-2012 the most recent review or revision of maintenance procedures):

Equipment Inspection Date (The date of the most recent equipment inspection or test):

07-Sep-2012

Equipment Tested (Equipment most recently inspected or tested):

Tank F-2 internal inspection

Management of Change

Change Management Date (The date of the most recent change that triggered management of change procedures):

13-Sep-2012

Change Management Revision Date (The date of the most recent review or revision of management of change procedures):

17-Apr-2012

Pre-Startup Review

Pre-Startup Review Date (The date of the most recent pre-startup review):

06-Nov-2012

Compliance Audits

Compliance Audit Date (The date of the most recent 31-Dec-2013 compliance audit):

Compliance Audit Change Completion Date (Expected or actual date of completion of all changes resulting from the compliance audit):

03-Sep-2012

Incident Investigation

Incident Investigation Date (The date of the most recent incident investigation (if any)):

27-Aug-2012

Incident Investigation Change Date (The expected or actual date of completion of all changes resulting from the investigation):

28-Aug-2012

Employee Participation Plans

Participation Plan Revision Date (The date of the most recent review or revision of employee participation plans):

13-Арг-2012

Hot Work Permit Procedures

Hot Work permit Review Date (The date of the most 23-Oct-2012 recent review or revision of hot work permit procedures):

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983

Plan Sequence Number: 1000031578

Contractor Safety Procedures

Contractor Safety Procedures Review Date (The date of the most recent review or revision of contractor safety procedures):

06-Sep-2012

Contractor Safety Performance Evaluation Date (The date of the most recent review or revision of contractor safety performance):

10-Jul-2012

Confidential Business Information

CBI Claimed:

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983

Plan Sequence Number: 1000031578

Section 8. Program Level 2

Section 9. Emergency Response

Written Emergency Response (ER) Plan

Community Plan (Is facility included in written community emergency response plan?):

Yes

Facility Plan (Does facility have its own written emergency response plan?):

Yes

Response Actions (Does ER plan include specific actions to be taken in response to accidental releases of regulated substance(s)?):

Yes

Public Information (Does ER plan include procedures for informing the public and local agencies responding to accidental release?): Yes

Healthcare (Does facility's ER plan include information on emergency health care?):

Yes

Emergency Response Review

Review Date (Date of most recent review or update 02-Nov-2010 of facility's ER plan):

Emergency Response Training

Training Date (Date of most recent review or update 30-Oct-2012 of facility's employees):

Local Agency

Agency Name (Name of local agency with which the Channel Industries Mutual Aid Org. facility ER plan or response activities are

coordinated): Agency Phone Number (Phone number of local agency with which the facility ER plan or response

(281) 474-8028

Subject to

OSHA Regulations at 29 CFR 1910.38:

Yes

OSHA Regulations at 29 CFR 1910.120:

Yes

Clean Water Regulations at 40 CFR 112:

Yes

RCRA Regulations at CFR 264, 265, and 279.52:

Yes

OPA 90 Regulations at 40 CFR 112, 33 CFR 154, 49 CFR 194, or 30 CFR 254:

Yes

State EPCRA Rules or Laws:

activities are coordinated):

Yes

Other (Specify):

Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983

Executive Summary

General Executive Summary for Risk Management Plan at the Rhodia, Houston facility.

Date of plan: 11/07/12

Rev. 0

1. Accidental Release Prevention and Emergency Response Policies

The Houston plant is strongly committed to employee, public and environmental safety. This commitment is demonstrated in the comprehensive accidental release prevention program that covers areas such as design, installation, operating procedures, maintenance, and employee training associated with the processes at the Houston plant. It is Houston plant policy to implement appropriate controls to prevent possible releases of regulated substances.

2. The Stationary Source and the Regulated Substances Handled

The Houston plant's primary activities encompass Chemical Manufacture, due to which regulated substances could be stored and/or handled on site. These substances include Oleum (Fuming Sulfuric acid), Sulfur Trioxide (liquefied), Carbon Disulfide, Vinyl Acetate, Toluene Di-isocyanate, Propionitrile, Acrylonitrile, Methyl Mercaptan, Ethyl Mercaptan, Acetaldehyde, Allyl Alcohol, Propylene Oxide, Hydrazine, Hydrogen Sulfide, Isopropylamine, 1-Butene, Propylene, Cis Butene-2, Trans Butene-2, Isobutylene, 1,3 Butadiene, Isopentane, Ethyl Chloride, Dimethylamine, Ethylamine, Methylamine, Trimethylamine, and Propane. Oleum (Fuming Sulfuric acid) is used as a chemical intermediate, as a drying agent and is a raw material for dyes and detergents. Sulfur trioxide is used as an intermediate in the production of high purity sulfuric acid for use in the electronics industry. Carbon Disulfide, Vinyl Acetate, Toluene Di-isocyanate, Propionitrile, Acrylonitrile, Methyl Mercaptan, Ethyl Mercaptan, Acetaldehyde, Allyl Alcohol, Propylene Oxide, Hydrazine, Hydrogen Sulfide, Isopropylamine, 1-Butene, Propylene, Cis Butene-2, Trans Butene-2, Isobutylene, 1,3 Butadiene, Isopentane, Ethyl Chloride, Dimethylamine, Ethylamine, Methylamine, Trimethylamine, and Propane could be received as waste streams for energy recovery and raw material value.

3. The General Accidental Release Prevention Program and the Chemical-Specific Prevention Steps The Houston plant has taken all the necessary steps to comply with the accidental release prevention requirements set out under 40 CFR part 68 of the EPA. The following sections briefly describe the elements of the release prevention program that is in place at the Houston plant.

Process Safety Information

Houston Plant maintains a detailed record of safety information that describes the chemical hazards, operating parameters and equipment designs associated with all processes.

Process Hazard Analysis (PHA)

The Houston plant conducts comprehensive studies to ensure that hazards associated with our processes are identified and controlled efficiently. The methodology used to carry out these analyses is Checklist, What If/Checklist (combined), HAZOP (Hazard and Operability), Fault Tree and LOPA (Layer of Protection Analysis). The studies are undertaken by a team of qualified personnel with expertise in engineering and process operations and are revalidated at a regular interval of five years. Any findings related to the hazard analysis are addressed in a timely manner.

Operating Procedures

For the purposes of safely conducting activities within the Houston plant covered processes, the plant maintains written operating procedures. These procedures address various modes of operation such as initial startup, normal operations, temporary operations, emergency shutdown, emergency operations, normal shutdown and startup after a turnaround. The information is regularly reviewed and is readily accessible to operators involved in the processes.

Training

The Houston Plant has a comprehensive training program in place to ensure that employees who are operating processes are competent in the operating procedures associated with these processes. Refresher training is provided at least every three years and more frequently as needed.

Mechanical Integrity

Houston Plant carries out maintenance checks on process equipment to ensure proper operations. Process equipment examined

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by these checks includes among others; pressure vessels, storage tanks, piping systems, relief and vent systems, emergency shutdown systems, controls and pumps. Maintenance operations are carried out by qualified personnel with previous training in maintenance practices. Furthermore, these personnel are offered specialized training as needed. Any equipment deficiencies identified by the maintenance checks are corrected in a safe and timely manner.

Management of Change

Written procedures are in place at Houston Plant to manage changes in process chemicals, technology, equipment and procedures. Process operators, maintenance personnel or any other employee whose job tasks are affected by a modification in process conditions are promptly made aware of and offered training to deal with the modification.

Pre-startup Reviews

Pre-start up safety reviews related to new processes and to modifications in established processes are conducted as a regular practice at the Houston Plant. These reviews are conducted to confirm that construction, equipment, operating and maintenance procedures are suitable for safe startup prior to placing equipment into operation.

Compliance Audits

The Houston Plant conducts audits on a regular basis to determine whether the provisions set out under the RMP rule are being implemented. These audits are carried out at least every 3 years and any corrective actions required as a result of the audits are undertaken in a safe and prompt manner.

Incident Investigation

The Houston Plant promptly investigates any incident that has resulted in, or could reasonably result in a catastrophic release of a regulated substance. These investigations are undertaken to identify the situation leading to the incident as well as any corrective actions to prevent the release from reoccurring. All reports are retained for a minimum of 5 years.

Employee Participation

The Houston Plant truly believes that process safety management and accident prevention is a team effort. Company employees are strongly encouraged to express their views concerning accident prevention issues and to recommend improvements. In addition, our employees have access to all information created as part of the facility's implementation of the RMP rule, including information resulting from process hazard analyses in particular.

Contractors

On occasion, the Houston plant hires contractors to conduct specialized maintenance and construction activities. Prior to selecting a contractor, a thorough evaluation of safety performance of the contractor is carried out. Houston Plant has a strict policy of informing the contractors of known potential hazards related the contractor's work and the processes. Contractors are also informed of all the procedures for emergency response should an accidental release of a regulated substance occur.

4. Five-year Accident History

Rhodia, Houston Plant has had an excellent record of preventing accidental releases. Due to the Houston plant's stringent release prevention policies, only 2 accidental releases off-site have occurred over the last 5 years. The releases occurred on 06/09/2012 and involved 30% oleum and the release on 11/29/2008 involved 20% oleum. No deaths or injuries occurred offsite or onsite from these releases.

5. Emergency Response Plan

Houston Plant maintains a written emergency response plan to deal with accidental releases of hazardous materials. The plan includes all aspects of emergency response including adequate first aid and medical treatment, evacuations, notification of local emergency response agencies and the public, as well as post-incident decontamination of affected areas. To ensure proper functioning, emergency response equipment is regularly inspected and serviced. In addition, the plan is promptly updated to reflect any pertinent changes taking place within our processes that would require a modified emergency response.

6. Planned Changes to Improve Safety

In order to encourage continuous improvement in all elements of Process Safety at the Houston plant reports to all employees on the progress of improvement efforts that are described in the Process Safety Management Plan. Many of these improvements are Facility Name: Rhodia, Houston Plant EPA Facility Identifier: 1000 0008 2983

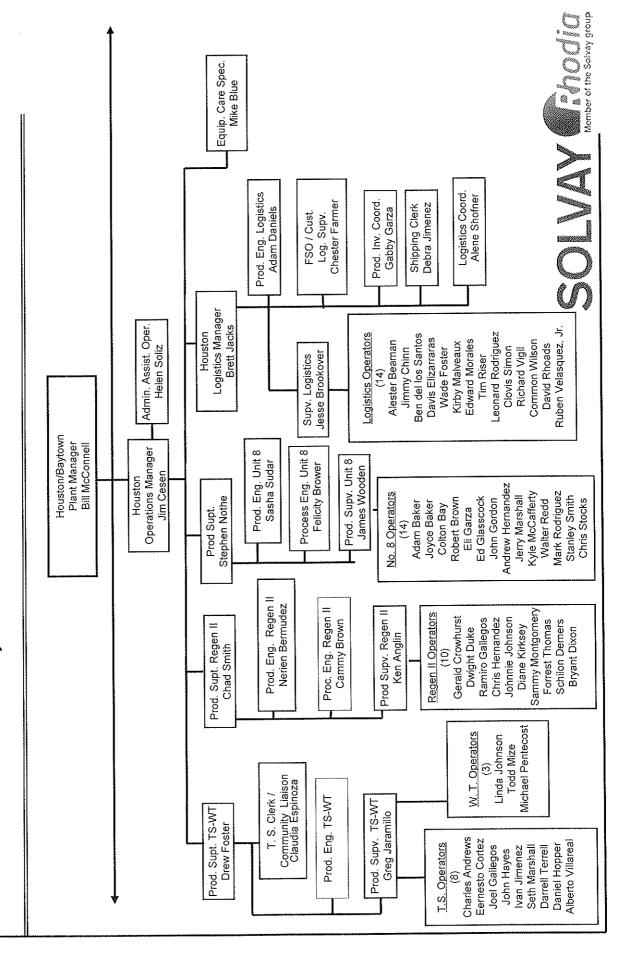
Plan Sequence Number: 1000031578

results of audits and other reviews such as Management of Change, Process Hazard Analysis, Accident Investigations and others.

Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5. Operator Training Records
- 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

HOUSTON, TEXAS



Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- (4.) Operating Procedures and Certifications
 - 5. Operator Training Records
 - 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)



Houston Plant EcoServices

Feeding T-18 acid onto Oleum Tower

Procedure No: HO-UNIT8-SOP012-UNIT8

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The purpose of this procedure is to feed T-18 onto Oleum Tower

2.0 Scope:

This procedure applies to Unit 8 Oleum tower

3.0 Responsibility:

The #8 Unit Superintendent is responsible for maintaining this form.

4.0 References:

N/A

5.0 Definitions:

N/A

Special Safety and Health Considerations or Unique Hazards:	MSDS Information
PPE Information:	Per PPE Matrix

		1	
Steps	Action	Reasons and Key Points to Watch For	,

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Effective Date: 04/17/2002	Author: Matt Butler	Approved By: Supt

1. Check Oleum concentration	Sample and check desired acid concentration	
2. Prepare process lineup	Line up the oleum feed to tower from A or D Pump south of Tank 31 through operator feed line	Coordinate with Logistics
3.	Line up the oleum feed to storage with the bypass valve completely open.	In this particular application, the control valve is for trim only.
4.	Verify cooling water is flowing through CIL cooler	Oleum pressure must always be greater than water pressure
5.	ADJUST gas valve (Valve #1) on the Absorbing tower .	Get pressure drop reading at the tower base. By feeding 18 tank will require less gas pressure. Monitor temperature on absorbing tower
6.	Verify that the controllers in the Control room are controlling the oleum level in the tower and the acid concentration.	Check gauges and level indicators. Along with the oleum analyzer.
7.	When temperatures are in range and analyzer is reading at desired strength. Pull sample.	Carry sample to lab in an approved sample carrying case to confirm analyzer reliability.
8. Secure process	When T-18 reaches 5' innage, secure pumps and change valve alignment	

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

3	Λ	Re	eco	rd	c.
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N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

03/07/2002

Version No.: HO-UNIT8-SOP012-UNIT8	Version Date: 03/07/2012	Page No.; 2 of 3
Effective Date: 04/17/2002	Author: Matt Butler	Approved By: Supt

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Effective Date: 04/17/2002	Author: Matt Butler	Approved By: Supt



Oleum Tower Recirculation Pump Startup

Procedure No: 20N 275.01

1.0 Purpose:

The purpose of this procedure is to describe steps for the normal startup of the Regen 2 Oleum Tower recirculation pump in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of starting the Regen 2 Oleum Tower recirculation pump.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

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N/A

5.0 Definitions:

N/A

Special Safety and Health Considerations or Unique Hazards:	MSDS Information		
PPE Information:	Per PPE Matrix		
	3.0 Reporting		

Steps	Action	Reasons and Key Points to Watch For
1. Pre-Startup	a. Check to make sure the main	
~	breaker to the pump is in the	4.7
	"ON" position	
	b. Check the level in the oleum	LT-1272 must be 5-5.5'
	pump tank	
	c. Open the 8" recycle valve	
	approximately two turns	
	d. Close the 2" acid drain valves	
	on the Oleum Tower CIL	¥
	e. Open the 12" acid valve to the	
	exit of the Oleum Tower CIL	
2. Recirculating Pump	Start the recirculating pump,	
	P-275	

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Effective Date:10-24-2012	Author: Cammy Brown	Approved By: Chad Smith	

3. Cooling Water	a. Close the 2" water drain	Control the acid temperature by bypassing
J. Cooming Water	valves on the Oleum Tower CIL	acid around the cooler.
	b. Open the 24" water inlet and	dela di odila die coolei.
		Maintain an arid autlat tammanatura of 120
	outlet valves to the Oleum	Maintain an acid outlet temperature of 120-
	Tower CIL	130°F.
	c. Make sure that one of the	The second
	cooling tower pumps (P-282A	Refer to SOP 20N 233.01 for starting the
	or P-282B) is running	Oleum Tower CIL.
4. Cross-Feed Pumps	a. Start one of the Oleum Tower	
	cross-feed pumps (P-276A or P-	
·	276B)	
	b. Line up the flow of the cross-	
	feed pump to AI-1291	
5. Final Check	a. Check valve alignment	
	b. Maintain the proper Oleum	
	Tower level	p = ==================================
	c. Check for leaks, noises, or	
	excessive vibrations	

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Brent Evans 09-15-2011

Version No.: Oleum Tower Recirc Pump Startup	Version Date: 10-24-2012	Page No.: 2 of 2	
Effective Date:10-24-2012	Author: Cammy Brown	Approved By: Chad Smith	



Oleum Tower Cross-Feed Pump Switching

Procedure No: 20N 231.03

1.0 Purpose:

The purpose of this procedure is to describe the steps for switching the Oleum Tower cross-feed pumps in Regen 2 in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of switching the Oleum Tower cross-feed pumps.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

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N/A

5.0 Definitions:

N/A

Considerations or Unique Hazards:	
Hazards:	
PPE Information: Per PPE Matrix	

Steps	Action	Reasons and Key Points to Watch For
1. Spare Pump Valves	a. Fully open the suction valve to the spare pump (P276A or B – North or South) b. Fully open the discharge valve of the spare pump	
2. Start Pump	Press the start button on the	
	spare pump	

Version No.: Oleum Tower Cross-Feed Pump Switch	Version Date: 10-31-2012	Page No.: 1 of 1
Effective Date: 10-31-2012	Author: Cammy Brown	Approved By: Chad Smith

3. Shut Down In-	a. Close the discharge valve on	
Service Pump	the pump that is being shut	
	down	
	b. Press the stop button on the	
	pump that is being shutdown	
	c. Close the suction valve	
4. Final Check	a. Check all valves positions	
	b. Check that the out of service	
	pump is secured	
	c. Check for leaks, noise, or	
	excessive vibration	

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Cammy Brown 10-31-2012

Version No.: Oleum Tower Cross-Feed Pump Switch	Version Date: 10-31-2012	Page No.: 2 of 2
Effective Date: 10-31-2012	Author: Cammy Brown	Approved By: Chad Smith



Oleum Tower Start Up

Procedure No: 20N 231.01

1.0 Purpose:

The purpose of this procedure is to describe steps for the normal start up of the Regen 2 Oleum Tower, pumps and CIL in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of placing the Regen 2 Oleum Tower in service.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

4.0 References:

N/A

5.0 Definitions:

N/A

Special Safety and Health	MSDS Information
Considerations or Unique	
Hazards:	
PPE Information:	Per PPE Matrix

Steps	Action	Reasons and Key Points to Watch For
1. Fill Oleum Tower	Fill the Oleum Tower to a satisfactory level between 7' using 25-LI-1272, 25-LI-1272B, and 25-LI-1272C	Fill from T-77, from the 98% pump tank, or #8 oleum line to T-77. Filling 98% pump tank requires more time for the concentration to increase to 107% and corrosion will be greatly increased.
2. Position Valves	a. Position the acid valves to circulate the towerb. Open the 8" bypass valve approximately 2 turns (¼ open)	

Version No.: Oleum Tower Start Up	Version Date: 10-29-2012	Page No.: 1 of 3
Effective Date: 10-29-2012	Author: Cammy Brown	Approved By: Chad Smith

3. Recirculation Pump	a. Check to make sure the main breaker to the pump is in the "ON" position	
	b. Verify level in the oleum tower pump tank c. Close the 2" acid drain valves on the Oleum Tower CIL d. Open the 12" acid chain valve to the exit of the Oleum Tower CIL e. Verify Nitrogen purge to seal is still turned on d. Start the recirculating pump, P-275	Pump Tank Level (25-LT-1272) must be 7'.
4. Cooling Water	a. Close the 2" water drain valves on the Oleum Tower CIL b. Open the 24" water inlet and outlet valves to the Oleum Tower CIL	Never bypass water to control temperature — only acid. Cooling Tower Fan(s) can be turned off to control cooling water temperature.
5. Oleum Tower CIL & Anatrol System	a. Verify 8" acid bypass valve alignmentb. Start the anatrol protection system	Control acid temperature by bypassing acid around the Oleum Tower CIL cooler. Maintain an acid outlet temperature of 120-130°F.
6. Oleum Analyzer Loop	a. Close the 1" drain valves on the oleum analyzer system b. Open the north and south oleum analyzer valves from the pumps to the analyzer c. Open the 4 valves around the analyzer loop d. Open the valve from the analyzer to the pump suction	
7. Cross-Feed Pumps	a. Open the suction and discharge valves 100% of the pump that is to be put in service (P-276A or B) b. Start one of the Oleum Tower cross-feed pumps (P-276A or B) c. Line up the flow of the cross-feed pump to 25-AI-1291	Notes: Keep an eye on 98% pump tank concentration. When the oleum samples are within concentration spec (106.9% - 107.1%), the valves can be opened to T-77.
8. Final Check	a. Check valve alignment b. Maintain the proper Oleum Tower level of 4-6' c. Check for leaks, noises, or excessive vibrations	Level will increase ~ 2-3' from runback if tower is shutdown.

Version No.: Oleum Tower Start Up	Version Date: 10-29-2012	Page No.: 2 of 3
Effective Date: 10-29-2012	Author: Cammy Brown	Approved By: Chad Smith

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Cammy Brown 10-29-2012



Oleum Tower Shutdown

Procedure No: 20N 231.02

1.0 Purpose:

The purpose of this procedure is to describe steps for the normal shutdown of the Regen 2 Oleum Tower in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of taking the Regen 2 Oleum Tower out of service.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

4.0 References:

N/A

5.0 Definitions:

N/A

Special Safety and Health	MSDS Information
Considerations or Unique	
Hazards:	
PPE Information:	Per PPE Matrix

Steps	Action	Reasons and Key Points to Watch For
1. Oleum Tower Level	Lower the level of the Oleum	The tower level should be approximately 4-
	Tower by putting LV-1272 into	5.5'. Tower run back will cause the level to
	manual with an output of 100%	rise 2-3'.
2. Oleum CIL Bypass	Open the 8" Oleum Tower CIL	
	cooler bypass valve halfway	
3. Control Valves	a. Fully close the control valve	
	on the Oleum line to T-77 (25-	
	LIC-1272)	
	b. Close the block valves on	Verify bypass valve around controller is
	both sides of the control valve	closed.
	c. Fully close the control valve	
	on the 98% feed to the Oleum	
	Tower (25-AIC-1271)	
	d. Close the block valves on	Verify bypass valve around controller is
	both sides of the control valve	closed.

Version No.: Oleum Tower Shutdown	Version Date: 10-31-2012	Page No.: 1 of 3
Effective Date: 10-31-2012	Author: Cammy Brown	Approved By: Chad Smith

4. Cross-Feed Pumps	a. Press the stop button located in the field for the pump that is in service (P-276A or B) b. Block in the suction and discharge valves of the pump c. Close the recirculation on the cross-feed discharge valve on	Prevents pump damage from running dry when the tower recirculation pump is stopped and spinning backwards. Prevents Oleum from going back to the tower when feeding from Tank 77.
	the discharge header back to the tower	tower when recently from rank 77.
5. Oleum Analyzer Loop	a. Close the north and south oleum analyzer valves from the pumps to the analyzer b. Close the 4 valves around the analyzer loop c. Close the valve from the analyzer to the pump suction	If system is to be drained - Open the 1" drain valves on the oleum analyzer system.
6. Recirculation Pump	Press the stop button located in the field to the recirculation pump	Leave the nitrogen purge on the seal.
7. Oleum Tower CIL & Anatrol System	a. Close the 12" acid chain valve from the CIL cooler to the tower b. Shut off the anatrol protection system	If system is to be drained - Open the 2" acid drain valves on the Oleum Tower CIL cooler.
8. Oleum Valves	a. Close the 6" product line valve going to the suction of the cross-feed pumps b. Fully close the control valve on the oleum to 98% pump tank line (25-FIC-1397) d. Close the oleum cross-feed block valves on top of the 93% and 98% pump tanks	If system is to be drained - Open the 3/4" expansion joint drain valves.
9. Cooling Water Valves	Close the 24" water inlet and outlet valves to the Oleum Tower CIL	If system is to be drained - Open the 2" water drain valves on the Oleum Tower CIL.
10. Final Check	a. Verify valve positions b. Check area for leaks	NOTE: Depending on the situation (oleum tower out of service due to turnaround, day shutdown, repairing leak in the system, etc.), a 98% flush may be required but this would be determined when the change is to be made. Discuss with supervisor.

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

Version No.; Oleum Tower Shutdown	Version Date: 10-31-2012	Page No.: 2 of 3
Effective Date: 10-31-2012	Author: Cammy Brown	Approved By: Chad Smith

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Brent Evans 09-16-2011 Cammy Brown 10-31-2012

Version No.: Oleum Tower Shutdown	Version Date: 10-31-2012	Page No.: 3 of 3
Effective Date: 10-31-2012	Author: Cammy Brown	Approved By: Chad Smith



Oleum Tower – Unplugging Equalizing Line

Procedure No: 20N 231.05

1.0 Purpose:

The purpose of this procedure is to describe steps to unplug the equalizing line of the Regen 2 Oleum Tower in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of unplugging the equalizing line of the Regen 2 Oleum Tower.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

4.0 References:

N/A

5.0 Definitions:

N/A

Special Safety and Health Considerations or Unique Hazards:	MSDS Information
PPE Information:	Per PPE Matrix
	Plevenge A 5.8

Steps	Action	Reasons and Key Points to Watch For
1. Boot Tank Level	Verify the need to unplug the	Check the DCS level of the boot tank (25-
	equalizing line	LI-1272B&C). If the reading is
		significantly different than oleum tower
		level (25-LIC-1272A) go into the field and
		physically touch the boot tank to verify the
		level. If the level is reading true there will
		be a temperature difference on the boot
		tank.

Version No.: Oleum Tower Unplug Equalizing Line	Version Date: 12-19-2012	Page No.: 1 of 1	
Effective Date: 12-19-2012	Author: Cammy Brown	Approved By: Chad Smith	

2. Equalizing Line to	a. Close isolation valves on the	
Oleum Tower	equalizing line to boot tank and	Programme and the second secon
	oleum tower	400
	b. Verify air hose is free of	Blow air-line before connecting to
	moisture. Attach air hose and	equalizing line to verify hose is dry
	open 100%	3: 3:
	c. Open valve to air line	
	d. Open isolation valve to oleum	7
	tower and verify air is flowing	
	e. Close isolation valve to oleum	8
II.	tower	
3. Equalizing Line to	a. Open isolation valve to boot	
Boot Tank	tank and verify air is flowing	
	b. Close isolation valve to air	mil 1 - a a militari
	line	H = 12.14
	c. Bleed air hose and remove	Store hose in appropriate area
	j. Open isolation valve to oleum	and the state of t
	tower	
	k. verify level on boot tank in	
	field	* 1 010
4. Final Check	a. Verify level on boot tank in	May take a few minutes for the level to
	field and DCS	come up in the boot tank
	b. Check area for leaks	

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Cammy Brown 12-19-2012

Version No.: Oleum Tower Unplug Equalizing Line	Version Date: 12-19-2012	Page No.: 2 of 2	
Effective Date: 12-19-2012	Author: Cammy Brown	Approved By: Chad Smith	



Oleum Tower Feeding T31 Storage

Procedure No: 20N 231.04

1.0 Purpose:

The purpose of this procedure is to describe steps for the lining up the Regen 2 Oleum Tower and feed T31 storage in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of lining up the Regen 2 Oleum Tower to feed T31 storage.

3.0 Responsibility:

The Regen -2 Superintendent is responsible for maintaining this procedure.

4.0 References:

N/A

5.0 Definitions:

N/A

6.0 Procedure:

Special Safety and Health	MSDS Information
Considerations or Unique	
Hazards:	
PPE Information:	Per PPE Matrix

Steps	Action	Reasons and Key Points to Watch For
1. Oleum Tower	Place Oleum Tower in service. Refer to SOP 20N 231.01	Communicate with Unit 8 that oleum tower is in service and will be feeding T31 storage
2. Flow to T31 Storage	a. Open the jumper valve in the crow's nest b. Open the unit 8 operator feed valve on the bottom of the rack	Verify the pump out valve on the bottom of the jumper valve is open similar to as if flow was to T77 storage
3. Final Check	a. Verify acid flowing to T31 storage b. Check area for leaks	

7.0 Review Schedule:

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

Version No.: Oleum Tower Feeding T31 Storage	Version Date: 12-19-2012	Page No.: 1 of 1
Effective Date: 12-19-2012	Author: Cammy Brown	Approved By: Chad Smith

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log: Cammy Brown 12-19-2012



Oleum Tower Recirculation Pump Shut Down

Procedure No: 20N 275.02

1.0 Purpose:

The purpose of this procedure is to describe steps for the normal shut down of the Regen 2 Oleum Tower recirculation pump in a way that sets the standards necessary for maintaining a safe manufacturing environment at the Houston Plant.

2.0 Scope:

This procedure applies to the practice of stopping the Regen 2 Oleum Tower recirculation pump.

3.0 Responsibility:

The Regen – 2 Superintendent is responsible for maintaining this procedure.

4.0 References:

N/A

5.0 Definitions:

N/A

Special Safety and Health Considerations or Unique Hazards:	MSDS Information
PPE Information:	Per PPE Matrix
	Allegary IP Company property and

Steps	Action	Reasons and Key Points to Watch For
1. Oleum Tower Level	Lower the level of the Oleum	The tower should be approximately 5'.
	Tower by putting LV-1272 into	Tower run back will cause the level to rise
	manual with an output of 100%	2-3'.
		The blower should be running between
		2400-2600 RPM. Furnace fuels will have
		to be adjusted accordingly.
2. Oleum CIL Bypass	Open the 8" Oleum Tower CIL	
5 th	cooler bypass valve halfway	

Version No.: Oleum Tower Recirc Pump Shutdown	Version Date: 12-19-2012	Page No.: 1 of 3	
Effective Date: 12-19-2012	Author: Cammy Brown	Approved By: Chad Smith	

3. Control Valves	a. Manually close off 25-LIC- 1272 b. Close the block valves on both sides of the control valve c. The controller bypass should be closed d. Manually close the 98 feed to the Oleum Tower (25-AIC- 1271) e. Close the block valves on either side of the control valve f. The control valve bypass should be closed	
4. Crossfeed Pumps	a. Press the stop button located in the field for the pump that is in service b. Block in the suction and discharge valves c. Close the recirculation on the crossfeed discharge valve on the discharge header back to the tower	Prevents pump damage from running dry when the tower recirculation pump is stopped. Prevents Oleum from going back to the tower when feeding from Tank 77.
5. Recirculation Pump	Press the stop button located in the field to the recirculation pump	Leave the nitrogen purge on the seal.
6. CIL	a. Close the 12" chain valve from the CIL cooler to the tower b. Open the acid drain valves on the Oleum Tower CIL cooler c. Shut off the anatrol protection system	
7. Oleum Valves	a. Close the 6" product line valve going to the suction of the crossfeed pumps b. Open the 3/4" expansion joint drain valves c. Close the oleum crossfeed block valves on top of the 93 and 98 pump tanks d. Manually close 25-FIC-1397	
8. Cooling Water Valves	a. Close off the inlet and exit cooling water valves to the CIL cooler b. Open the cooling water drain valves	

Version No.: Ofeum Tower Recirc Pump Shutdown	Version Date: 12-19-2012	Page No.: 2 of 3	
Effective Date: 12-19-2012	Author: Cammy Brown	Approved By: Chad Smith	

This procedure will be reviewed, at a minimum, every three years or as required per the Houston Plant HS&E Plan.

8.0 Approvals:

This procedure requires the approval of the Unit Superintendent.

9.0 Records:

N/A

10.0 Attachments:

N/A

11.0 Flow Charts:

N/A

12.0 Revisions Log:

Cammy Brown 12-19-2012

#8 Unit Start Up Procedure and Checkilist Procedure Number

1-5 6 7-12 13 Table of Contents
Checks Prior to Start Up
Pre-start Trip Checks
Checks During the Start Up
Converter Temperatures for Start Up
Blower Start Up Sequence

	Startup pH (top stage) = 10.0	
	emissions while starting the unit up.	
bri (mb stage)	the scrubber to maintain low SO ₂	is the upper stage pH acceptable for startup?
	scrubber does not run empty.	recirculating pumps?
	This will ensure the top stage of the	Are the cross flow valves open at the
	Normal flow (bottom stage) = 1200 gpm	Commence of the Commence of th
Bottom stage flow rate	Normal flow (top stage) = 1200 gpm	
	before exiting the stack.	
Top stage flow rate	This will ensure any SO2 is scrubbed	Is the #8 Scrubber in service?
DT Motor Amps	Normal amps = 70 amps	ange
DT Flowrate	Normal flow = 5100 gpm	Is the flow rate and motor amps at acceptable
	hotwell and acid will not cool to much.	acid bypass valve fully open?
	This will ensure water returns to the	Are both the DT CIL water drains closed and the
	Adequate flow over the drying tower will absorb moisture from the air and prevent it from contaminating the converter catalyst.	Is the drying tower pump in service?
AT Turbine Speed	Normal rpm = 2800 rpm	range :
AT Flowrate	Normal flow = 5500 gpm	Is the flow rate and turbine speed at acceptable
	This will ensure water returns to the hotwell and acid will not cool to much.	Are both the AT CIL water drains closed and the acid bypass valve fully open?
	saturation, and prevent a smoking stack condition.	
	Adequate flow over the absorbing tower will absorb SO ₃ , prevent brinks	Is the absorbing tower pump in service?
	65 to 70 inches of acid level is required to start a circulating pump. This will ensure the pump does not cavitate.	Check and record the pump tank level?

be the 50	ooling Level Pumps lined up (North, Middle, or South)		the 1 st for	the	the 4 th
This will ensure the caustic valve will operate correctly. Scrubber should be set up in SO ₂ control, cascade with the caustic valve, and with a setpoint of 50 prom	This will ensure there is adequate cooling available to cool the acid streams.		This will ensure the temperature of the 1st bed inlet temperature targets 800°F for the start up. Block valve - 1/8 open Bypass valve - 100% open	This will ensure the temperature of the 2 nd bed inlet temperature targets 800°F for the start up. Block valve - 1/3 open Bypass valve - 100% open	This will ensure the temperature of the 4 th bed inlet targets 750°F to 800°F. Air dilution valve - 100% closed.
Is the caustic addition set up in the proper mode This will ensure the caustic valve will and setpoint? Scrubber should b set up in SO ₂ control, cascade with the caustic valve, and with a setpoint of E caustic valve, and with a setpoint of E	Is the #8 Cooling tower ready for service?	Is the oleum tower and diluter out of service?	Are the #1 boiler valves adjusted properly?	Are the #2 boiler valves adjusted properly?	Is the 4th bed air dilution valve adjusted properly?

Is an electric oil pump in service and cooling water on the cooler?	ls the main gas blower ready for service?		Is the electric boiler feedwater pump in service?		Is the deaerator at the normal operating level?	Are the boiler chemical feed pots at the proper level and are the pumps running?			level and is it set in AUTO?	is the hailer steam drim at normal anerating
to ensure cooling and lubrication systems are operating correctly.		The recycle valve for the BFWP must be open 100% back to the deaerator to prevent cavitation.	This is to pump boiler feedwater from the deaerator to the boiler.	Normal operating level is 60%.	This is the ensure adequate supply of boiler water for the boilers.	This is to ensure proper BFW treatment.	Normal level is 55% on the DCS or half the sightglass (4 + 0.5 lugs).	trip. High level will cause water carryover into the steam header.	boiler. Low level will cause the plant to	This will and the proper operation of the
									•••••••••••••••••••••••••••••••••••••••	
		Recycle Valve postion	Discharge Pressure		Level				1	Level

	Pre-Start Up Trip Checks	Explanations	YES	NO NO	COMMENTS
	Did the low water level on the #8 boiler alarm and trip correctly?	This will ensure proper operation of the low boiler water level interlock. Blowing the water column down should trip the			
	Did the back-up electric motor start once the main oil pump stopped?	plower trip and throme valve. This is ensure the back up electric oil pump will start if the main oil pump were			
		to fail and ensure the trip and throttle valve closes if there is low oil pressure.			
t	Did the blower auxillary oil pump operate Correctly when the electric pumps were stopped? starts up properly. To test the pump, stop both electric pumps and ensure is the pump.	To ensure the steam auxillary oil pump starts up properly. To test the pump, stop both electric pumps and ensure the			
		steam pump turns on and build up oil pressure.			
1	Did the plant ESD operate correctly when tested?	To test the plant ESD and verify all parts are operational.			
		The MGB trip and throttle valve should close and the Woodward governor should trip.			
	Did the sulfur block and bleeds activate?	To ensure the sulfur block and bleeds operate during a trip condition. This can			
		be completed after sulfur was run into a barrel.			

*****Note: Do not start up unless all parts of this system are working.

			This is to allow the governor to be switched to remote speed control after starting the blower.	Is the blower controller in AUTO with a setpoint of 0 rpm?
			This allows steam to turn the blower.	Is the blower trip and throttle valve latched and the governor panel reset?
			To ensure valves are closed and prevent sulfur from leaking through into the furnace.	Is the sulfur control valve in manual and in the closed position and the manual block valves closed?
		***************************************	To allow air to enter the furnace from the drying tower and prevent the blower from surging.	Is the drying tower exit valve open and does the position indicator show open?
			To pump product acid to the storage tank as it is being made.	Is the product pump lined up to pump to the storage tank? Do not start the pump until after start up.
			To allow the gas to flow to the absorbing tower and prevent the blower from surging.	Is the SO ₃ gas valve from the economizer to the absorbing tower open? (84" valve)
			To pump condensate to the deaerator.	Are both condensate pumps in service?
Ejector Pressure			This is to create a vacuum and remove noncondensibles from the condenser. Set point = 250 psig	Is steam supplied to the jet ejectors?
			To condense the steam from the blower turbine.	Are the blower fin fans in service?
			To ensure there is vacuum on the turbine exhaust.	Is the turbine drain pot vent and drain closed? (Mark's pot)
			This is to ensure there is water flowing through the economizer and prevent the economizer RV from relieving.	Is the continuous blow down open on the #8 boiler?
COMMENTS	NO O	YES	Explanations	Checks During the Start Up

		OK? Comments Comments Potents MCR sneed step #1 on page 14
Put the blower governor in local and bring the blower to 500 rpm's. Once blower is at 500 rpm's switch the governor panel from local to remote.	Inis is to slowly purge and excess 50.2 or SO ₃ . This normally takes 5-15 minutes. Blower vacuum must be > 10"Hg	אַבוּפּוּט פֿאַפּפּט פּיספּט אַבּאַני פּיספּט פּאַפּט פּאַט פּאַע פּאַט פּאַט פּאַט פּאַט פּאַט פּאַט פּאַע פּאַט פּאַע פּאַע פּאַע פּאַע פּאַט פּאַע פּע פּאַע פּע פּאַע פּע פּאַע פּע פּאַע פּע פּע פּע פּע פּע פּעט פּע פּע פּע פּע פּע פּעט פּע
Check furnace pressure indicator to establish air flow through the unit.	Pressure on the furnace is another check to ensure air flow.	
Is the stack SO ₂ monitor picking up and SO ₂ ?	Residual sulfur in the furnace could cause SO ₂ to exceed the allowable limit	Shutdown the blower if the start-up SO_2 exceeds 400ppm.
	and must be monitored closely.	The SO ₂ limit under normal operating conditions is 3.0 lb/ton acid for a 3 hour average. This is roughly 200 ppm averaged over 3 hours. This limit does not apply during the first 24 hours after a start-up.
Does the stack have any opacity?	Opacity should be measured visually along with the use of the opacity meter.	Maximum permit limit is 10% opacity for 6 minutes.
Are the ambient SO ₂ monitors picking up and SO ₂ concentrations?	Ambient SO ₂ monitors will pick up any SO ₂ in the viscinity.	Ground level SO ₂ should not exceed 0.28 ppm for a 30 minute average. Abort start-up if these conditions exist.
Is the blower vacuum greater than 15"Hg?	This is to ensure the steam leaving the turbine is condensing at the fin fans.	Do not increase blower speed or add sulfur until vacuum reaches 15"Hg.
Has the furnace temperature dropped 50°F?	This is to ensure there is no residual sulfur left in the furnace before sulfur initiation.	Do not increase the blower speed or start sulfur initiation until this check has been completed.
Does the stack have any opacity?	Opacity should be measured visually along with the use of the opacity meter.	Maximum permit limit is 10% opacity for 6 minutes.
Is the stack SO ₂ concentration below 50 ppm and stable?	Do not start sulfur until SO_2 concentration is stable and below $50ppm$.	There is an interlock for stack SO_2 set at 500 ppm with a 1 minute delay.

S >				ळ	***************************************			ter Si	<u></u>	St.		
	Are the ambient SO ₂ monitors picking up and	Does the stack have any opacity?		Is the stack SO ₂ monitor picking up any SO ₂ ?				Slowly add sulfur to the furnace until the furnace temperature rises to 1200-1250°F.	Line up sulfur to the start-up sulfur gun.	Speed the blower up to 1500-1600 rpm's.	Step	
	Ambient SO_2 monitors will pick up any SO_2 in the viscinity.	Opacity should be measured visually along with the use of the opacity meter.	and must be monitored closely.	Residual sulfur in the furnace could cause SO ₂ to exceed the allowable limit					Keep the sulfur control valve closed along with the block valves to the three other sulfur guns closed.	ore race		Sulfur Initiation Step / MGB speed step 2
מונפשפ בסוומומסווש פאושני	Ground level SO ₂ should not exceed 0.28ppm for a 30 minute average. Abort start-up if these conditions exist	Maximum permit limit is 10% opacity for 6 minutes.	The SO ₂ limit under normal operating conditions is 3.0 lb/ton acid for a 3 hour average. This is roughly 200ppm averaged over 3 hours. This limit does not apply during the first 24 hours after a start-up.	Shutdown the blower if the start-up SO ₂ exceeds 400ppm.	If sulfur ignition is not visible and furnace temperatures do not increase, shut off sulfur to the furnace and abort start-up until the cause is determined.	Look for puddling of sulfur on the furnace floor. Puddle should be well agitated to avoid sudden increase of SO ₂ .	If furnace temperature exceeds 1400°F all sulfur must be shut off until temperature comes into range.	Visually check for sulfur ignition by looking into the sight glass in the front of the furnace.		Refence MGB speed step #2 on page 14.	OK? Comments	

	Is the pump tank water feed controller in auto with the desired setpoint and the manual block valves open?	To allow water to be added to the pump tank.	
	Are the Drying Tower and Absorbing Tower temperatures ok? If the temperature is higher, put the #8 CT in service?	Proper DT temperature 110°F-130°F. Proper AT temperature <135°F.	
	Are the Drying Tower and Absorbing Tower CIL anodic protection on and in service.	Proper temperature should be reached before starting the anodic protection. Turn on ANATROL at 122°F.	
	Adjust the 1st and 2nd layer inlet temperatures as necessary by adjusting the boiler block and bypass valves to maintain an inlet gas temperature in the normal range.	Typical Inlet Temperature = 800°F.	
<u> </u>	Is the stack SO ₂ monitor picking up any SO ₂ ?	Residual sulfur in the furnace could cause SO_2 to exceed the allowable limit	Shutdown the blower if the start-up SO_2 exceeds 400ppm.
		and must be monitored closely.	The SO ₂ limit under normal operating conditions is 3.0 lb/ton acid for a 3 hour
			average. This is roughly 200ppm averaged over 3 hours. This limit does not apply during the first 24 hours after a start-up.
<u> </u>	Does the stack have any opacity?	Opacity should be measured visually along with the use of the opacity meter.	Maximum permit limit is 10% opacity for 6 minutes.
	Are the ambient SO ₂ monitors picking up and SO ₂ concentrations?	Ambient SO ₂ monitors will pick up any SO ₂ in the viscinity.	Ground level SO ₂ should not exceed 0.28ppm for a 30 minute average. Abort start-up if these conditions exist.
1	Are the steam header pressures at the desired settings?	Add load to the generators. Reduce firing rate of the package boiler. Start the steam boiler feedwater pump.	High steam pressure could cause back pressure in the boiler and cause the relief valves to open.
	Is the steam drum level at the desired setting and are the block valves at the level controller wide open?	Normal level should be 1/2 full. The water will initially expand from heating up and then the level will start to drop.	

Maximum permit limit is 10% opacity for 6 minutes.	Opacity should be measured visually along with the use of the opacity meter.	Does the stack have any opacity?
The SO ₂ limit under normal operating conditions is 3.0 lb/ton acid for a 3 hour average. This is roughly 200ppm averaged over 3 hours. This limit does not apply during the first 24 hours after a start-up.	and must be monitored closely.	
Shutdown the blower if the start-up SO ₂ exceeds 400ppm.	Residual sulfur in the furnace could cause SO ₂ to exceed the allowable limit	Is the stack SO ₂ monitor picking up any SO ₂ ?
Should be ~4 hours.	Typical Furnace Temp = 1700°F	Raise the furnace temperture to the specified temperature by putting the controller in automatic and opening sulfur guns when needed.
Should take ~2 hours.	Typical Inlet Temp = 800°F (both beds) Typical Outlet Temp = 1150°F (1 st bed) Typical Outlet Temp = 930°F (2 nd bed)	Once the 1 st and 2 nd bed tempertures have reached normal operating temperatures, increase the blower to the desired production rate.
There is an interlock to shut down #8 if the scrubber level is to high.	This will ensure the scrubber product will be processed and the scrubber will not fill.	Set the scrubber to pump to either the Regen 2 acidulator or the #8 acidulator.
	20 gpm will be enough to keep the top stage from running empty. Monitor bottom stage specific gravity and adjust as necessary.	Start the make-up water addition to the top stage of the caustic scrubber. Start with 20 gpm of water flow and close the cross over valves.
	Typical Inlet Temperature = 800°F.	Adjust the 1 st and 2 nd layer inlet temperatures as necessary by adjusting the boiler block and bypass valves to maintain an inlet gas temperature in the normal range.
Procede to Blower Speed Step #3 on page 14.		Raise the blower speed to 2000 - 2200 rpm's maintaining the same furnace temperature.
Should be 2-3 hours		Is the 1 st layer inlet temperature at 800°F and the 1 st layer exit temperature above 1050°F and rising?

L			Ospania 10, 101 Charlet avecad 0 28nnm
	Are the ambient SO ₂ monitors picking up and	Amblent SO ₂ monitors will pick up any	Glouina level 602 stroatia fiot exceed 6.26ppm
	SO ₂ concentrations?	SO ₂ in the viscinity.	for a 30 minute average. Abort start-up if these conditions exist.
	Pull an acid sample from the absorbing tower when the temperature is between 130°F - 150°F to verify acid strength and Fe content.	This temperature range is within the compensation range for the conductivity meter.	Ensure lab strength and analyzer strength are similar or a calibration is needed on the instrument.
	Start the product pumps to pump to the desired product storage tank.		
<u> </u>	Set the scrubber to pump to either the Regen 2 acidulator or the #8 acidulator.	This will ensure the scrubber product will be processed and the scrubber will not fill.	There is an interlock to shut down #8 if the scrubber level is to high.
<u>L</u>	Check to ensure all valves are set at proper position for normal operation.		
	Monitor converter temperatures, acid strength, stack SO ₂ , opacity, etc. and other items on the logsheet.		
1	Put the oleum tower in service as needed.		
<u> </u>	Run boiler water samples and make necessary adjustments.		
1	Make sure the chemical feeds are being added to the cooling towers and the boiler. Make sure the cooling tower pH is within acceptable range (pH is 7.5-8.0).		
1	Make a note in the log and verbally communicate any malfunctioning items the next shift should be aware of.		
1	Make sure all interlocks are not bypassed and in the normal operating position.		

Minimum Converter Temperatures for Start-up

Recommended Temperatures not requiring a Natural Gas Heat-up
In Out

1st Layer	520	700
2nd Layer	650	700
3rd Layer	550	550
4th Layer	520	550

Consult with start-up supervisor on how to proceed if the temperatures are lower than the above temperatures.

Minimum temperatures after a Natural Gas Heat-up.

4th Layer	3rd Layer	2nd Layer	1st Layer	
600	600	750	800	=
600	600	750	800	(

the addition of the Caustic Scrubber. #8 Unit has been started up with the following conditions after a prolonged shutdown due to changing out the Dry Tower Brinks Elements and with

Furnace Temperature	4th Layer	3rd Layer	2nd Layer	1st Layer	
berature	662	565	503	405	Ξ
840	670	733	701	577	ב

These temperatures are a reference of what has happened in the past. Please consult with start-up supervisor if these temperatures are present.

Blower Speed Step #1 Unit Purge Sequence

		Oille algo ocquesios	
	Maximum	Minimum	Preferred Range
Blower Speed RPM Must be Stable	700	200	450-600
Furnace Temperature Must be Decreasing	N/A	510 Interiock at 700	950-1200
Sulfur Flow	0	0	0
Blower Vacuum Must be Increasing	27	15	20-25
Furnace Pressure	30	5	5-10
2			

Blower Speed Step #2 Sulfur Initiation Sequence

	Maximum	Minimum	Preferred Range
Blower Speed RPM	1700	1200	1500-1600
Furnace Temperature	1400	510 Interlock at 700	1200-1250
Sulfur Flow	20	8	10-15
Number of Sulfur Guns		7	- Pares

Begin to Bring Unit up to Maximum Speed

	À		(,
	Maximum	Minimum	Preferred Kange
Blower Speed RPM	2500	1800	2000-2200
Furnace Temperature	1400	1200	1200-1250

Shutdown Checklist

700 ∪	Procedure Number	Operators
)ate		Supervisor
		YES NO COMMENTS
	Sulfur flow controller in manual closed position?	
N	2 Sulfur guns closed off?	
ω	Steam on sulfur guns?	
4	Are the sulfur guns leaking steam?	
O1	Sulfur manual valve closed and line drained to barrel?	
0	6 Absorbing tower water feed controller in manual closed position?	
7	Water to pump tank block valves closed?	
œ	Blower speed controller in manual and closed position?	
	9 Air valve to furnace closed?	
13	10 Drying tower pump shutdown?	
1	Product pump shutdown and valves closed?	
<u>₹</u>	12 Electric boiler feedwater pump on?	
	13 Blower fin fans shutdown?	
14	Is the turnine drain pot open to drain the turbine of condensate? (Mark's pot)	
15	15 Seal steam, jet ejectors, and hot well pumps off?	
 	Oleum tower shutdown with feed loop and storage loop manual and automatic valves closed?	
	17 Cooling water off oleum tower CIL and the drains open?	
<u>x</u>	18 Is the anodic protection turned off the oleum tower CIL?	

-		YES NO COMMENTS
19 Dilu	Diluter shutdown with product feed valve and water feed valve closed?	
20 Coc	Cooling water off the exchangers and exchangers drained of cooling water?	
21 Coc	Cooling water pumps and fans shutdown?	
	Strong acid and chemical feeds to cooling towers shut off? 22 (Leave AEC running for short term shutdowns)	
23 Dra	Drain the water from the AT CIL, DT CIL, and product cooler?	
24 Is th	Is the CW header valve to product cooler closed?	
25 Abs	Absorbing tower pump left running if possible?	
26 ls t	26 Is the anodic protection turned off the DT CIL and AT CIL?	
Pur 27 (No	Pump tank level has adequate space if absorbing tower pump shuts down? (Note: 24% level increase of runback for each tower)	
	Boiler water at normal level?	
29 #1	#1 and #2 boiler gas exit valves closed and bypasses open?	
30 Blo	Blower oil pump running?	
	Air dilution valve closed?	
32 AU	AUX cooling tower in service for 65% oleum and 70% diluter?	
33 Str	Stripper valves secured and line blown to neutralization?	
SCI SQI WAR	Scrubber water and caustic valves closed and cross over valves open? Demin water feed off Scrubber, blocked in and pump off?	
	Raise the steam pressure on the front of the furnace while the unit is down.	
	36 Is the AT CIL pH probe out of service? See SOP# HO-UNIT8-SOP016-UNIT8	
37 WE	37 Was this an emergency shutdown?	
38 lf e	If answer to #37 was YES list in detail the sequence of events	

YES NO COMMENTS



8615 Manchester St.

Houston, TX. 77012

December 27, 2012

Certification of Standard Operating Procedures

I hereby certify that the Standard Operating Procedures for the #8 Unit, Utilities, 65% and TXUP of the rhodia Inc. Houston site were reviewed in 2012 and were determined to be accurate and current. Qualified personnel, Drew Foster and I have reviewed these Standard Operating Procedures, ensuring that they reflect current practices, including modifications resulting from changes in process chemicals, technology, equipment and changes to stationary sources.

Jimmy Wooden, #8 Production Supervisor

Date

15-52-5015

Unit/Area: #8 Unit

Rhodia Inc. Houston



ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures for the Regen II operating unit of the Rhodia Inc. Houston site are accurate and current. Qualified personnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice.

Robert Stafford Operations Superintendent

Date

Unit/Area: Regen II Rhodia Inc., Houston



ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures for the Regen II operating unit of the Rhodia Inc. Houston site are accurate and current. Qualified personnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice, including modifications resulting from changes in process chemicals, technology and equipment and changes to stationary sources.

Dean Sloan, Operations Superintendent

Unit/Area: Regen II Rhodia Inc., Houston Date



ANNUAL CERTIFICATION OF STANDARD OPERATIONG PROCEDURES

I here by certify that the Standard Operating Procedures for

Regen II

area of Rhodia Inc Houston Site are accurate and current. Qualified personnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice.

Operation Superintendent
Unit/Area: Research

Rhodia (Solvay)

8615 Manchester St.

Houston, TX

ANNUAL CERTIFICATION

OF

STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures (SOPs) the for **REGEN II** area of Rhodia (a member of the Solvay Group) Houston Site are accurate & current. Qualified personnel under my direction have reviewed these SOPs, ensuring that they reflect our current practice.

Operations Superintendent

Date 8-Nov. Zoiz.

Unit/Area Regen 77.





ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

hereby certify that the Standard Operating Procedures for the
(Name of Unit/Area)
(Name of Unit/Area)
of the Rhodia Inc. Houston Plant site are accurate and current. Qualified the error of the sersonnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice.
ogistics Superintendent Z/15/08 Date
Init/Area: Logistics
hodia Inc.,
Iouston Plant



1/2003

ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Ope	erating Procedures for the
Logistics	
(Name of U	Jnit/Area)
of the Rhodia Inc. Houston Plant site personnel under my direction have re Procedures, ensuring that they reflect	eviewed these Standard Operating
1 toccautes, ensuring that they refree	content practice.
Matt Butce	1/5/09
Logistics Superintendent	Date
Unit/Area: Logistics	
Rhodia Inc.,	
Houston Plant	



ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures for the Logistics Department at Rhodia Inc.'s Houston site are accurate and current. Qualified personnel under my direction have reviewed and updated department Standard Operating Procedures, ensuring that they reflect current practice.

R. Brett Jacks, Logistics Manager

Date

6/2/09

Rhodia Inc., Houston



ANNUAL CERTIFICATION OF STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures for the Logistics Department of the Rhodia Inc. Houston site are accurate and current. Qualified personnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice, including modifications resulting from changes in process chemicals, technology and equipment and changes to stationary sources.

Brett Jacks, Logistics Manager, Rhodia, Houston Date: 6/25/10

Unit/Area: Logistics Rhodia Inc., Houston



ANNUAL CERTIFICATION OF STANDARD OPERATIONG PROCEDURES

I here by certify that the Standard Operating Procedures for

Logistics

area of Rhodia Inc Houston Site are accurate and current. Qualified personnel under my direction have reviewed these Standard Operating Procedures, ensuring that they reflect current practice.

Operation Superintendent Date
Unit/Area:

Rhodia (Solvay) 8615 Manchester St. Houston, TX

ANNUAL CERTIFICATION

OF

STANDARD OPERATING PROCEDURES

I hereby certify that the Standard Operating Procedures (SOPs) for oleum for the **Logistics Department** of Rhodia (a member of the Solvay Group) Houston Site are accurate & current.

Qualified personnel under my direction have reviewed these SOPs, ensuring that they reflect our current practice.

Logistics Manager

Date 11/8/12

Unit/Area Logistics .

Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5.) Operator Training Records
- 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

Name Jerry Marshall Job Title Chier Operation

Check the appropriate boxes to Indicate the following:

D = Demonstrate; W = Written; V = Verbal; P = Pass; F = Fail

No.	D	W	V	Job Procedures/Job Aspects	P	F	Date
1	~			Unit Startup Procedure	P	<u> </u>	4-3-2012
2	~			Unit Shut Down Procedure	ρ		11
3	1			Oleum Tower Startup Procedure	P		رد
4	~			Diluter Startup Procedure	ρ	ļ	11
5	1			#8 Boller and Cooling Tower Water Tests	P		
6	1			Unit Heat Up Procedure	P		ξ
7			V	Unit Emergency Alarm and Shutdown Procedure	P		1,
8			1	Unit Critical Operating Parameters	P		
9	1		7	Unit Interlock Matrix	P		10
10		***************************************	J	Emergency Scenarios	P		11
11				Permit Limits	P		16
12			0	Unit Safety Rules and PPE Requirements	ρ		"
13			1	Life Critical Permit Procedures	P		"
14				Written Test	P		4

Overall Performance:	(Circle One) (Pass) Fail		
Evaluator's Comment	s:		MALANIA MARIANIA MARI
Trainee's Comments:			
Trainee's Signature:	Jerry Mashall	Date:	4-3-7012
Evaluator's Signature:	July Wooden	Date: _	10 SO15
Demonstrate	The Operator will either perform or den	nonstrate hov	v to perform the procedure
Verbal	The Operator will verbally answer the q		
Written	The Operator will take the final written	exam	
Pass	Greater than or equal to 80% of the an	swers are cori	rect
Fall	Less than 80% of the answers are corre	ect	

#8 Operator Recertification Test

- 1. List the PPE required for starting a piece of equipment, after maintenance has worked on it, where a potential for acid exposure could occur?

 HARA 14 AT FACK Shidd- Copples Sheeker

 Robber Goots
- 2. What is the Mastercard permit system and why do we use it?

 This Form is used to Document Aboutout Between Main trade 4
 operations of Show All Lock ON SOB there sind By Man T. That The

 Equipment is 215 of Ready for World
- 3. List five critical operating parameters (COP's), the critical set points, what may cause the condition and your response? (Be brief)

 0 ABS Pup Less 54800 Surfur rep L 3440 Blower Trip

 0 STACK High 502 500 PM So. Imin Unit Trips

 80 DT FLOW E3600 Suffer Tryps L2639 Unitarips

 41 Sur But Low Plan Less 600 LPM Unit Trips

 5. MEB ashny Presson 280 on High Trips down

 4. Describe the steps in order, how to bring the unit up to full production after a short shutdown?

 P.11 Statup Saple Subser 11 STRIPPER 115 Trip Checks

 VACUM EN CO-A. ABS Running DT Running Mall Blower Soo RPM

 Mointer STACK & Furnase. VALL Converte Temps APP 17 Subser

 WALL SOP Add CAUSTICE I MAINTAIN 12 50 L
 - 5. List the #8 operating permit limits?

 Opacity Less 10°70 A-1 10m .~

 500 Texas 50°2

 L7 ppm hor 7 crm 50°2

 3.0 ppm 3 ldr. 50°2
 - 6. Describe the procedure on how to feed 20% Oleum on the Oleum tower to make 30%?

 Open 89 " NAWE ON CLOSA 48" VALUE ANSOUT HOO ON CLE

 LINE UP 20% From Tank Dy OFEL TO OT- MONITOR LEVEL

 + STrength of Tower + Adoust to maintain Proper Level & Strength
 - 7. The sulfur pump stops and will not restart and the spare is out of service. What would be your response?

 Out Sulfur value in market open to were it was approx

 Out Sulfur pump try to Reset it I felt wort Go

 Go to Sulfur pump try to Reset it I felt wort Go

 Notific Riz do the operator unit is Going Aown

8. Why are cooling tower and boiler water chemicals important to the unit? How often should the analyses be performed?

Caustic. Alker Ling of phi in Boiler. Bleach Maintain Chi in LT

Condeal of SC Aveyan. Stendar Pass Condens for PH

Condeal of SC Aveyan. Stendar Pass Condens for PH

Optispass Convisor who beton

Stendar Feel water 88 to 9.2 School 2.05

Strong Acid on Town PH Control

Condeal will 20 Condeast phis phis to 9.2

Harlacks (0.1

Boiler Cond. 700

9. What is the first indication of a boiler tube leak and what would your response be?

9. What is the first Indication of a boller tube leak and what would your response be?

Size of REC in OPACITY - MILL TEMP WILL RISE - BOLLER LOCK WILL FILL OUT

Shut Down Unit & Secure ASAP ... Leave ABS AppRoxing - acck fail 57 Puts

Chose of S Nort Return ope Bollers to profin water & Economizer Defin

Leave CT 1/5 To Cook Aud

10. What is stack opacity? What should your response be if opacity is rising?

Op. 1-17: 5 Moiston in the System chick staken on Suffer

Coys & cherch Boile hold End & Euromize Prairies abso

Check make sum A east raps are in Range

11. Describe how to switch the scrubber liquid flow from regen to #8 acidulator?

STUND of Acidulator FAN + Pups call R-2 Tall Thun

All be quil 13 Caning +3 Thin

12. Describer how to switch the #8 scrubber from SO2 control to pH control and in what sceanics would you do this?

STACK TESTINY + CAMBRAGING OF STRUCK

USE MOUSE PRESS LOTO SULLIA TO PH. CONTROL AND VIEW NEVER TO BELL CONTROL FOR SILL RASSIC RASSIC RASSIC OF TO THE PAISE PH ON UPPER STRYT

13. What interlocks to the unit are on the Scrubber system and what are they?

Sindiffer here 9) 70 to leseption over their Scribber

Surabber those 6000 to Ensure Mar those Circles over The Town

High STACK 502 502 PM 1 min

Town Marshall

STAUFFER EMPLOYEE SINCE: 198

S.A.P. OPERATIONS ENTRY: 3-10-82

JOB FUNCTION	DATE TRAINED	TRAINER	DATE, FOLLOW UP TRAINING, COMMENTS	FINAL REVIEW
LUBRICATION.	***************************************		•	Camarant S
No. 8 blower turbine	3-11-82	50	4-22 OC	6-7 6
b. No. 8 cooling tower pumps	3-11-85	50	<i> →</i>	
c. No. 8 water booster pumps				
d. No. 8 drying tower gearbox, motor,	3-11-82	50	5.22 CC	Jo 5-3
pump 8 absorbing tower turbine, gear-	3-11-82			
dund	3-11-82	Transport of the Parks	- Andrew Marie Control	
turbine, pump 8. No. 8 electric boiler feed pump	3-11-85	_		
h. Treated water pumps(5)				
1. Inert gas generator				
ACID SAMPLING			.•	
a. P.P.E.	3-12-82	V	4-22 86	20 r-9.
Types of acid to be sampled (115, 107, 104.5, 99, 96, 93)	3-17-82	, _		
c. Method	3-(2-92	$\overline{}$		
			-	

S.A.P. OPERATIONS EMIRY: 3-10-92

STAUFFER EMPLOYEE SINCE: 198

· 		Ħ						·			н	
c. Method	a. P.P.E b. Types of acid to be sampled (115, 107, 104.5, 99, 96, 93)	ACID SAMPLING	1. Inert gas generator	R. No. 8 electric boiler feed pumph. Treated water pumps(5)	steam boiler fe	e. No. 8 absorbing tower turbine, gear- 3-11-82	d. No. 8 drying tower gearbox, motor,	c. No. 8 water booster pumps	b. No. 8 cooling tower pumps	a. No. 8 blower turbine	LUBRICATION.	JOB FUNCTION
3-12-82	3-12-82	,		3-11-80	3-11-82	3-11-82	3-11-82		3-11-82	3-11-82	····	DATE
	~ ×	·			And the second		20		S	50		TRAINER
	12 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2						der de		$\sqrt{}$	1-22 ox		DATE, FOLLOW UP TRAINING, COMMENTS
							6-406					FINAL REVIEW AND COMMENTS

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	FINAL REVIEW AND COMMENTS		6-7.08						•	6-4 ok					<u>/</u>	· January		
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	TRAINER		SQ			\	20			Ç.	4	management of the same	**************************************	the section of the section of	The second secon	and the second s	**************************************	
	DATE TRAINED		3-15-82	3-12-82	3-15-82	3-17-82	2/2			Ċ) () ()							
•	JOB FUNCTION	65% OLEUM	a. Process & Flow	b. Equipment & Function	c. How to put in service.	d. How to take out of service.	e. How to flush for maintenance.	f. What to do for a 65% leak in pump or line.	g. What to watch during normal operation.	AIR COMPRESSORS	a. Process & flow	b. Equipment & functions	c. How compressors operate.	d. Now dryers & filters operate.	e. Importance of dry air for inst. & other uses.	f. Housekeeping duties: change oil-sorb, wipe down.	g. Start up and shutdown procedures.	
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g. Start up and shutdown procedures.	 d. Now dryers & filters operate. e. Importance of dry air for inst. & other uses. f. Housekeeping duties: change oil-sorb, wipe down. 	b. Equipment & functionsc. How compressors operate.	AIR COMPRESSORS a. Process & flow	e. How to flush for maintenance. f. What to do for a 65% leak in pump or line. g. What to watch during normal operation.	How to put in service. How to take out of service.	a. Process & Flow b. Equipment & Function	JOB FUNCTION
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JOB FUNCTION	h. Normal operating limits, air pressure, water temp.	1. Shurdown devices: high air temperature, low oil pressure.	j. Routine checks & duties.	a. Process & flows	b. Equipment & functions	c. Water flow	d. Uses of inert gas	e. Startup & shutdown of units.	f. Normal operating limits, gas & air pressure, inert gas discharge temp. & pressure drop on dryer &	g. Routine checks & duties.	OLEIM/NITRIC VENT SYSTEM	a. Process & flow	b. Equipment & functions	c. Startup and shutdown	d. How to establish vacuum on tanks.	e. How to control #4 tower
	-			۵	······································				····		ΗΔ					,

JOB FUNCTION	TRAINED	TRAINER	TRAINING COMMENTS	AND COMMENTS
h. Normal operating limits, air pressure, water temp.	722)~ Q	d'in occ	6-4 Ole
1. Shutdown devices: high air temperature, low oil pressure.	·		•	
j. Routine checks & duties.	Constant			
INERT GAS SYSTEM	23.6	~	G. W. Fan	for 4 Far
b. Equipment & functions	`,	\		
c. Water flow				Cerci
d. Uses of inert gas		·		
e. Startup & shutdown of units.				١
f. Normal operating limits, gas & air pressure, inert gas discharge temp. &				
pressure drop on dryer & filters.	,			
g. Routine checks & duties.		Description of the second		
OLEUM/NITRIC VENT SYSTEM	7 - 7	200	you de	6-1
a. Process & flow	W. C		Α,	
b. Equipment & functions				
c. Startup and shutdown				
d. How to establish was		Market Control		
on tanks.				

	JOB FUNCTION	DATE TRAINED	TRAINER	DATE, FOLLOW UP TRAINING COMMENTS	FINAL REVIEW AND COMMENTS
-	f. How to control Brinks	3-12	10	4.22 OCC	70 5-9
IIA	NO. 4 BOILER a. Process & Flow	2,	5.0	4.22 Ol	M 4.9
	b. Equipment & Function				
	c. How to fire boiler, control firing rate.				
	d. How to maintain water level & header pressure.		, and a second		
	e. Chemical treatment.		The same of the sa		<i></i>
	f. How to shutdown.	•			. Barrenser-Frag.
,	g. What to watch during operation.	managan ami			
VIII	NO 1 COOLING TOWER	22	2		
	a. Equipment functions & flow			2-27 29	6-7 ell
	b. Chemical treatment	•	<u>,</u>	<i>C</i> .	
	c. Lubrication				
	d. What No. 1 tower supplies water to.	and the second second	and and an		
Ħ	SPIT TARGETS & MIST TESTS	and the second	\		
	a. What they are δ why we do them.	7	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	2- 22 ok	(e-y Oll
	b. How to do stick test on abs. & dry tower.				
	c. Where spit targets are, how to change & how often to change.				

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			Ä		•			VIII	ı							VII		-
c. Where spit targets are, how to change & how often to change.	b. How to do stick test on abs. & dry tower.	a. What they are & why we do them.	SPIT TARGETS & MIST TESTS	d. What No. 1 tower supplies water to.	c. Lubrication	b. Chemical treatment	a. Equipment functions & flow	NO 1 COOLING TOWER	g. What to watch during operation.	f. How to shutdown.	e. Chemical treatment.	d. How to maintain water lev- el & header pressure.	c. How to fire boiler, con- trol firing rate.	b. Equipment & Function	a. Process & Flow .	NO. 4 BOILER	f. How to control Brinks	JOB FUNCTION
$\overline{}$		3-12	and in	The state of the s			. (212	para de la compansión de		The American			geriam objec sakreka bez	\	1°	3-1-2	DATE
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TRAINER	50	~ \ ~			and the same of th	200	20	
DATE TRAINED	<u>}</u>	3.18				28-21-8	3-15-82	
JOB FUNCTION	x VALVE ALIGNMENT a. How to align feed & product tanks.	XI ASSIST NO.1, NO.8, & UTILITIES OPERATORS a. Normal operations	b. Startup Duties 1.Sulfur pump operation 2.No.8 boiler control c. Shutdown Duties	d. Emergency Duties 1.Oleum spill 2.Power failure 3.Low steam header	XII STICK GAUGE TANKS a. How to do and why	AIII HOUSEKEEPING a. Control room; desks, lab, kitchen, locker room b. Unit; hoses, cords, rugs, oil lockers, trash.	XIV EMERGENCY DRILLS a. Safety equipment b. Duties	

	, XIV	IIIX	XII		×	ĸ	
	EMERGENCY DRILLS a. Safety equipment b. Duties	HOUSEKEEPING a. Control room; desks, lab, kitchen, locker room b. Unit; hoses, cords, rugs, oil lockers, trash.	STICK GAUGE TANKS a. How to do and why	d. Emergency Duties 1.Oleum spill 2.Power failure 3.Low steam header	ASSIST NO.1, NO.8, & UTILITIES OPERATORS	valve align feed s product tanks.	JOB FUNCTION
	3-18-82	3-12-82			3-12	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	DATE
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TRAINER			•		
DATE TRAINED	~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~	3-10-82 3-10-82 3-10-82			·
JOB FUNCTION	a. Know what safety equipment is needed to do job duties. b. Multiple lockout procedure.	<u> </u>			
	X	xvx			;

· ·	·							> 4	ST.	×v		
						d. Power Distribution	b. 1500 & 5000 KW GENERATORS	a. No. 1 & No. 8 unit.	b. Multiple lockout procedure	a. Xnow what safety equipment is needed to do job duties.	JOB FUNCTION	
				-	. •	3-10-80	3-10-82	3-10-82	<u></u>	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	DATE TRAINED	
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-								6-4 Fan	6-7 CK	6-4-22	AND COMMENTS	
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Name Robert Brown Job Title B Operator	
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Check the appropriate boxes to indicate the following:

D = Demonstrate; W = Written; V = Verbal; P = Pass; F = Fail

No.	D	W	٧	Job Procedures/Job Aspects	P	F	Date
1	1			Unit Startup Procedure	·		11-2012
2	V			Unit Shut Down Procedure	t-/		
3	V			Oleum Tower Startup Procedure	٠~١		1
4	~			Diluter Startup Procedure	c		٠,٠
5	V	***************		#8 Boiler and Cooling Tower Water Tests	e		ر
6	V			Unit Heat Up Procedure	w		ر ب <u>ي</u>
7			~	Unit Emergency Alarm and Shutdown Procedure	~		<i>-</i> \
8			V	Unit Critical Operating Parameters	•		د ۳
9			<i>u</i>	Unit Interlock Matrix	V		11
10			<i>y</i>	Emergency Scenarios	V		11
11			V	Permit Limits	1		٧,
12			V	Unit Safety Rules and PPE Requirements	1		11
13			V	Life Critical Permit Procedures	V		(1
14		\mathcal{I}		Written Test	1		٦

Overall Performance	e: (Circle One) (Pass) Fall		
Evaluator's Comme	nts:		
	A O A . A	Λ_ ι	
Trainee's Comment	s: 6000 Krunledge &	wt a der	un stut un
Trainee's Signature	*	Date: _	
Evaluator's Signatu	re: Jin () woln	Date: _	12-7-2012
Demonstrate	The Operator will either perform	or demonstrate ho	w to perform the procedure
Verbal	The Operator will verbally answer	r the questions base	ed n the procedure
Written	The Operator will take the final w		
Pass	Greater than or equal to 80% of t	the answers are co	rrect
Fail	Less than 80% of the answers are	correct	

#8 Op	erator Recertification Test
1.	List the PPE required for starting a piece of equipment, after maintenance has worked on it, where a potential for acid exposure could occur?
2.	What is the Mastercard permit system and why do we use it?
3.	List five critical operating parameters (COP's), the critical set points, what may cause the condition and your response? (Be brief)
4.	Describe the steps in order, how to bring the unit up to full production after a short shutdown?
5.	List the #8 operating permit limits?
6.	Describe the procedure on how to feed 20% Oleum on the Oleum tower to make 30%?
7,	The sulfur pump stops and will not restart and the spare is out of service. What would be your

response?

Name:___

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	10. Call up on D.C. S. screen a constre anthol suitch either
	Ph control ox Sb2 control, To cal, brate probes,
	B) Lew water How over Tower Llove GPM. High So 2 AROVE SOOPPA In IMIN, Low water level in Tower, High temp in Tower high water level in Januar 795/p,
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Provide Frank

#8 Operator Test

1. Explain the purpose and function of the following items:	
• Blower Force Exigent GAS through the s • Drying Tower Remone Moist AIR that is	force into the system.
- #1 Roller that exchange the 40 5 the	S 1501 WE GHS STARREIM,
• Converter (SN/ant 30 70 30	- Claus.
• #2 Boiler Heat exchanges to cool 9113 • Economizer Heat exchanges to cool 9113	
• Beconomizer Head exchanges to and offs • Absorbing Tower 1650x the gas indu the	liquand Held strangth.
· Brinks To Eliminate And MIST To Aym	seh cae
2. Explain the purpose and the function of these parts of the	steam system,
· Steam Drum Collect steam at high pressure	
· Deaerator Romone AIR from Denye Water	t none condenables.
· Non-Return Valve Let steam flow memby one	direction.
\$3. What are your responsibilities during a normal plant shute	down?
· ·	
4. What are your responsibilities during an emergency shutch	iown?
✓ ↓5. Describe how #8 production rates are maximized via the	SO₂TPD.
6. What is the permit limit for stack opacity? SO2 SOUTH FOR IMPLIED BY SOUTH AND SOU	7/tov 2/1/2 AVG, SK 325 LB 1 HEAVG PAGE
7. Describe how to put the oleum tower in service to 77 tank	scoullen.
8. Draw a block diagram of the #8 unit gas flow.	ery frank man () device Mission)
9. What are the different types of dilution water that can be	fed on #8 pump tank. Commercia Beneg
Chown duality Plocoss march, venin ware,	
10. List the interlocks that will trip #8 unit.	ne, Blower 46-palace, low oil passing on the
He 185 HH 335 Partru	195° HA - HH235°.
12. At what temperature do you turn off the anodic protection	on the acid coolers?
Sout down when you have to Hon	d ofter a nower failure
\$13. Explain what you would do it power could not be restore	·
14. What is the approximate strength of the acid that is circultower? Drying tower?	ating over the absorbing
18.5-96.96	
10.2 10.110	

15. Explain what steps are necessary each time you open the bus tie, close the bus tie.

**Plant for the Story three states are sufficiently show the fill t

And Fine cause,

If opports 15 710% for 5min would need to shitden

Question 4 3 + 4 Unat me your responsabilities during normal Dent Gut lan? D. Wifisupersis dod plat. Q Close off sefur How & block in Selfur relies open stant Car sur Diei selfen to Conside D. Close off water to the page tak i monitor Haid stripth i bul in pays take B flace M.G.B in married i place in ORPM, Do Close farare Am Value tore of positile, also statelen product to Start boile feed uctor pro (E/c) nantais I Sunt den ander so for i pryso, close off Shanna anyederla D. SLA de Olutow, ad fad to the town Olov detides propo a lucter feel D. Cooling with for O.I. L'S al form of the Cool down 10, Cluse #1 12 holler values. or Check oil prove you Mr. G. B. What are you re spositities during energy, shit down? D. All the others and determine the cause of this situation Acrid flows, cooling 15 source, electrical issues under locktupe, storell,

Question #5

Hew to Burns HB tachetim Pates 119 So2 lunts. D. Will used Hard sample In Rab, Check strongth. Jo Notify Experiorisition i have stant-up copies. So. Do hip about In loven water boilen waterlooks i SD24 Opasity duft Charks. Q Have steam on 450 header-yp. 5 Start Duying tensor 1 Absorbing tomen gays. 6. Start anderson downs i flores ... O. Establish steam ejectors for M.G. E. Manule & Goo PPM Open B4" Value, Set M.G.B., ~ Roto on D.E.S. Low Open one sulfue gun i close stean an sun. 1 Monton 562 1 Opacity on Speck/ senther. Purplante level 1 And strength. Boiler level Mon for Conventor hap In #1 intel i Exit. 500° intel 1100° out taps. Monton Had lagratures & for C.I. L'S, start cooling page when deeded also fins when meeted. I as would need to months So? on senther souppout I min true, or 318/100 on 3HR Ang ox 1.7 / for fax 24 He May ox 305 LB/ 14x Arg. and aparty greater than 10% In some Aug.

Overtratt 7 Oleum tomen in source - 77 tale. 10 De former where you will got your fuel.
Line-up to oleun dances. Joseph Boot purps into CIL Color mex fourer Check How 1 Brg. I B. Stant Por prop Six water Stew. Coling a fox coding water I Dopon 48" take for grs flow Sox Acid strength. Lined-up 98% And In to montain Oleum structh. Dopen Cham Value to 77 tank close chains value to On Open controll loop In Oleun stonage.
Mandain Oleun stragth in tower,

Question A-13 What To Do after former failure? 10. Notety supervisition of event. 10. Nove NON-REBERT Velve for Boiler 77/ (772 1 Exit while on Boiler, JO Close weter to porpo tark. JO Black sultire to tremse, JO Gen skon values to Silfue Gows, 16. Manuley Close Had nothe that may lead By, Mar, lex Boiler water level.

Questin # 16 How to pet the delike in secure to 23 tank. O. Will weed to establish where you will get your feed And, But mostly off daying logs seal. Close of all dean that have been opened. Line of North South And purp Q. Line-youeter for exchangeus, 1. Line-yo demmuater for mixing fee, 6. Control values in mouvel i reset on 2.65, & After Hard is flowing stant marker games, 6 witch tous use or minery too Q Close all other value to storage I have 23 tout bud-up on top of tall montal level in tank,

Mame	Ed	GLASSCOCK
ivanie		(A) (3.2.2

Verbal

Pass

Fall

Written

Job Title Levad Operator

Check the appropriate boxes to indicate the following:

D = Demonstrate; W = Written; V = Verbal; P = Pass; F = Fail

No.	D	W	V	Job Procedures/Job Aspects	Р	F	Date
1	V			Unit Startup Procedure	<u> </u>		8-2012
2	ν.	 		Unit Shut Down Procedure			۸,
3	Ŷ			Oleum Tower Startup Procedure			ąt
4	Y.			Diluter Startup Procedure			\1
5	V			#8 Boiler and Cooling Tower Water Tests			~1
6	Υ.			Unit Heat Up Procedure			(,
7	3,		K	Unit Emergency Alarm and Shutdown Procedure		<u></u>	11
8			у.	Unit Critical Operating Parameters			11
9		*********	V.	Unit Interlock Matrix			13
10			V.	Emergency Scenarios			* * *
11			X	Permit Limits			'\
12			2	Unit Safety Rules and PPE Requirements			١,
13			K	Life Critical Permit Procedures		<u> </u>	١
14		X		Written Test		<u> </u>	11

Overall Performance:	(Circle One) Pass Fail
Evaluator's Comment	s: Excellet knuledge of with -
Trainee's Comments:	
Trainee's Signature:	NA Date: NA
Evaluator's Signature	Jim Words Date: 11-2012
Demonstrate	The Operator will either perform or demonstrate how to perform the procedure

The Operator will verbally answer the questions based n the procedure

The Operator will take the final written exam

Less than 80% of the answers are correct

Greater than or equal to 80% of the answers are correct

#8 Operator Recertification Test

- 1. List the PPE required for starting a piece of equipment, after maintenance has worked on it, where a potential for acid exposure could occur? Full red suit, rubba boots, rubba qloves Hadhat, face shield, safety glasses, hood
- 2. What is the Mastercard permit system and why do we use it? A form used to downent Lockart/tag outs. The purpose is to make sure that equipment is safely secured a de-energized to prevent injuries and equipment damage during maintenance operations.
- 3. List five critical operating parameters (COP's), the critical set points, what may cause the condition and your response? (Be brief) (I) His scribbon level, 90%, 5tripper brips out allower from at brinks low. Alarm @ 2 = blower trip, towar packing collapse, acid indust. Shutdown a spource unit. (I) how boder what level alarm @ 25% level control unive tailore, tubeloake, feedwater purp shutdown, economizer libe look Trip unit, get water into boder asep, alose non return shutdown, economizer libe look Trip unit, get water into boder asep, alose non return shutdown, needed. (I) ABS purp law flow < 4800 gpm low stem, turbine trip, suction phygodown value if needed. (I) ABS purp law flow < 4800 gpm low stem, turbine trip, suction phygodown value if needed. (I) Describe the steps in order, how to bring the unit up to full production after a short shutdown?

 Make some unit is correctly lind up. Trip checker. Vaccoum. ABS turbine (Jumming. Roll blowers) bring up to 500 pm. Start dryingtown pup. Get sandbow in service. Manifer 502 @ str-162
 - 5. List the #8 operating permit limits?

 Short term 502 init: 3.0 502/ton acid produced: 502 325.03 #/hr . 806.65 tons/yr

 Long term 502, init: 1.7 503/ton acid produced: NOx 14.65 #/hr . 4357 tons/yr

 Acid Mist limit: ,15/ton acid produced

 Operative LOB average for 5minutes

 May Production rate 2600 tol

 6. Describe the procedure on how to feed 20% Oleum on the Oleum tower to make 30%?

 Set the 84° a 48° values as desired. Adjust cooling when as dosired. Line up 20% oleum through the operator feel lie to the oleum tower. Switch feel from product to blow at the day tower feed loop. Horiter strength a lovelet tower + make adjustments as necessary. Ensure oleum is lined up to 77 took.
 - 7. The sulfur pump stops and will not restart and the spare is out of service. What would be your response? Shitoun & secure the unit

Name:	

65%/UP Operator Recertification Test

- 1. List the PPE required for starting a piece of equipment, after maintenance has worked on it, where a potential for acid exposure could occur? Hard hat, face shield, gapples, full Slicken Rubber books, rubber glows, Hood
- 2. What is the Mastercard permit system and why do we use it? A system for documenting lock outs / Tagorts to ensure that equipment is safely secured a deenergized prior to main tonce to prevent equipment damage or injuries
 - 3. What condition can occur at unit 8 that could shut 65% and UP down? Low \$250 show header. Power Confuse.
 - 4. What is the indication of a tube leak in the 30% vaporizer? Low ph in coil basin. Vaporize temperature a pressure spite. Low ph in coil basin.
 - 5. List the interlock valves in the 65% Oleum emergency shutdown system?

 Stean Control unlue & interlock value.

 30% Dleum feed control value & interlock calve.
- 6. How should you flush the 65% system for maintenance? Drain 5 ystan to 20% proposale. Close chair ine up flush acid to 30% feed lies line up unt but close last value into 20% proposale. Close chair value into 9 as line to TKUP & open gas values to 74 tank. Run acid through unit filling it up 50 aporices over flows into gas line them into 74 tank. Check for furning acid at Saple point to answer ystem is coupletely flushed of furning acid. The tank Tush acid a open drains to 20% propolar and up out system.
 - 7. How can you prevent the 65% coils from freezing?
 Keep work on the coils at all three and drain coils whenever is down
 - 8. Describe how to purge the evaporator? Make sure chat value in purge line from europarator is open. Open (CODI) as desired. Monitor purge tout leviel & temp. Allow purge flow into purge tout as lovel a temp permit. Adjust cooling water to purge tout if needed

#8 Operator Recertification lest Cont.

3) discharge or suction values closed, line break. Shutdown a secure unit. 5) ABS acity strength 99.1% to 99.4% - analyzer failure, loss of flow to analyzer, controller loft in manual, loss of where to purp tank. Correct rause of strength doisintion if possible, check simple flow a pull supples to check strength. Shutdown a secure unit if strength exceeds 99.9%.

UP Test

#10 Cont. - Place bother in overpack. Good suples are critical inorder to verify
the quality of the product.

9. What happens if you fire the pkg boiler too fast?

It can trip out

10. Describer how to control the 450/250/125 headers. What is priority? What does each affect?

Be specific? The \$450 header has a control value & manual waste value

Used to hold header @ \$450. Excess steem in the \$450 is durped into the

\$250. He \$250 header has a waste durp value that main tains the header

at \$250. The \$125 header is fed from the \$450 via the \$125 control

whoe \$4450 is priority. \$450; Blown, 500 kWS, jetajetors, SBFWpup, ABS builtee

250: 1500 kWO 65 Mpup. \$4125 steem fracing:

11. When should you open the bus tie? When should you switch panels form the generator bus, to the Utility bus? Dring fail weak. Swap panels to the utility bus on the Utility bus on the plant or can't supply power for the plant

12. When should you close the 2nd tie line? The GED KNG gres down. When the # Bunit hips out or the BED KNG gres down.

13. How many kw's can the plant carry without the risk of blowing a weak fuse?

Now KW load 13 3800 KW.

Name	e			Job Title				
Chec	k the	appı	ropriate l	boxes to Indicate the following:				
D = D	emo	onstra	ite; W = \	Written; V = Verbal; P = Pass; F = Fall				
No.	D	W	V	Job Procedures/Job Aspects			Date	
1				Unit Startup Procedure				
2				Unit Shut Down Procedure				
3			:	Oleum Tower Startup Procedure				
4			•	Diluter Startup Procedure				
5				#8 Boiler and Cooling Tower Water Tests				
6				Unit Heat Up Procedure				
7		,•		Unit Emergency Alarm and Shutdown Procedure				_
8				Unit Critical Operating Parameters				
9				Unit Interlock Matrix			·····	
10				Emergency Scenarios			~~~~	
11				Permit Limits				
12				Unit Safety Rules and PPE Requirements				
13				Life Critical Permit Procedures				_
14				Written Test				_
				(Circle One) Pass Fail				
Traine	ee's	Comr	ments:			,		
Trainee's Signature:			ture:	Datę:				-
Evaluator's Signature:			nature:	Date:				,

Demonstrate

The Operator will either perform or demonstrate how to perform the procedure

Verbal

The Operator will verbally answer the questions based n the procedure

Written

The Operator will take the final written exam

Pass

Greater than or equal to 80% of the answers are correct

Fall

Less than 80% of the answers are correct

Pass

#8 Operator Test

- 1. Explain the purpose and function of the following items:
 - Blower
 - Drying Tower
 - Furnace
 - #1 Boiler
 - Converter
 - #2 Boiler
 - Economizer
 - Absorbing Tower
 - · Brinks
- 2. Explain the purpose and the function of these parts of the steam system:
 - Steam Drum
 - Deaerator
 - Non-Return Valve
- 3. What are your responsibilities during a normal plant shutdown?
- 4. What are your responsibilities during an emergency shutdown?
- 5. Describe how #8 production rates are maximized via the SO₂ TPD.
- 6. What is the permit limit for stack opacity? SO2
- 7. Describe how to put the oleum tower in service to 77 tank.
- 8. Draw a block diagram of the #8 unit gas flow.
- 9. What are the different types of dilution water that can be fed on #8 pump tank.
- 10. List the interlocks that will trip #8 unit.
- 11. What is the maximum inlet acid temperature to the acid coolers?
- 12. At what temperature do you turn off the anodic protection on the acid coolers?
- 13. Explain what you would do if power could not be restored after a power failure.
- 14. What is the approximate strength of the acid that is circulating over the absorbing tower? Drying tower?

- 15. Explain what steps are necessary each time you open the bus tie, close the bus tie.
- 16. Describe how to put the diluter in service to 23 tank.
- 17. Describe what steps are necessary to switch feed on the oleum tower from product to 18 storage.
- 18. How do you adjust the amps on the sulfur pumps?
- 19. How could you tell if you had tube in the 65% oleum vaporizer?
- 20. The #8 stack opacity is suddenly rising. What are the possible causes and what action do you take? What do you do if the opacity continues to rise?

Ed Glasscock 10/25/04 #9 Operator Test D Blower - generates the gas flow for the unit. Draws in sir from the almosphere and pishes it thru the unit where it is converted ultimately into 503 which is used to make acid. Daying tower - This is where air drawn in from The atmosphere is dried Sulferic acid from the pump tank is recirculated over the top of the drying town while air is pushed up from the bottom out the duct lat the top. The acid absorbs the moisture in the air. Furnace - This is where sulfur is burned to create 502 905. #1 Boiler - 15 used to control the temperature of the 1st layer of the converter, waste heat is converted into steam for use throughout the plant. Converter - This is where the 50z 9as is converted to SO3 gas by passing it through layers of variation pentoxide catalyst.

2 Boiler - 15 used to control the temperature of the second layer of the converter. Again waste heat is converted into steam for use throughout the Economizer - This where the gas stream is cooled and the boiler feedware is preheated. The economizer is in effect a large exchanger Absorbing tower This is where the 503 gas stream passes up through acid which is recirculating lover the force, fortitying the acid

Brists - This is where acid mist is removed from the gas stream before moving on to the D Steam drum - This is the top drum of the boile where boiler water is boiled off into steam Co. Use throughout the plant

Deaerator - This is where air is removed

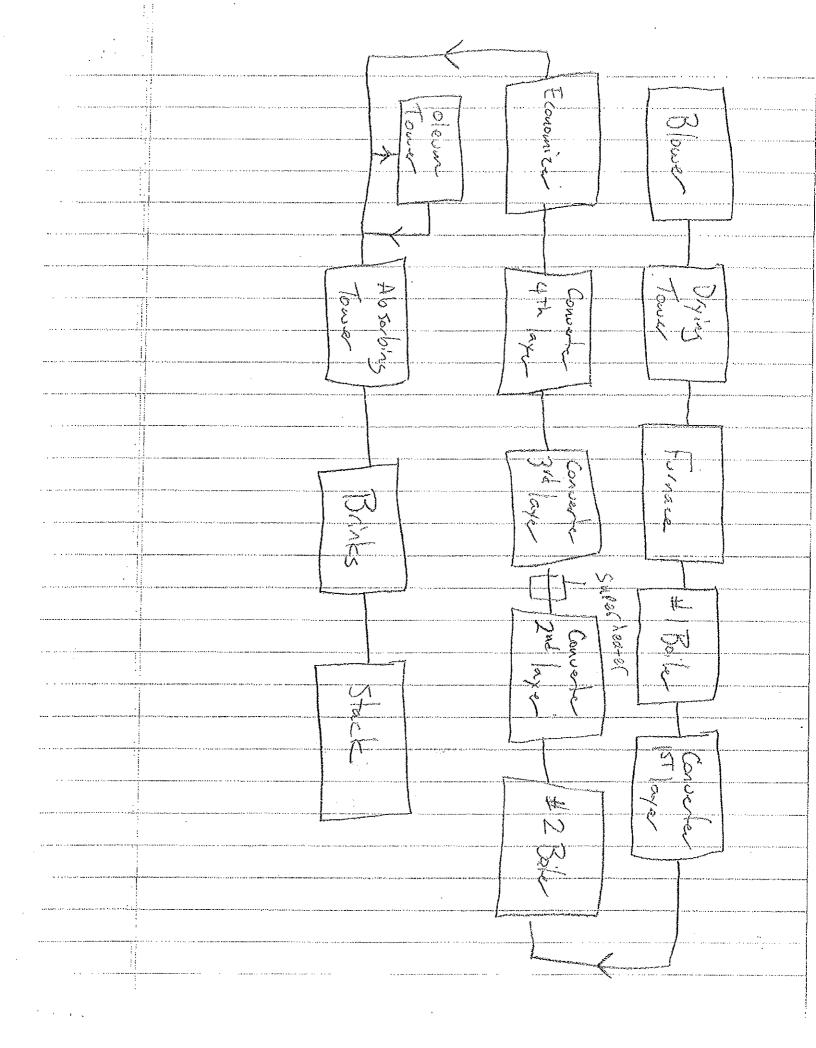
from the boiler water which could cause pitting on damage to the boiler. Also, the water is pre-booked and treatment chemicals are added in the dearrator, Non-return value - This value is located on the Steam header at the exit of the strain drum It is open during normal operation but during upset conditions when you can't get water into the beiler it is closed to ensure a water level remains in the boiler 3) To secure the unit with the shuldown checklist, Tip blower Ret appropriate controllers in manual aclosed Block in suffer al turnace, put steam on guns. Block in water to the pump tank, Shut down # 8 cooling tower a chanicals, Shutdown doying tower pump Close boiler exits. Close diving tower value. Shuldown condonser. Shuldown & secure Oleva lower Shutdown product pump. Block in acid lo #8 cooling tower Drain acid coolers. Close 84 value Secure diluter Switch la electric boster feed water pump

(4) Same as #3 plus assist utility operator with
Stean as necessary, monitor boiler steam dum level
Close non-return value if nocussary. Monitor stack emissions.
15 Monitor 502 TPD allowable us average reading on
emissions screen on compto. The average must stax
below the allowable. When the average comes within
ITPD of the allowable it will turn yellow indicating
that you are approaching the allowable limit and giving
you time to make adjustments. You may increase or decrease
blower speed or Evenace temperature as necessary
to maintain emissions within allowable limits, Increasing
blower speed or turnace temperature increases the production
rate
60<200 for 5 minutes < 3500ppm for 5 minutes
D Start oleum circulation pump. Set 84 value as desired. Line
up when to CIL cooler, Line up product feed to tower Line
up to 77 storage. Adjust acid inlet temperature to 100x + 110°4.
up to 77 storage. Adjust acid inlet temperature to 1004 + 1104, 45°4 across tower is maximum production. 1200 TPD is maximum to storage vale. Start amatrol.
to storage vale. Start anatrol
(8) Dec (as) Dage
B) See last page (D) Deepwell water, Demin water a process water. (D) MGB ESD hand switch Dodward governor tripped Suffer MGB lo lo oil pressure Abstancer lawflow 4900ppm Trip
(TO) MGB ESD hand switch Ward governor tripped
MGB lo lo oil pressure Abstance low flow 400pp Tois
MGB lo lo chest pressure Abstone low flow 3440 gpm trip
MGB hi vibration (200 more dage Hes) Sulfur inhat value closed X
-MGB hi discharge prossure 280° ESD hand switch in control room
Trip throttle value closed Boiler lo lo level 5w. 1ch
Trip throttle value closed Boiler lo lo level Switch Furnace temp > 1900° F Steam dum lo lovel 6.10°8
Ill winace temp

@ 195°f
(2) 120°€
3) Secure unit, monitor boile level, dose non-return
value if necessary - How downs
14 99.4 to 99.8 Abs 98.5 to 99.0 daying house
(5) Gen - fire package boiler, back down 5000 kwg
to plant load, trip bustie
Close - In Smitch gen 100m, Make sure all synch scopes:
one off, Bustie breaker scopion', synch in @ 12° clock position
Bus he breaker synch scope to off
To line up diluter to 23 tank. Put all consrollers in manual
and closed, Rush diluter reset. Line up acid to diluter and
establish flow, Line up dilution, water and start dilution
when pump. Line up cooling water. Set controllers as
desired. Wear ppe when lining up to 23 tank and
arid feed to diluter
Dow back blower as needed, open 84 value as desired,
Make adjustment on cooling when to CIL as necessary. Line
up 18 tank on operator feed line to down tower feed loop
Block in product food, line up OFL to tower. Monitor
strength and temperature in control room
Opening or closing the recirc unive. Opening = more than
= mory amps. 28 to 30 amps is desirable
19 Sudden temperature or pressure rise in the upprison,
low ph in 20% coil lasin. (D) Causes - Sean leat on sullingen, leat in economica check drains Corwale, low acid temperature in pump tank.
(10 Lauses) Jean leat on Sultur gun, leat in economica check drains
torwar, low acid temperature in pump tank.
Corrective action - block in steam to gun (should already be close)
Turn off fars and or pumps on \$1.8 cooling tower, if you can't stop

· · · · · · · · · · · · · · · · · · ·	
	rise cut off sultur. You may have to shut unil down if the rise continues.
	the rise continues.
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Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5. Operator Training Records
- 6, Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)



North American HSE SERVICES

To: B. McConnell

Date: October 31, 2012

From: G Baran

Subject: Houston site 2012 PHMP-FSA Report

The Rhodia Process Hazard Management Program (PHMP) Facilitated Self-Assessment (FSA) was conducted at the Houston site during September 4th, 5th, and 6th, 2012 by George Baran and Lou Higgins. This report summarizes the assessment. This FSA constitutes the OSHA-PSM and EPA-RMP compliance audit for the site, and certification of the evaluation of compliance with the requirements of these regulations.

The FSA covered the entire plant both covered and non-covered areas. The audit consisted of a review of the files (policy, documentation & procedures) including the last FSA in 2009 plus discussions with employees and plant supervision (Bill McConnell, Rob Stafford, Chester Farmer, Brett Jacks, Floyd Dickerson, Keith Praytor, Chad Smith, Drew Foster, and James Shaw) on PHMP issues and inspection of the sites maintenances files with John Willis and Steve Szabo.

The Houston site received a score of 95 acceptable PHMP items out of 129 PHMP items with 31 items needing improvement and 3 unacceptable items. The detailed FSA results can be found in the attached spreadsheet below.



Audit Results

The results are present in two categories (findings, and recommendations) and identify the key areas where the site should focus to enhance its process safety program. The unacceptable items are highlighted. An action plan should be developed in a timely manner to address the findings.

Findings: Those required to comply with OSHA-PSM and EPA-RMP regulations **Recommendations**: Those required for complying with Rhodia PHMP requirements only,

Findings (OSHA-PSM and EPA-RMP/CalARP requirements):

Process Safety Information – Chemicals

3.1 The current maximum inventories for chemicals in the process unit were not available for TS. A list needs to be compiled.

Process Safety Information – Technology

- 4.1 Block flow diagrams were unavailable for the oleum vaporizer. A diagram needs to be developed.
- 4.3 A chemical material of construction matrix needs to be developed for TS.

Process Safety Information – Equipment

5.2 Transfer of project files from engineering to the plant needs improvement.

Equipment files are missing on the TS risk 1 mitigation changes (valves and instruments installed), Regen 2 vapor combustor (seal pot and vapor combustor) and on the new sulfur tank vent changes to T-802.

- 5.3 TXUP P&IDs could not be found Need to determine and document electrical classification for the logistic barges and storage tanks.
- 5.8 Unable to find safety relief valve sizing for TS nitrogen relief valve and TS tank vacuum relief valves. Continue work of relief valve sizing throughout the plant
- 5.9 Unable to find SIL calculations for any safety interlocks.
- 5.10 Develop a complete written functional description of all safety system (SIS) in laymen terms including logic, computer code, and code function.
- 5.11 Develop a complete written functional descriptions of all safety interlocks in laymen terms.

Process Hazard Analysis (PHAs)

- 6.6 Unable to find PHAs for Regen 2 oleum before 2009. Check the files based on the 2009 PHA it was conducted in 2004.
- 6.7 Action tracking on PHA action items, recommendations, and human factors needs improvement. 65% oleum, Unit 8 oleum, TS, and Regen 2 oleum PHAs need follow-up on PHA items listed above.
- 6.10 PHA result need to be reviewed with affected personnel and documented.

Standard Operating Procedures (SOPs)

- 7.1 SOPs need to be updated to new format to meet regulations. Complete P&ID updating. Shutdown procedures must document personnel authorized to shutdown the unit. This is lacking in the Regen, Logistics, TS, and TXUP procedures.
- 7.2 SOPs need to be certified annually. Certifications could not be found.
- 7.3 COPs for TS and Logistics oleum need to documented in the SOPs

Training

- 8.3 Employee refresher training must be conducted every three years. Records could not be found in several areas (TS and logistics oleum). Check all area and conduct refresher training as needed.
- 8.4 Employees must be consulted on refresher training and this needs to be documented. No documentation exists.
- 8.5 All training must include the name of the instructor and the means used to verify the training was understood (tests results with a grade not pass or fail)

Contractors

9.6 Contractor evaluations are not be completed by engineering and only one was done by maintenance on the last turnaround. More contractor safety evaluations need to be completed.

Pre Start-up Safety Review (PSSR)

- 10.5 No records could be found that employees and plant supervision were trained on the pre start-up safety reviews.
- 10.7 No follow-up (action tracking) on B items identified on PSSRs. A items identified on the PSSR are required to be completed prior to start-up
- 10.10 Expand use of PSSR to include all physical equipment and instrument changes

Management of Change (MOCs)

11.7 Several temporary MOCs are open past due dates. Make sure all temporary MOCs are not open beyond identified dates.

Mechanical Integrity

- 12.3 Transfer of engineering files to the plant needs improvement. Files on instrumentation could not be found for new projects (TS risk1 mitigation changes, Regen 2 VCU project and new sulfur tank project)
- 12.4 Transfer of engineering files to the plant needs improvement. Equipment specification files are not complete to covered area. Unit equipment files were missing in all areas. The files need to be reviewed for completeness and updated accordingly.
- 12.9 Document missing on initial testing missing or inadequate on 4 projects checked (TS risk 1 modifications, barge vent testing, VCU redesign, and the new sulfur tank project) barge Improvements are needed in interlock and alarm testing. None of the units have DCS interlock or alarm testing records except TXUP

Incident Investigations

14.3 Action items on incident investigation not tracked to completion. Open items from incident investigations need to be tracked.

Compliance Audits (FSA)

16.4 All action items from the 2009 FSA have not been completed. Open items need to be tracked to completion.

Recommendations (Rhodia PHMP requirements):

Safety File Management Systems

- 1.4 The safety file system needs to be updated with current information and locations of electronic files.
- 1.7 The site needs to expand the use of the action tracking database to include PHA action items, recommendations, human factors and sitings findings, plus open PSUSR items and MOC items.

Process Safety Information - Equipment

5.4 Unable to find electrical classification drawings for spent acid. Other drawings found need updating.

Pre Start-up Unit Safety Review (PSSR)

- 10.8 No documentation could be found that results of PSSRs were communicated to Affected. Document communication of PSSRs.
- 10.9 No records could be found that the PSSR process was audited to ensure Proper procedures were followed and all open items were completed.

Management of Change MOCs

11.6 Need to establish time frame for emergency changes to issue MOCs.

An action plan should be developed in a timely manner to address the findings, which identify the key areas where the site should focus to enhance its process safety program. Please contact me if you have any questions or need further assistance with any of the findings and/or improvement options.

G. Baran



North American HSE SERVICES

To: B. McConnell Date: November 9, 2009

From: G Baran Subject: Houston site 2009 PHMP-FSA Report

The Rhodia Process Hazard Management Program (PHMP) Facilitated Self-Assessment (FSA) was conducted at the Houston site (note best practices were not audited) during September 22, 23, and 24, 2009 by Bala Balachandran, and George Baran. This report summarizes the assessment. This FSA constitutes the OSHA-PSM and EPA-RMP compliance audit for the site, and certification of the evaluation of compliance with the requirements of these regulations.

The 2009 FSA for the Houston site covered the entire plant and was broken down into 6 areas Regen including oleum, Treatment Services (TS), Logistics, Unit 8 including oleum, 65% Oleum and TXUP. The audit consisted of a review of the files (policy, documentation & procedures) including the last audit plus discussions with plant supervision (Bill McConnell, Mark Miget, Rob Stafford, Jim McCreight, Thaun Nguyen, Chester Farmer, Frances Romero, Jimmy Wooden, John Willis, Donna Schultz, Brett Jacks, Tim Collins, Wesley Carter, Kevin Copeland, Bryan Cecil, Ken Oliver, Keith Praytor, and James Shaw) on PHMP issues and a tour/inspection of the site with operator and maintenance interviews (Chris Stocks, Robert Brown, Paul Barrnet and Kyle McCafferty).

The Houston site needs to improve their process safety program and has only met minimum standards in 5 of the 17 applicable elements with an unacceptable rating for relief valve sizing and sizing basis in all units (no documentation available) except 65% oleum. The detailed FSA results can be found in the attached spreadsheet below.



Audit Results

The results are present in three categories (findings, recommendations, and improvement options) and identify the key areas where the site should focus to enhance its process safety program. An action plan should be developed in a timely manner to address the findings.

Findings: Those required too comply with OSHA-PSM and EPA-RMP regulations **Recommendations**: Those required for complying with Rhodia PHMP requirements, **Improvement Options**: Those not required, but offer opportunity for further improvement.

Findings (OSHA-PSM and EPA-RMP/CalARP requirements):

Safety File Management

 OSHA PSM and EPA RMP coverage determination documents need updating and awareness training is needed throughout the site on this determination

Process Safety Information - Chemicals

 The current maximum inventories for chemicals in the process unit were not available for Regen, TS, Logistics, and TXUP. This need to be available.

Process Safety Information - Technology

- Block flow diagrams were unavailable for TS. Diagrams need to be developed.
- A written description of the TXUP process chemistry was unavailable. This
 documentation needs to found or developed (see spread sheet for details)
- Critical operating parameters (COPs) for TS and Logistics were unavailable. COPs need to be determined and documented for these units.
- Material and energy balances for the TXUP unit need to be developed and placed in the unit safety files.

Process Safety Information - Equipment

- Need to determine and document electrical classification for the logistic barges and storage tanks.
- Need a written procedure for bypassing safety interlocks
- Equipment files need to be checked for completeness files were found missing in all units especially TXUP which could not be found. The TXUP files need a major overhaul.
- Relief valve sizing calculations and the sizing basis was not available in all area except 65% oleum. This is unacceptable and the documentation must be developed.

Process Hazard Analysis (PHAs)

• A management system needs to be put in place to timely address the findings from PHAs including sitings and human factors.

Standard Operating Procedures (SOPs)

- Emergency shutdown procedures must document personnel authorized to shutdown the unit. This is lacking in the Regen, Logistics, TS, and TXUP procedures.
- Definitions of COPs needs to be improved in the TS, Logistic, and TXUP procedures.
- Continue work on updating the unit SOPs throughout the plant into the format

Training

 Employees must be consulted on refresher training and this needs to be documented. No documentation exists for Unit 8, 65% Oleum and TXUP.

Contractors

Procedures for contractor IH certifications and record keeping needs to be updated
with personnel training on the procedures to ensure compliance. There is confusion
in all areas of the plant involved in this process including the engineering platform
and corporate purchasing.

Mechanical Integrity

- Unit equipment files were missing in all areas. The files need to be reviewed for completeness and updated accordingly.
- Improvements are needed in interlock and alarm testing. None of the units have DCS interlock or alarm testing records except TXUP
- Site needs a procedure on MOC work orders with training of all personnel.
- Continue work on developing an interlock matrix for each unit

Work Permits

Training documentation of personnel on work permits needs improvement. The
training conducted (permit specific), dates, names of personnel trained, the name
of the instructor, and method to insure effective training all needs to be
documented.

Management of Change (MOCs)

• Target date for completion needs to be added to the MOCs. — This is a corporate wide issue being addressed by process safety shared services.

Emergency Plans

• Emergency equipment needs to be inspected to ensure readiness when needed. No inspection records were available

Audits

 No action plan or documentation on address the finding from the 2003 FSA could be found.

Recommendations (Rhodia PHMP requirements):

Safety File Management Systems

 The safety file system needs to be updated with current information and locations of electronic files.

Process Safety Information - Technology

 Chemical material matrix was unavailable and needs to be found or developed for Regen, TS, Logistics, Unit 8 and 65% Oleum.

Process Safety Information - Equipment

- A list of all equipment with materials of construction was not available and needs to be developed for all units.
- Unit 8 and TXUP should maintain current P&IDs showing fail-safe positions for actuated valves (or a referenced valve specification sheet indicating fail-safe position)
- Safety integrity levels for safety instrumented systems in all areas should be documented

Process Hazard Analysis

- Risk sheets should be updated and revised as mitigation activities are completed
- · Risk sheets need to be signed by the plant manager

Training

 A written training program for the site needs to be developed (see spreadsheet for details)

Mechanical Integrity

 Safety Integrity Levels should be determined for safety systems, and safety systems should be inspected at the appropriate frequencies

Improvement Options (opportunities for further improvement):

Safety File Management

- Files for the annual process safety plan needs to centralized and break out process safety being unit specific.
- Specific measurable goals for process safety stop at the superintendent. They include all the production engineers and supervisors.

Process Safety Information – Chemicals

· Written Haz-Com procedures need updating

Process Safety Information - Technology

 Unit safety files for all units need to point to manufacturing solutions for current incident investigations

Contractors

- Site contractor policy is out of date and needs updating
- Conduct additional contractor performance evaluations

Pre Start-up Unit Safety Review (PSUSR)

Get rid of the old short form still in the Lotus Notes Platform database

Mechanical Integrity

- Mechanical Integrity written program needs updating
- Inactive equipment should be removed from the equipment list as it is removed from the unit and clearly identified as inactive if it is still in the unit process areas
- Work Order system should the name of the person performing the work on the work order
- The procedure of handing projects over from the platform to the operating units needs an overhaul.

Management of Change MOCs

- MOC procedure out of date needs updating
- MOC audit should not be part of the FSA as documented in the procedures. This is a separate plant audit.

Incident Investigations

- Procedures need to updated and reference manufacturing solutions
- Documentation on incidents reviews in safety meeting needs improvement. The safety meeting must document the Incidents reviewed by number not just say incidents were reviewed.

An action plan should be developed in a timely manner to address the findings, which identify the key areas where the site should focus to enhance its process safety program. Please contact me if you have any questions or need further assistance with any of the findings and/or improvement options.

G. Baran

ECO Services Project Action Form



Created by William McConnell on 02/19/2010 at 03:48:33 PM









Status:	Completed	Priority: Medium			
o carcos.	compicação	1330TCy 777.33CG3GE			
Completion Date:	04/12/2012				
Completion Date:	04/12/2013				

Action Tracking ID: PAT-ECO-HO-10-2 Site:

Responsible Department: Office/Administration

Category:

Safety Audit

Sub-Category: Team Name:

Houston Management Team

Audit Name: FSA Audit

Project Title: Response to Houston 2009 FSA Audit

Task Summary Description: This project will be used to track responses to the 2009 FSA Audit. Assigned individuals are

responsible for seeing the action items get the resources needed to get them done. Put responses including diagrams, calculations, etc. in this document. Also put the responses in the appropriate section of Lotus Notes, equipment files, or the Lan in the S-Drive/Process Safety/FSA section. This

project action tracker only addresses findings. It is not meant to address recommendations.

Target completion of all items if September 1, 2010.

Further Details:

Attachments

Title

Assigned By:

Houston 2009 FSA Audit Report

Attachment ക്ക Hou_2.doc

Author

William McConnell on 02/19/2010

Project Manager: William Date Assigned:.. 02/19/2010

McConnell

William McConnell Action Due Date: 09/01/2010

cc List: George Baran Action Notification Date: 07/01/2010

Num	Task Description	Project Tasks: Responsible	43	Due Date	Status Link
1	Update OSHA PSM and EPA RMP coverage determination	William McConnell	. A	05/28/2010	08/25/2010 <u>Link</u>
2	Calculate current maximum inventory levels for chemicals in	Jim Cesen	л ц	04/01/2010) _{12/29} /2012 <u>Link</u>
3	Calculate current maximum inventory levels for chemicals in	Drew Foster	D T	04/01/2010	08/25/2010 <u>Link</u>
4	Calculate current maximum inventory levels for chemicals in	Brett Jacks	* ±	04/01/2010	08/10/2010 <u>Link</u>
5	Calculate current maximum inventory levels for chemicals in	im Cesen	я " 👗	12/31/2012) _{12/03} /2012 <u>Link</u>
6		Jim Cesen	. A	Œ	08/25/2010 Link
7	A written description of the TXUP process chemistry needs to be	Drew Foster	. <u>1</u>	06/01/2010	09/03/2012 Link
8	Critical operating parameters (COPs) for Treatment Services	Brett Jacks	. Å	06/01/2010	08/30/2010 <u>Link</u>
9	Critical operating parameters (COPs) for Logistics need to be	» Jim Cesen	5 <u>\$</u>	06/01/2010	11/30/2012 Link

10	Material and energy balances for the TXUP unit need to be	5	Brett Jacks	15 A.	06/01/2010 09/03/2012 Link
11	Determine and document electrical classification for the logistic	S	Robert Stafford	lz van	06/01/2010 (m) _{12/31} /2012 <u>Link</u>
12	Need a written procedure for bypassing safety interlocks.	E F	Jim Cesen	8 8	06/01/2010 📵 _{12/20/2010} Link
13	Equipment files need to be checked for completeness. Make	a H	Drew Foster	e &	09/01/2010 11/30/2012 Link
14	Equipment files need to be checked for completeness. Make	P	Brett Jacks	n 👗	09/01/2010 (12/21/2012 Link
15	Equipment files need to be checked for completeness. Make	B ·	Jim Cesen	n B	09/01/2010 (a) 12/07/2012 Link
16	Equipment files need to be checked for completeness. Make	5	Jim Cesen	. .	09/01/2010 @ 09/03/2012 Link
17	Equipment files need to be checked for completeness. Make	B .	Jim Cesen	n	09/01/2010 (09/03/2012 Link
18	Equipment files need to be checked for completeness. Make	B A	Jim Cesen	<u>.</u> .	09/01/2010 @ 09/03/2012 <u>Link</u>
19	A management system needs to be put in place to timely address		Jim Cesen	. A	09/01/2010 08/25/2010 Link
20	Emergency shutdown procedures must document personnel	D	Brett Jacks	, z	06/01/2010 (11/30/2012 Link
21	Emergency shutdown procedures must document personnel	B	Drew Foster	s 	06/01/2010 11/06/2012 Link
22	Emergency shutdown procedures must document personnel	n n	Jim Cesen	n	06/01/2010 (12/21/2012 Link
23	Emergency shutdown procedures must document personnel	E .	Drew Foster	в Д	06/01/2010 (a) 12/21/2012 Link
24	Definitions of COPs need to be improved. Treatment Services.	B #	Brett Jacks	# Å	09/01/2010 (a) 08/30/2010 Link
25	Definitions of COPs need to be improved. Logistics	5 3	Jim Cesen	я _ А	09/01/2010 🗐 12/21/2012 <u>Link</u>
26	Definitions of COPs need to be improved. TXUP.	e 0	Jim Cesen	n <u>a</u>	09/01/2010 (a) 09/03/2012 Link
27	Update SOP's throughout the plant into current format. Regen and	n p	Drew Foster		09/01/2010 (m) 12/21/2012 Link
28	into current format. Treatment	5 £	Brett Jacks		09/01/2010 (12/21/2012 Link
29	Update SOP's throughout the plant into current format. Logistics.		Jim Cesen	о Д	09/01/2010 (08/11/2011 Link
30		s 2	Jim Cesen	b = &	10/31/2010 @ 09/03/2012 Link
31	Update SOP's throughout the plant into current format. 65% Oleum	H F	Jim Cesen	ь Б	09/01/2010 (12/21/2012 Link
32	Update SOP's throughout the plant into current format. TXUP.	E .	James Wooden	и В	12/02/2012 (a) 12/17/2012 <u>Link</u>
33	Update SOP's throughout the plant into current format. No. 8 Unit	5 5	Keith Praytor	а 7	09/01/2010 🗐 12/21/2012 Link
34	Employees must be consulted on refresher training and it needs	 22	Robert Stafford	21 A.	06/01/2010 @ 09/14/2010 <u>Link</u>
35	Procedures for contractor IH certifications and record keeping	8 8	Robert Stafford Jim Cesen	» Д	07/01/2010 @ 08/31/2010 Link
36	Unit equipment files were missing in all areas. The files need to	p 	Keith Praytor		09/01/2010 (m) 07/22/2010 Link
37	Improvements are needed in interlock and alarm testing.	E	James Shaw	п Б	06/01/2010 (m) 12/19/2011 Link
38	Site needs a procedure on MOC work orders with training of all	B B	Jim Cesen	iz 🔻	06/01/2010 (10 08/31/2010 Link

39	Training documentation on personnel on work permits needs	B	James Shaw	B B		05/01/2010 (a) 01/16/2013 Link
40	Target date for completion of MOC's need to be added to each	5	William McConnell	# #	4	09/30/2010 (a) 08/25/2010 Link
41	Emergency equipment needs to be inspected to ensure readiness	9	Drew Foster	2	Å	06/01/2010 (10/15/2010 Link
42	No action plan or documentation on addressing the findings from	B		p	A	05/01/2010 (08/25/2010 Link
43	Create block flow diagrams for Treatment Services.	п В		6	A.	06/01/2010 @ 08/25/2010 Link

Task Progress and Attachments	
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Log Type	Task	Statue	Log Fotov	Attachment Title	Attachment	Author
nog rype	Trisk Training documentation on personnel on work permits needs improvement. The training conducted (norm) specifical dates	Status	Log Entry	Attachment Title	Attaclusent	
Compi Log	(permit specific), dates, names of personnel trained, the name of the instructor, and method to insure effective training all needs to be documented.	Completed	[No Comments submitted]			James Shaw on 01/16/2013
Compl Log	Determine and document electrical classification for the logistic barges and storage tanks. Calculate current	: Completed	Per progress log entry: conservative classifications implemented. See 2013 Tracked M[more]	e		Robert Stafford on 12/31/2012
Compl Log	maximum inventory levels for chemicals in the process unit at Regen	Completed	Chad Smith completed on 12/28 - copy on the S drive and in the regen2 file cabinet			Jim Cesen on 12/29/2012
Compl Log	Definitions of COPs need to be improved. Logistics	Completed	done - see progress log attached below for matrix compiled by Adam Daniels			Brett Jacks on 12/21/2012
Compl Log	Emergency shutdown procedures must document personnel authorized to shutdown the unit. Treatment Services.	Completed	all TS procedures include this statement - "All T.S. Operators are responsible for un[more]			Thuan Nguyen on 12/21/2012
Compl Log	Update SOP's throughout the plant into current format. Treatment Services.	Completed	complete - S:\TS\Procedures\Controlled Documents			Thuan Nguyen on 12/21/2012
Compl Lag	Equipment files need to be checked for completeness. Make sure all necessary files are complete. Relief valve sizing calculations and	Completed	supporting docs found at S:\Process Safety\Relief Calcs\TS			Thuan Nguyen on 12/21/2012
Consulta-	the sizing basis need to be complete. Treatment Services. Update SOP's throughout the plant into current	Constant	completted at			Jim Cesen
Compl Log	format. No. 8 Unit and oleum system. Update SOP's throughout	Completed	S:\#8 unit\SOP's\Unit 8			on 12/21/2012
Compl Log		Completed	complete at S:\#8 unit\SOP's\65 %			Jim Cesen on 12/21/2012
Progress Log	maximum inventory levels for chemicals in the process unit at Regen		Chad working on it, model built, Albert assisting with burn-rite, about 50% complete[more]			Jim Cesen on 12/21/2012
Compl Log	authorized to shutdown the unit. TXUP.	Completed	completed, in HQ-UNIT8-SOP012- TXUP.			Jim Cesen on 12/21/2012
Compl Log	Update SOP's throughout the plant into current format. Regen and oleum system.	Completed	completed and uploaded to lotus notes (also on S:\#2REGEN\Procedure on new Format 200[more]			Jim Cesen on 12/21/2012
Compl Log	Update SOP's throughout the plant into current format. TXUP. Equipment files need to	Completed	Procedures have been updated and are on the S drive			Drew Foster on 12/17/2012
	be checked for completeness. Make sure all necessary files are	Completed	All logistics PSV calculations are located on the S drive at the follow location: S:\[more]			Adam Daniels on 12/07/2012
Compl Log	including oleum system. Calculate current maximum inventory levels for chemicals in the process unit at TXUP.	Completed	Performed Max Capacity Calculations for TXUP	TXUP Max Capacity	TXUP .xlsx	Drew Foster on 12/03/2012
Compl Log	documented for this	Completed	[No Comments submitted]	Logistics COP matrix 2012	ழ Logis.xlsx	Adam Daniels on 11/30/2012
Progress Log	area. Critical operating parameters (COPs) for Logistics need to be determined and documented for this area.			Logistics COP Matrix 2012	D Logis.xlsx	Adam Daniels on 11/30/2012

Overall Progre	ess and Attachments	A Division and the second seco	ng may ng ng nggg pa philipsag draig draidh de in dea aduidh draidh dhaidh		ng taobranian randark (19 dan) aman ay akan bana dan ana
No Entries					
F	etion Statement				
Status Completed	Log Entry Cleaning up the database, I noticed this project was	Attachment Title	Attachment	Author William McConnell	Add Response
	Recreate Project Recreate Project Recreate Project with Assignees	(2) Help	:	Print	(a) Home
Edit History					

PROCESS HAZARD MANAGEMENT PROGRAM FACILITATED SELF ASSESSMENT

Introduction

The PHMP Facilitated Self Assessment measures the progress towards implementing a comprehensive process hazard management program.

The assessment evaluates current status against minimum standards established in PHMP and also process safety elements

The tool can be used to evaluate a single unit or process or the entire site. It incorporates PHMP, Responsible Care® elements, CCPS and other industry practices into a comprehensive process safety evaluation tool. It is meant to evaluate not only the "quantity", but also the quality of a site's program.

The tool can be used to facilitate continuous improvement of all process safety management elements.

The tool can also be used for technology assessment on a unit or process.

It also is used as a compliance assessment for 29 CFR 1910.119 (OSHA PSM Standard.) as required by section 0, 29 CFR 1910.119(o).

The tool is meant to be used by site management to critically assess their process safety program. An outside facilitator assists in this evaluation to bring consistency between sites and units, but the site must participate in an open, self critical manner in order to achieve understanding and buy-in.

Methodology

The various sections within the facilitated self assessment correspond to the sections of PHMP.

The site's or unit's program elements are to be assessed versus the minimum standards and some best practices by using common auditing techniques including;

review and verification of procedures, records and supporting documentation, interviews with employees and observations of on-site conditions. Site participation during the assessment must include personnel knowledgeable in the process or unit being assessed.

Each section will receive a score or rating. Minimum standards will be assessed first. Each minimum standard that is met will be given a score of acceptable. All minimum standards within a section must be met to achieve an acceptable score of for that section. Certain minimum standards may be not applicable at a site and in such a case will not be counted. Periodically new minimum standards will be added to the assessment. During the first year after addition the new minimum standards will not be rated unless required by regulation. They will appear in the tool as New "Year" (ie New 2011). If a plant does meet the new standard it will initially be rated in-place. See the table below for more details.

The individual sections are weighted in determining the overall plant or unit rating

The weightings are based upon the relative importance of each section.

Output

The output of the assessment process will be a summary report of the various elements, the completed assessment tool, individual section scores and an overall composite rating. The report will list all items where minimum standards were not met.

The PHMP-FSA and subsequent report can be used to meet requirements for OSHA Process Safety compliance auditing

Scoring Key

Score	Key
Acceptable	Meets all requirements
Needs Improvement	Action plan in progress or minimum standard partially met or implemented
Unacceptable	Minimal or no progress toward minimum standards



Chemistry is our world, Responsibility is our way

North America Process Hazard Management Program (NA PHMP)

Facilitated Self-Assessment

Facility Name: Houston

Date: September 4, 2012

Auditors' Names: George Baran and Louis Higgins

TOTALS

Acceptable 95

Needs Improvement 31

Unacceptable 3

Not Applicable 1

Name:	Houston	Date:	9/4/2012	Ì						
Blement	Safety File Management System	ļ								
Requirem	ent	Status		Applic	able Standards	Guid	elines	Criteri	a for Implementation	Comments
1.1	Responsibility for Process Safety activities clearly defined, assigned and understood	1.1	Acceptable		PR 501 PR 502	1.	Employees must be aware of activities covered under Process Safety Management coverage at the facility Responsibilities must be defined for areas covered under Process Safety Management		Auditors must assess PSM knowledge from interviews with employees By M Training records must exist for each employee Documentation must show all PSM responsibility for all PSM covered areas and elements	
	The skills required for various process safety management assignments/responsibilities are defined and training is conducted for assignees as required.	1.2	Acceptable		PR 500 PR 501 PR 502	1.	2 Skills must be defined for all employoes parfroming Process Safety Functions		Documentation must exists showing the requirements for all employees with process safety responsibilities	
1.3	OSHA PSM coverage determined for all units and documented	1.3	greetable	İ	29 CFR 1910.119(a) PR 501 PR 502	1.	Documentation must exist defining the coverage of all units at the facility		Documentation must show PSM coverage on all processes	
1.4	Unit safety file concept established and functioning	1.4	Needs Improvement	1.4	PR 501	1.	4 Each unit must have a Unit Safety File	1.4	Unit Safety Files must exist for each unit	File links and documents need to be updated
	An annual process safety plan is established, communicated to all employees and performance against plan is documented and communicated. Plan covers activities for upcoming year.	1.5	Accretic	1.5	PR 501	1.	5 the site must create a Process Safety Plan annually and communicate the plan to the employees. The facility's progress toward the plans goals must be documented and communicated to the employees. The plan must include various areas of Process Safety Management, specifically - Process Hazard Analyses - Audits - Training - Management of Change		Documentation must exist showing a. The Process Safety Plan (including an action plan) b. Progress toward the plan c. Records documenting communication to plant employees	
	Specific measurable goals for Process Safety Management performance are established and ovaluated annually for appropriate management and staff personnel	1.6	Acceptable		PR 501 PR 502	1.	G The sito must annually create Process Safety goals that include the following: - Written Process Safety Objectives for individuals or departments with measurable goals - Goals and Action Plans are tracked for completion for progress - Management review		Auditors will review completed the Process Safety Plan Review Process Safety objectives for the technical manager or site "Process Safety Coordinator" for MOCs	
	An electronic action tracking system is used including process safety issues, as needed	1.7	Needs (mixevement	1.7		1.	7 The site must used an electronic tracking mechanism for all Process Safety Related action (toms		Utilization of Manufacturing Solutions of a similar system	FSA, MOC, PHAS , PSUSR

Page 2 of 28

Name:	Houston	Date:	9/4/2012	1				II		
								<u> </u>		
Element:	Employee Participation		l	ļ				ļ		
220000000000000000000000000000000000000		d.	į				•		icria for Implementation	Comments
Requirem	ent	Status	ı	ybbre	able Standards	Stria	lines	S. Carlle	ena for imprementation	Continents
2.1	Written Employee Participation program is in place	2.1	Acceptable		29 CFR 1910.119(c)(1) FR 503	2.	A written program must exist documenting how employees are included in the PEMMP process - The written program must cover employee participation in all elements of the site's PEMMP - The written program should describe how employees, including contract employees, are consulted in various areas of the program		2.1 The site must create a written program that addresses employee participation in all elements of the site's PHMP Supporting documentation must show employee participation in various areas of the program	
	Employees (and contractors) have access to all program documentation	2.2	Acceptable		29 CFR 1930.119(c)(3) PR 503	2.	Documentation must be readify assessible to all employees	1	2.2 Employees must demonstrate their ability to access PHMP related information	
	Written program clearly delines HSE (including process safety) responsibilities for all employee	2.3	Acceptable	2.9		2.	Document must exist defining each employee's HSE responsibilities	7	2.3 The site must croate a document defining the HSE responsibility for each employee	
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Employee Partic.

Name:	Houston	Date:	9/4/2012						
171amanti	Process Safety Information - Chemicals								
J. K. ISICOTI	THOUSE SALETY THE HEALTH CALL THE ASS						1		
Requirem	ent	Status		Applicable Standards	Guide	lines	Crise	ria for Implementation	Comments
3.1	Facility maintains a current list of all chemicals, associated maximum inventories (including reaction products) and intended use.	3.1	Freeds improvement	3.1 PR 504 (3.1)	3.1	Maintain documentation of chemicals at the facility including, inventory amounts, locations, and intended luse	3	The site should review the list on a regular basis and document the review The review should be included in the MOC process whenever there are changes in raw materials or finished speeds.	A complete list of TS chemicals and maximum inventories is needed
3.2	Current MSDS for all chemicals are readily available on the site network.	3.2	Acceptable	3.2 29 CFR 1910.119(d)[1] PR 504 (3.2)	3.2	Maintain electronic copies of all MSOSs and ensure that they are readily available to all employees	3	2 Document a system for ensuring all MSDSs are added to the electronic "database" The system should include a process to ensure the most recent MSDS is available	
	Material hazard information located on Material Technical Shoets and/or Reaction Sheets, or other documents, are available for all hazardous chemicists in cases where the hazard information located on the MSDS is inadequote, including the following in the case of MTSs. - A rationals for determining when Material Technical Shoets are needed, is available - information is completed on Material Technical Shoets - References are indicated on the MTS	3,3	Acceptable	3.3 29 CPR 1910.119(d)(1) PR 504 (3.3)	3.3	Material Technical Sheets are maintained for all hazardous chemicals A procedure exists documenting how Material Technical Data Sheets are maintained	3	3 The site must have a system for mointaining Material Technical Sheets. A procedure/policy must exist which states the rationale for determining when a MTS is required. The Material Technical Sheets procedure includes the following: - Information is completed on Material Technical Sheets - References are indicated on the MTS	
	Operators understand how to access MSDSs and the chemical hazards listed on the MSDS	3.4	Acceptable	3.4 PR 503	3.4	All employees must have a working knowledge of MSDS and chemical hazards, specifically the employees listed below - Operators - Technical testf - Maintenance	3	4 Documentation inust exist showing training in hazard communication Eraployees must demonstrate the ability to locate and understand a MSDS	
3.5	Process hazards are documented and available	3.5	Acceptable	3.5 29 CFR 1910.119(d)(1) PR 504 (3.3)	3.5	Documentation includes the following: - Toxicity, reactivity, and corrosivity information - Pernissible exposure limits - Hazardous effects of inadvertent mixing - Stability data	3	5 Process hazards should be documented and readily available to all employees The Information should include more than a MSDS, however if all of the required information can be found on a MSDS, a MSDS is acceptable for all products and raw materials in the process	
	A system or process is established to identify new hazards in the process or reactive chemicals introduced to the site, changes to current inventory, identify HSE impacts and approve introduction.	3.6	Ac atriable	3.6 29 CFR 1910.119()(1) PR 514	3.6	The system identifies new hazards: a. In the process or reactive chemicals being introduced to the site b. due to changes to current inventory AND identifies HSE impacts and requires approval prior introduction.	3	6 New hazards should be introduced using the MOC process and/or a PHA There should be no instances where a new hazard was not reviewed win the MOC process at a minimum	
3.7	All process safety information is made available to employees	3.7	Acceptable	3.7 29 CFR 1910.119(c)(3) PR 503	3.7	All PSI should be readify available at within or near the process	3	7 Operators should demonstrate ability to easily obtain process safety information	Review with affected personnel

PSI - Chemicals

Name:	Houston	Date: 9/4/2012				į		
Element	Process Safety Information - Technology	-				-		
Requireme	ent	Status	Applicable Standards	Guide	lines	Criteri	a for Implementation	Comments
4.1	The facility must maintain Block Flow Diagrams for each process in the facility	4.1 Needs improvement	4.1 29 CFR 1910.119(d)(2)(I)(A) PR 505 (4.1)		Block flew diagrams (or Process Flow Diagrams) must exist for all processes indicating: - the unit operations in the process - the ways the operations are related to each other the materials fed to, recycled, and discharged from the process		The facility must create and maintain block flow diagrams for all processes in the facility The block flow diagrams must be roadily accessible	Oleum vaporizer block flow diagram could not be found
4.2	The facility must maintain documentation of all process chemistries at the facility - This documentation can be in the form of Reaction Sheets	4.2 Aceptable	4.2 29 CFR 1910.119(+)(2)(!)(B) PR 505 (4.2)	4.2	Written descriptions of the process chemistry(ies) must include the following: - Reactions and blends - Side reaction, wastes and by-products - Operating conditions - Haararks of the reaction (or blend) process - Heat of reaction [mining)		The facility must document the process chemistry for each menofacturing process within its bounds. The process chemistry information should be included with the process's other process safety information.	
4.3	The facility must maintain documentation on all possible chemical interactions	4.3 Needs Improvement	4.3 29 CFR 1910.119(d)(1)(II) PR 505 (4.2 & 4.3)	4,3	A written matrix should exist documenting all possible interactions including - Chemical / Chemical - Chemical / Material of Construction		The facility must create a matrix showing the reactivity of the material with other chemicals and materials	No chemical/material of construction matrix for TS
4.4	Critical operating parameters must be documented and made available to employees	A.A Arreptable	4.4 PR SOS (4.4)	4,4	The documentation of Critical Operating Parameters should include the following: - Maximum normal operating limits: - Operating adjustments to be implemented once maximum normal operating limits are exceeded. - Never Exceed Limits: - Immediate actions required when the Never Exceed Limits reached: - Safe Operating Limits: - Description of the safety interlock system		Critical Operating Parameters must be identified and documented These COPs must be made readily available to all applicable employees The facility has a documented basis for Never Exceed Limit of the COPs such as: - Experimental data - Models and/or calculations - Physical properties.	Continue work in progress to update COPs for lagistics
	The facility must document all incidents associated with each process	4,5 Acceptable	4.5 29 CFR 1910.119(m)(4) 29 CFR 1910.119(m)(7) FR 504 (4.8)	4.5	Document all incidents and make them readily available		The facility must utilize an electronic system to document each incident associated with each process	
4,6	The facility must maintain Material and Energy Balances for each process built after 1992 - For a small facility the Material and Energy Balance could be on a flow diagram	4.6 Acceptable	4.6 29 CFR 1910.119{d}(3)(II)(G) PR 505 (4.6)		Create a Material and Energy Balance for each process built after 1992 - The Material and Energy Balance should be updated as changes occur in the process	4.6	Material and Energy Balances should be documented for each process built post 1992 - Material and Energy Balances should be reviewed and undated via the MOC process	
4.7	The facility has a process for identifying the necessary process safety telermation	4.7 Acceptable	4.7 PR 505 (4.7)		The site has a documented system for: - Determining what reactivity, stability, decomposition for other essential process safety) data is necessary - Obtaining such data - Evaluating data for process safety issues - incorporating such information into the new product introduction and/or PHA process	4.7	Written procedures must exist documenting how the required process safety information is defined for each process, including how the information will be obtained. The system includes a management system to validate that all information obtained is sufficient.	

Page 5 of 28

NA PHMP I'SA

Name:	Houston	Date: 9/4/2012				
Element:	Process Safety Information - Equipment					
						 -
Requiren	nent	Status	Applicable Standards	Guidelines	Criteria for Implementation	Comments
5,2	Site information is maintained documenting boundaries of the facility and each unit	5.1 Acceptable	5.1 PR SOG (5.1)	5.1 Documetation should exist with general site information including: - maps or photographs indicating surrounding businesses, communities, geography - boundaries for all units including warehouse storage, packaging, and transport areas - a facility layout - layouts for each unit	5.1 The facility will document all boundaries of the facility as well as each unit. The documentation will include information on other businesses nearby, the surrounding community, and the geography of the area Documentation will include information on the physical boundaries of each process including layouts to support the written physical boundaries	
5.2	2 Documentation exists for all equipment	5.2 Needs Improvement	5.2 29 CFR 1910.119(d)(3) PR 506 (5.2)	5.2 Documentation should exist with all equipment information, including the materials of construction for all pieces of equipment within the process	5.2 The facility must create a list for utilize a specification sheet for Jo all equipment with Materials of construction in process or unit. Includeing the following: - valves - gaskets - packing The design specifications should be made available to maintenance as well as the operators within the process area An electronic equipment database or file system with links to: design basis, specification sheets, process and hozard data, design standards, P&ID's, loop sheets, etc is preferred.	Transfer of project files to equipment files - missing equipment from vapor combuster (seal pot, vapor combuster), files missing from sulfur tank - (vent changes to 1-802)
5.3	P&iDs exist for all processes and are up-to-date and are made available to employees	5.3 Needs Improvement	5,3 29 CFR 1910.119(d)(\$)(i)(8) PR 506 (5.3)	5.3 P&IDs are created for all aspects of each process - P&IDs are up-to-date - P&IDs are readily accessible - P&IDs have been reviewed in a PHA study	5.3 The facility must have up-to-date P&IDs for each process The valves must show failsafe position The P&IDs must be made readily available for each operator PHA study reports should document that each P&ID has been reviewed.	TXUP P&IDs could not be found in lotus notes PR&ID for logistic causitic scrubber missing update on controls from project
5.4	Electrical classifications are identified for each area	5.4 Needs improvement	5.4 29 CFR 1910.1.19(4)(3)(i)(C) PR 506 (5.4)	5.4 Drawings should exist documenting the electrical classifications of each process	5.4 The facility should create drawings showing the electrical classification of each area Electrical classification shall be reviewed and the most recent drawing should be made available to employees	
5.9	Documentation of safety instrumented systems (interlocks) exist for each process within the facility	5.5 Acceptation	5.5 29 CFR 1910.139(d)(3)(i)(H) PR 506 (5.5)	5.5. Documentation should exist containing detailed descriptions of all safety systems Interlock matrices should be created for each facility	5.5 The facility will document in detail all installed safety systems including: - hazards being addrossed - hardware (and software) installed - design critoria used to select and size the equipment - adety interlocks and their purpose and procedure for any interlock bypass - applicable reference material	Make sure project information is transferred to interlock matrix to keep files up to date
5.6	S Document that Recognized and Generally Accepted Good Engineering Practices are used in new projects and new processes	5.6 Acceptable	S.6. 29 CFR 1930.319(d)(3)(ii) PR 506 (5.6)	5.6 Documentation should exist noting that Recognized and Generally Accepted Good Engineering Practices are used when installing new equipment, modifying a process area, or adding new processes. There should also be determination and documentation that existing equipment designed and constructed in accordance with codes. • Standards and practices no longer in general use is designed, operated, maintained inspected and tested in a safe manner.	5.6 The facility will document Recognized and Generally Accepted Good Engineering Practices via the MOC process • The facility shall maintain documentation that all existing equipment was designed and constructed according to code within the Unit Safety File	

PSI - Equipment

Requirement	Status	Applicable Standards	Guidelines	Criteria for Implementation	Comments
5.7 Document the design standards and codes as well as the design basis for each aspect of the process	5.7 Acamskig	5.7 29 CFR 1910.119(d)(3)(iii) PR 506 (5.7)	5.7 Documentation must exist nating all of the codes, standards, and design bases used when designing a each system in the process	5.7 The facility must maintain and make available all equipment files including design standards and codes used and design basis for: - All equipment in the process - Safety systems (including pressure relief devices) - Electrical systems - Vontilation systems - Controls, alarms and interlocks - Pumps - Other process equipment - Structures - Fiping systems	
5.8 All Pressure relief devices must be shed for use in each vesse	5,8 Needs Improvement	29 CFR 1910.119(d)(3)(f)(D) DRC 15-01 DRC 15-02 PR 554 (6.1) - MI Pressure fieliel Devices	5.8 Documentation exists for each pressure relief device in the process area	5.8 The facility must size each pressure rolled device for both fire and release scenarios The facility shall demonstrate that the pressure relief device in use is appropriate for the vessel to which it is attached.	Continue work on sizing relief valves, Check master relief valve for completeness
5.0 Safety integrity Levels shall be indentified for each safety integrity Levels shall be indentified for each safety intermediad system.	5.9	DRC 11-36 (3.4.2) PR 554 (6.2) - MLEmergency Shutdowns and Interlocks	5.9 Each safety instrumented system must have documented Safety Integrity Levels and calculations to support all safety instrumented systems that are not SIL-0	5.9 The facility must document the Safety integrity Level each safety Instrumented system a. Each Safety Instrumented System and corresponding Safety Integrity Level shall be documented on the interlock matrix. b. The calculations shall be done using the Rhodia approved method for any Salety Instrumented System not SIL-O.	
5.10 Process control information is documented and made available to each employee	5.10 Needs improvement	29 CFA 1910.119(c)(3) PR SO6 (5.5)	Documentation must exist for each process control system This documentation shall be made readily available to each employee	5.10 The facility shall ensure that written process control software descriptions are up-to-date and include: - Logic - Computer Code Used - Document describing what the code does	Description in lay mans terms for all SISs
5.11 Instrumentation details shall be documented and made available to all unit employees and maintenance	5.11 Needs improvement	29 CFR 1910.119(c)(3) PR 506 (5.5)	5.11 Documentation must exist detailing instrumentation within the process Each instrument must be included on the loop diagrams Documentation shall be included in the equipment file.	The facility shall make instrumentation details readily available to all area employees as well as maintenance including all of the following: Loop and ladder drawings Specification Data Sheets Vendor information and manuals Written functional descriptions	Description in lay mans terms for all interlocks

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Name: Houston	Date:	9/4/2012						
Blement: Process Hazard Analysis (PHA)						ļ		
	201320000			0.000				16
Requirement 6.1 Create a schedule of all Process Hazard Analysis to be completed at the facility	Status 6.1	Acuptable	Applicable Standards 6.1 29 CRR 1910.119(e)(1) PR 507 (6.1)	f c	nies Document a schedule of completeting PMAs at the acillity. This schedule should include a priority ranking of all of the units at the facility. The documentation should include rationale on how he schedule was determined	6.1	a for Implementation Facility must create a PHA schedule that includes the following: a. Timeline of all PHAs to be completed, including the dates of the previous PHA and the future PHAs. b. Priority ranking of all units at the facility c. Rationale of the priority ranking. d. Complete coverage of the facility (including boilers, utilities, etc) e. PID list should exist that links PID to PHA coverage	Comments
6.2 Complete PHAs as documented on the PHA schedule Revalidations must be completed within 5 years.	6.2	Acerteble	6.2 29 CFR 1910.119(e)(6) PR 507 (6.1)		Maintain documentation of the previous PHA schedules is well as the dates of all completed PHAs	6.2	The facility must document the start and end dates of completed PHAs - Facility must show that the PHAs were completed per the PHA schedule	
6.3 PHAs must be completed using one of the approved methodologies.	6.3	(Constraint)	6.3 29 CFR 1910.319(e){2} PR 507 (6.2)		complete all PHAs using one of the methodologies isted below: Proliminary Safety Analysis What-If / Brainstorming (Checklists) Haz-Op Layers of Protection Analysis (LOPA)	6.3	The facility must document that one of the approved methodologies was used during each PHA study.	
6.4 Complete, maintain, and review Risk Evaluation Sheets	6.4	Acaptelia Erroration Considera	6.4 DRC 92 PR 507 (6.1, 6.2, & 6.3)	6 6 6	ilsk Evaluation Shoets with Residual Risk 1 must be losed and mittigation completed with in one year. lisk Sheets with Residual Risk 1 or 2 and severity "C" re signed by the Plant Manager and reviewed on an innual basis tesidual Risk 1 Risk Sheets are reviewed by a Guarantor lisk Sheets are updated as new Information becomes wallable (such as information generated from lispersional modeling)		The facility must maintain all Risk Sheets and document the following: -All Risk Sheets with Residual Risk 1 or 2 and severity -Chave been signed by the Plant Manager and reviewed on an annual basis -A guarantor has reviewed - All Risk 1 Risk Sheets have been completed and closed within one year - All risk sheets have been updated if new information becomes available	
6.5 All PHA teams must be led by an individual trained in the methodology used with members familiar with the process.	6.5	A conjulate	6.5 29 CFR 1910.119(e)(4) DRC 10 PR 507 (6.2)	, p , n	ul PHAs must consist of a leader trained in the Rhodia HA methodologies PHA teams should include the following members at a ininimum: PHA Yeam Leader Operations employee familiar with the process Technical employee familiar with the process		Facility must document that all PHAs were led by individuals trained in the Rhodla PHA methodologies - The PHA study should state that the individual was trained in one of the approved methodologies - The PHA study should state that the postdors/qualifications of all individuals on the PHA Study Team	
6.6: Maintain all final PHA study reports for the life of the process	6,6	Reeds Imployement	6.6 [29 CFR 1910.119(e)][7] PR 507 (6.1)	5	Maintain all documentation included with the PHA tudy report - Ensure the documents are available for a guarantor eview	A TOTAL OF THE STORY A STORY OF THE STORY OF	The following items must be available for review for each PHA studied - Final PHA study report (including a listing of all Process Safety information reviewed during the study) - PHA recommendations and action items - All signed Risk Sheets - The facility must keep records of each PHA study for the life of the process	Could not find for PHAs Regen 2 Oleum before 2009

PHA Page 8 of 28

Requirement	Status	Applicable Standards	Guidelines	Criteria for Implementation	Соимения
6.7 Maintain a management system to ensure findings and Risk Sheets are closed and that recommendations are completed.	6.7 Needs improvement	6.7 PR SO7 (6.2 & 6.3)	Must maintain a system that documents all actions taken to ensure Risk Sheets and audit findings are closed and all PHA recommendations completed	Documentation showing the actions taken for each finding, Risk Sheet, and PHA recommendation and that they are tracked to completion A written schedule of when actions are to be completed individuals responsible for each item.	Not consistant some tracking of action items or recommendations from Pilats - 50 cleurs, fresh acid handling, and TS needs follow-up. Unit & oleum and Regen cleum could not be found. Sitings and Human factors items identified in the PHA need to be tracked
6.8 PHA study reports must include the following information: - PHA study completion date - The scope and objective(s) of the study - List of all Frocess Safety information reviewed - List of all toam members - Methodology used - Risk Sheets generated during the study - List of all action liters and recommendations - List of PIDs reviewed with revision number	6.8 Acceptable	6.2; 79 CFR 1910.119(e)(3) PR 507 (6.2 & 6.3)	6.8 The PHA study report should include all of the required information - The minimum Process Safety information are: - MSOSs of raw materials and products - Hazards of inadvectent mixing - Piping and instrumentation Diagrams for Process Flow Diagrams for less complex systems) - MOC during the period being reviewed - Significant process safety incidents during the period being reviewed	6.8: The facility must ensure that all PtA study reports include the required information	
6.9 Major capital projects include a PHA review at the appropriato stages	6.9 Acceptable	6.9 29 CFR 1910.119(e)(5) PR 507 (6.1 & 6.4)	6.9 Major capital projects should be reviewed for process safety throughout the planning process PHA reviews can be one of the following methods: - LOPA - What-If/Checklist - HozOp/LOPA - Prolitninary Safety Analysis - Risk Assessment - Pre-Startup Safety Review	The facility should insure that all capital projects include a PHA or safety review that is documented independently or included in RACE or MOC documentation	
6.10 Review the rosults of PMAs with affected employees	6.10 Needs Improvement	# 29 CFR 1910.119(e)(5) # PR 507 (6.1) # # #	6.10 The results of PHA studies must be reviewed with all employees working in the process	6.10 The facility shall maintain documentation showing that the results of PHA studies are communicated to employees through: - Sign-in sheets documenting the training - OR - Meeting minutes listing the employees in attendance	
6.11 Report Process Safety Data In Bilan	6.11 (cu-relable	H PR 507 (6.1 & 6.2) H H H H	6.11 Report all required Process Safety data in Bilan, including - Number of P&IDs - % of P&IDs included in a PHA studies - Number of Seveso/RMP P&IDs - % of Seveso/RMP P&IDs not included in PHA studies	6.11 Maintain documentation of total P&IDs and P&IDs covered in PHA studies Maintain documentation of all P&IDs covered by Seveso/RMP	

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Name:	Houston	Date:	9/4/2012						
Element:	Standard Operating Procedures						-		
Requirem	ent	Status		Applicable Standards	Guidel	ines	Criteri	a for Implementation	Comments
7.1	Each processing unit shall have standard operating procedures that include guidelines for the following phases: Normal operation Initial Startup Shutdown Emergency Shutdown Startup after an emergency Startup after as Autdown Tomporary operations Cleaning/decontamination Preparation for maintenance	T	NeedcImproviment	7.1 29 CFR 1910.119(I)(1)(I) PR 508 (7.1)	7.1	Procedures must exist for each processing area and shall be available in the processing area	Ì	The facility shall maintain operating procedures that clearly identify the actions taken in each phase the facility shall maintain operating procedures in the area of operation - Procedures shall be easily accessible for each operator (either electronic or hardcopy)	Need to update to new format. Sections missing in different areas.
7.2	Proceduces shall be current annually certified	7.2		7.2: 29 CFR 1910.119(f)(3) PR 508 (5.2)		Maintain a management system to ensure operating procedures are annually certified	7.2	The facility shall provide documentation of the annual certification Operations should verify that the procedures accurately reflect the process as it is currently done	
	All procedures shell include Critical Operating Parameters (COPs), consequences of deviation, steps to corroct a deviation/troubleshoot problems, and a listing of safety systems	7.3	Needs in proviment	7.3 29 CFR 1910.119(f)(1)(ii) PR 508 (7.1)	7.3	Each procedure shall list the following: - Each COP along with its description - Each safety sytem along with its description - Each safety sytem along with its description - The consequences of deviating from the procedure - Steps on how to troubleshoot process deviations		The facility shall show documentation of each section in each standard operating procedure. Operators should be able to identify the COPs in each process and have an understanding of the consequences of deviations and troubleshooting. Operators should understand the safety systems in the area.	Neods COPs for TS and Logistics documented.
7.4	Operators are consulted when writing/changing procedures	7.4	Acceptable	7.A PR 508 (7.1)		Each procedure modification shall include a review with operations personnel	7.4	Maintain documentation showing that operators are consulted when changes are boing made - feamples could include MOSt situlated by operator or signed off sheet when an SOP is updated.	

Standard Operating Procedures

Name:	Heuston	Date:	9/4/2012						
Element:	Training	ļ]			, , , , , , , , , , , , , , , , , , ,	
***************************************					0.00		100000	= 6. Landon arotto	Comments
	DIL: Employees must received detailed training on the process and process hazards prior to entry into a new facility, department, or job classification	Sintus 8.	Acceplable	Applicable Standards 8.1 29 CFR 1910.119(g)(1)(i) PR 509		Each employee must receive training in the following areas: - Process overview including Process Flow, chemistry, potential hazards, and environmental Impacts - Standard Operating Procedures with emphasis on a safety and health hazards, emergency operations, and safe work practices applicable to the employee's job tasks - Critical Operating Parameter's - Operation of the equipment used in the process - Process simulation of abnormal conditions on a control, OCS or computer system where the operator is required to regain control - Troubleshooting techniques		ria for Implementation J. The facility shall maintain documentation of all employees training - Training matrix for each employee or position - Training documentation shall consist of a listing of each topic covered in the training as well as the signature or an initial sign-off by the employee.	Supervisors should have a tracking grid for training
8.2	Each employee in a PSM covered facility must receive initial PSM training	8.3	Acceptable	8.2 29 CFR 1910.119(g)(1)(i) PR 509		include a section on PSM in all new hire training programs	8	2 Document that PSNA is included in all initial new hire orientation/training programs	
	Each employee must receive refresher training at a militinum of every three years	8.3	3 Rects Improvement	8.3 25 CFR 1910.119(g)(2) PR 509		Each employee must receive refreshor training in the following areas: - Process overview including Process Flow, chemistry, potential hazards, and environmental impacts - Standard Operating Procedures with emphasis on safety and health hazards, emergency operations, and safe work practices applicable to the employee's job tasks - Critical Operating Parameter's - Operation of the equipment used in the process - Process simulation of abnormal conditions on a control, DCS or computer system where the operator is required to regain control - Troubleshooting techniques	8	3) The facility shall document that all employees receive job specific refresher training at a minimum of every three years. The facility shall maintain a management system to ensure that all employees recover refresher training at a minimum of every three years, (This should include agenda, sign in sheet, and documentation that employee understands the information.)	Refresher training records to be verified for employees need to be verified for all units
	Consult employees on the frequency and content of refresher training	B.4	. Recti inprovement	8.4 23 CFR 1910.119(g)(7) PR 5:09		Employees must be consulted on determining the frequency and content of roftesher training. The minimum frequency of roftesher training must be three years. The training must contain a minimum of the following elements: Process overview including Process Flow, chemistry, potential hazards, and environmental impacts. Standard Operating Procedures with emphasis on astely and health hazards, emergency operations, and safe work practices applicable to the employee's job tasks. Critical Operating Parameter's. Operation of the actual equipment used in the process simulation of silvormal conditions on acounts). ECS-or computer-system where-the operator-is-required-to-regimeoutre.	8	A The facility shall maintain documentation that the employees have been consulted on the frequency and content of refresher training . A comptain documentation may include, but are not limited to, the following: (a) Questions on refresher training assessments (b) Questions asked during departmental meetings (c) Surveys	Record needed on consulting employees on frequency of rafresher
8.5	All training documentation must include the following: - The name of the employee trained - The Iraining content - The date of the training - The means of ensuring that the individual understood the training - The name of the individual giving the training	8.9	Needs improvement	8.5 29 CFR 1910.119(g)[2] PR S09		include all of the information on the training documentation. - The means of ensuring that the individual understood the training should be measurable	6	.5: The facility stall maintain all of the required information on training documents The means of ensuring that the operator understood the training shall be through one of the following methods Training quiz OR On the lob training evaluation	Need documentattraining was understood and who conducted the training

Requirement	Status Applicable Standards	Guidelines	Criteria for Implementation Comments
8.6 The facility shall establish a training program for all employees, contractors, and visitors	8.6 PR 509	8.6 Establish a written procedure documenting how all employees, contractors, and visitors will be trained. - The procedure must include the criteria for qualifying and certifying employees.	8.6 The facility shall maintain documentation showing that each employee, contractor, or visitor is trained as stated in the training procedure - The facility must document that each employee is "qualified" for the job based on the criteria for qualification and certification of employees
8.7 The site shall have a management system for its training program	8.7 PR 509	8.7 The management system must include the following: - An Individual assigned responsibility for the written training program - The responsibilities of personnel associated with the training program - A matrix of training for all positions - Trainer qualifications - A mechanism to audit the training program for effectiveness - Identified and implemented improvement opportunities	8.7 The facility's management system must contain all of the required information and must be made available

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Name:	Houston	Date:	9/4/2012				
Element:	Contractors						10.000
Requirem	nu.	Status		Applicable Standards	Guidelines	Criteria for Implementation	Comments
9.1	Maintain a written contractor safety program that includes the following: A system to readily identify trainied contractors (i.e. hardinat stickets, etc.) A sixt of approved contractors for use at the facility A system in place to assess the contractor safety program (including the auditing of training records) - A system in place to audit and approve contractors A system in place to audit and approve contractors A system in place to qualify contractors performing provendations and contractors performing provendations.	<u> </u>	Arceptable	9.1 29 CFR 1910.119(h)(2)(i) PR 510	S.1. Ensure that all employees responsible for contractor selection, evaluation, and sudits are included in the contractor safety program.	2.1 Miaintain documentation showing that each contractor has been selected based on the criteria set forth in the contractor safety program. The documentation must show that the contractors meet all of the requirements of the contractor safety program The documentation must show that the contractors have been audited offsite and evaluated onsite.	
	if applicable, the contract employer has the following as a portion of their safety program and that all employees working on-site are trained in each area, as required: - New thire Safety Orientation ProgramyPlan - Written Incident Investigation Plan - Undustrial Hygiene (Including respirator fit testing, hearing protection, etc.) - Confined Space Entry - Hot Work - Lockout/Tagout	9.2	Arceptalis	9.2 PR 510	9.2 Obtain documentation from the contracted company documenting the required training of all employees working on-site Ensure that the site has a management system for ensuring that each employee is current on all required training	9.2 The facility must obtain and maintain the safety plan and training records of approved contractors. The facility shall maintain documentation stating that the contracted company has a management system to track and ensure employee training. The following documents are acceptable documents: - Written safety plan that includes the required information - Copies of annual safety training presentations along with their respective sign-in sheets. - Signed certifications from respirator fit testing allowing respirators to be worn by each individual - Confined Space Entrant/Attendant certification cards	
9.3	Maintain a record, OSHA 300 log, of contractor injuries on-site	9,3	Acceptable	9,3 29 CFR 1910.119(h)(2)(vi) PR 510	9,3 Maintain records of all contractor Injuries on an OSHA 300 log or similar decument	9.3 The facility must maintain a record of all contractor injuries on-site	
1	The contractor approval process must include a system to review the company's safety record prior to bringing the contractor onsite	9.4	Арээр ь На	9.4 29 CFR 1910.119(h)(2)(f) PR 510	9.4 Prior to introducing a contactor to the site the following information must be obtained: - Total number of lost time injuries - Total number of fatalities - Total number of fatalities - Total number of fatalities - Total number of obys of restricted work - OSHA incident rate The facility must establish acceptable ranges for each them	9.4 The facility shall obtain the Information required and document this Information in the contractor's file. When contractors are selected with records outside of the acceptable ranges there just be a documented justification.	
	Create and maintain a written Contractor Safety Plan that includes the following: - An orlentation plan for new contractors working on-site - Training on the Hammability, toxicity, and explosivity neareds of the facility with specific training on the hazards of the particular area(s) where the contractor will be located - Training on site rules and regulations - Training on Emergency Response Plan and the emergency actions - A means of assessing whether the employee understood the renining	9.5	Acceptable	9.5 29 CFR 1910.119(h)(2) 29 CFR 1910.119(h)(5) PR 509 PR 510	9.5 A written Contractor Salety Plan must be maintained at the facility containing all of the required documents. The Contractor Safety Plan must be updated as changes occur at the facility.	9.5 The facility shall maintain a current Contractor Safety Plan. • The Contractor Safety Plan must clearly state the revision date The facility shall maintain documentation of all contractor's Contractor Safety Orientation via completed pre-job assessments or quitzes • The assessment shall include the name, date, subject matter, and results of the assessment	
	The site shall conduct periodic evaluations of all contracted employees noting the conformance to site rules and regulations as well as job performance	9.6	Nee 31 mproviment	9.6 29 CFR 1910.119(i)(2)(v) PR 510	9.6 A written worksite evaluation form must be created and completed for each confractor working on-site. The facility shalt ensure that all contracted employees follow site safe work practices. - This can be documented via on-site audits of contractors which evaluate work safety as well as job performance and professionalism	9.6 The facility shall maintain records of contractor on-site audits documenting job performance and that the contractors follow site rules and regulations The facility shall also maintain records documenting an Instance where a contractor was found not following the rules as well as the consequences of the violation(s). The facility shall maintain documentation of any instance where folloperformance was deemed poor and the consequences of the poor evaluation.	turnaround and found only CCC was evaluated the other contractors were not evaluated

Requirement	Status	Applicable Standards	Gnidelines	Criteria for Implementation Comments
9.7 Industrial hygeine data must be maintained on-site	9.7 Not Applicable	9.7 PR 510	9.7 In the event that a contractor performs industrial hygoine sampling at the facility, the results must be shared with the facility and maintained on-site with other industrial hygeine data	9.) The Contractor Safety Plan must state that the results of Industrial hygeine sampling taken on-site must be submitted to the facility within a set time-frame. There must be a location where this information is stored at the facility.
9.8 The facility must document the contracted employer's responsibilities in the Contractor Safety Plan and maintain documentation of the adherence to these responsibilities	9.8 Arrepteds	9.8 PR 510	9.8 The contracted employee's responsibilities shall include, at a minimum, the following: - Contract employees are trained in work practices necessary to safely perform the job - Contract employees are instructed of the known potential fire, explosion, or toxic release hazards and the applicable sections of the emergency action plan - Employees have received and undestood the training required by this section (identity of employee, date of training, subject, and the means used to verify that the employee understood the training) - Contract employees follow the safety rules of the site - Contractor advises Rhodia of any unique hazards presented by the contractors work or any hazard found by the contractor's work.	9.8 The facility must obtain copies of the employees training prior to coning on site The facility must ensure that the training includes all of the roquirod elements

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sientent:	Pre-Startup Safety Review				-			
Requireme	ent	Status		Applicable Standards	Guide	lines	Criteria for Implementation	Comments
	The facility must have a Pro-Startup Safety Review procedure In place that includes the requirements of the review and when a Pre-Startup Safety Review is required	10.1	Acceptable	10.1 PR 511	10.1	The procedure shall state that a Pre-Startup Safety Review is completed whenever there is a change to the Process Safety information	10.1 The facility must document the completion of the Pre- Startup Safety Review with the MOC The facility shall have all Pre-Startup Safety Review forms available for review, of their hardcopy or electronic	
	Maintain the Pre-Startup Safety Reviews for the life of the process	10.2	Acceptable	10.7 PR 511	10.2	The facility shall maintain all Pre-stertup Safoty Reviews for the life of the process in either herdcopy or electronic form	10.2	
	Assign a responsible person/people for the oversight of the Pro-Startup Safety Review	10.3	Acceptable	10.3	10.3	The facility shall assign a responsible person/group for the oversight and maintenance of the program	10.3 The facility shall document the responsible individual(s) for the Pro-Startup Safety Review program Mate: There should be a procedure or form indicating who is responsible.	
r	Estabilish a timeline of when a Pre-startup Safety Review Is required for startup of Idled processes/facilities or inactive products	10.4	Acceptable	10.4 PR 511	10.4	The facility must create a maximum timeframe for when inactive/killed materials or processes are to be brought back into service	10.4 The facility shall document the required timeframe in the written Pro-Startup Safety Review procedure Note: This may be included in the site's MOC policy.	
	The facility must train employees on the use and requirements of Pre-Startup Safety Reviews	10.5	Needs improvement	10.5 29 CFR 1910.119()(2)(w) PR 511	10.5	All employees should have a working knowledge of the Pre-Startup Safety Review process	10.5 Pre-Startup Safety Review training shall be documented for each employee via sign-in shoots and/or training assessments or quitzes - These documents should be accompanied by the training documents or could be attached to MOCs	No records could be found
, c c c c c c c c c c c c c c c c c c c	All Pre-Statup Safety Review forms shall include the following regularements: - Name of the area modified - Name of the project - Review of parts Safety Reviews - Review of procedures required for safe start-up and operation and normal and emergency shutdown - Training requirements for all affected employees, along with documentation of the completed training - A walk through of area modified??? - Signatures noting the formal approval or authorization to start process - Construction and equipment are in accordance with design specifications - Safety, operating, maintenance and emergency procedures are in place and are adequate - For now Laciflice, or major capital projects, a PHA has been performed and recommendations have been resolved or implemented before start-up - Modified facilities need the requirements of Management of Change	10.6	Acceptable	10.6 29 CFR 1910.119()](2) PR 511	10.6	The Pre-Startup Safety Review form shall include all of the required Information - Each item shall be addressed in each Pre-Startup Safety Review - If an Item is not completed the justification shall be noted on the form	10.6 The facility shall address and complete each requirement in each Pre-Startup Safety Review • Those documents must be made available for review	
	Employees shall be made aware of the Pre-startup Safety Review findings and action items	10.7	Needs improvement	10.7 PR 511	10.7	All findings and action items must be communicated to semployees	10.7 The facility shall maintain documentation showing that all applicable employees have been informed of all action Items and findings - This shall be documented using a training sign-in sheat	No documentation
	Actions from each Pre-Startup Sofety Review are documented and tracked to completion	10.8	Needs improvement	10.8 29 CFR 1910.119(I)(2)(III) PR 511	10.8	A management system, such as Manufacturing Solutions, shall be used to track all findings and action Items	10.8 The facility shall record all action items and findings in Manufacturing Solutions or a similar database	No tracking on 8 tiems, A items should be corrected before start-up no documentation
	Periodically review the quality of all Pre-Startup Safety Reviews for completeness and accuracy	10.9			10.9	Review the Pre-Startup Safety Reviews on a defined periodic basis to ensure that all action items are closed and that there modifications are completed as stated on the forms	10.9 The facility shall maintain documentation of the review of the Pre-Startup Safety Reviews	

Requirement	Status Ap	olicable Standards	Guidelines	Criteria for Implementation	Comments
10.10 A Pre-Startup Safety Review must be done on all MOCs including ones that Involve changes to Process Safety Information	10.10 Needs Improvement	29 CFR 1910.119(i)(1) PR 511	10.10 Perform a Pre-Startup Safety Review on all changes that affect PSI, including changes to Process Flow Diagrams, P&IDs, process chemistry, operating procedures, critical operating parameters, etc.	10.10 The facility shall maintain documentation of Pre-Stat Safety Reviews for all changes involving changes in Process Safety Information	tup Simple changes (pressonnel changes, procedure changes, etc.) included in MOC form questions. Expand PSSR to include all equipment changes

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Name:	Houston	Date:	9/4/2012						
Element:	Management of Change (MOC)	1			4			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	
Requirem	ent	Status	i.	Applicable Standards	Guide	lines	Criter	ia for Implementation	Comments
	Create and maintain a written Management of Change Procedure		Acceptable	11.1 29 CFR 1910.119(1)(1) PR 514		The facility shall create a written procedure explaining the Management of Change program and process		The facility shall make the written MOC procedure available	
	The MOC procedure shall require completed MOCs for the following types of changes: - Chemicals - Yechnology - Equipment - Procedures - Sitting, equipment relocation and layout - Personnel - Process control philosophy (including critical operating parameters) - Process control equipment including DCS and PLC - Process control configuration / application engineering - Organization - Process control configuration / application engineering - Organization - Policies, management systems - Critical operating parameters - New information on process hazards - Safety systems including alarma and interlocks setpoints - Others as defined by site-specific conditions - Sacurity - Products		Acceptable	11.2 29 CFR 1910.119(I)(1) PR 514 (15.1)	11.7	The completed MOCs must be done on all changes that are not "Replacement in Kind" and that have any affect on the safe operation of any process, unit, procedure, etc.	11.2	The facility shall make the written MOC procedure available listing the required types of changes	Expand MOCs to include facility siting empacts (trailorw, ctc.) and equipment brought into the site (thermal oxiders, open flamo equipment, etc.)
	The written procedure must define the roles and responsibilities of key individuals involved in the Management of Change process The procedure shall include the regultements for the review and authorization of changes	11.3	Acceptable	11.3 29 CFR 1910.119(I)(2)(v) PR 514 (13.1)	11.5	The written procedure shall state who is authorized to make, review, and approve changes at the facility	11.5	The facility shall make the MOC procedure available listing the roles and responsibilities of those involved in the MOC process	
11,4	All employees must be trained in the MOC process	11.4	Acaptable	31.4 PR 514 (13.1)	11.4	Training shall be conducted in each of the following situations: - Initial training for each new employee - Periodic training, at a defined frequency, noting changes to the program - Project training on all changes that occur in an area as a result of a project.	11./	The facility shall document MDC training using the training materials and sign-in sheets	
	Each MOC shall include the following information: - A written description of and the technical basis of the change - Safety and health considerations, including orieria for performing formal risk assossment - Written approvals that authorise the change to be executed based on the analyzed safety and health considerations - Provision for satisfactory resolution of change review recommendations - Follow up to ensure that affected documentation is updated - Affected operations, maintenance, and contractor personnel are trained before they are "exposed" to the change - Regulatory impacts of Change		Acceptable	11.5 29 CFR 1910.119()(2) PR 514 (13.1)	11.5	MOC forms shall include all of the required information	11.5	The facility shall include the required elements in the MOC procedure and shall address each element in each MOC in any case where an element is not complete there must be a supporting justification. The facility shall make MOCs available for review in either hardcopy electronic form	
11.6	Establish a maximum timeframe for emergency changes to be implemented prior to approval	11.6	Needs improvement	11.6 PR 514 (13.1)	11.0	in the event of an emergency change a MOC must be completed soon after the change. The facility must establish a timeframe when the MOC must be complete after the change.	11.0	6 All emergency MOCs must be documented with the required information using Manufacturing Solutions or a similar database	Need to establish time frame for emergency changes to issue MOC
11.7	Define a timeframe for each temporary change, prior to the initiation of the change	11.7	Needs Improvement	11.7 PR 514 (19.1)	11.	The MOC must require predetermined start and end dates for each temporary MOC The start and end dates must be defined prior to the approval of the MOC	11.	All temporary MOCs must be documented with the required information using Manufacturing Solutions or a similar database	Several temporary MDCs past due

Requirement	Status	Applicable Standards	Guidelines	Criteria for Implementation Comments
11.8 Define types of changes that cannot occur without prior approval, even in the event of a emergency	11.8 Acceptable	11.8 PR 514 (13.1)	11.8 The facility must define which changes cannot occur with out prior approval	11.8 The facility must document all amergency changes with the date of implementation and approval The facility must show zero instances where a probabiled emergency change was implemented prior to approval The MOCs should be documented in Manulacturing Solutions, or a similar database
11.9 All MOCs must be documented using a database or a form and maintained for the life of the process	11.9 Acceptable	11.9 29 CFR 1910.119(I) PR 514 (13.1)	11.9 Document all MOCs in either electronic or hardcopy form and retain for the life of the process	11.9 The facility must maintain documentation nof all MOCs using Manufacturing Solutions or a similar database
11.10 The facility must have an audit program to assess the MOC process relative to the written MOC procedure	11.10 Acceptable	11.10 PR 514 (13.1)	11.10 The audit program should consist of the following: - Reviews deficiencies in signatures and approvals - Completion of all required sections - Completion and documentation of follow-up activities - Effectiveness of system in reviewing all changes	11.10 The facility shall maintain documentation of the completed audit forms The facility shall make completed audit forms readily available for review
31.11 The facility's written MOC procedure must include changes to security elements.	11.11 Aceptabe	11.11 PR 514 (13.1)	11.11 The security elements included in the site's MOC procedure include the following: - Target assets including physical, chemical, information and cylor recommendation of the site of	11.11 The facility must document all security elements in the site Management of Change Program. The facility shall maintain documentation of MOCs for changes to security elements

Name: Houston	Date:	9/4/2012		1				
Element: Mechanical Integrity								
	1			004-0440			nteria for Implementation	Comments
Requirement 12.1 The site must have a written Mechanical Integrity Plan that Includes the required preventative/productive maintenance (PM) for all of the following picess of equipment: - Pressure versels and storage tanks - Piping systems (Including piping components such as valves and hoses) - Relief and vent systems and devices - Emergency shutdown systems - Controls (including monitoring devices and sensors, alarms, and interlocks) - Pumps and other rotating equipment - Other process equipment that may contain process imaterials or impact process sets in the process of the proce	12.1 Ats		Applicable Standards 12.1 29 CFR 1910.119()(1) FR 512 (11.1)		The Mechanical Integrity Program must describe, in detail, the inspection and testing requirements and frequencies for all equipment categorized as A or B. The plan must also address actions to be taken if a PM is late or missed. The inspection frequencies must be defined in accordance with manufacturers recommendations, good angineering practices, codes, or more frequently if determined by prior operating experience.	1	12.3 Documentation of the written Mil Program for the facility that includes the PM schedule and all inspections/testing for all applicable equipment. The document must also address past-due inspections/tests The plan should be an active document that is updated as equipment is added/removed at the facility. Manufacturer recommendations must be documented and maintained with all inspection records.	
12.2 All equipment must be categorized as A, B, or C according to the guidelines set forth in MI PR-550 - Categorization of Equipment for Mechanical Integrity	12.2 70	apirili	12.2 PR 512 (11.1) MI PR 550 - Categorization of Equipment for Mechanical Integrity	12.2	Equipment must be categorized as A, B, or C based on regulatory or Rhodia requirements		12.2 The facility must document the categorization of all equipment in the MI Program The categorization must include a justification for each Item	
12.3 Each place of equipment and its components must identified	12.3 Ne	eds improvement	12.3 Mt PR 550 - Categorization of Equipment for Mechanical Integrity	12.3	Each place of equipment, including the individual components, must identified using a unique number or code		12.3 The facility must document the unique number or code in the MI Program for each place of equipment and its components	Project Information - instrumentation not in maintenace files for sulfur tank and VCU
12.4 Equipment specifications shall be maintained and updated as changes are made or new information is obtained	12.4 Né	ed/Imprevement	12.4 PR 512 (11.1)	12.4	Maintain all equipment specifications in the Unit Safety File for each piece of equipment - Component specification sheets shall be maintained in a defined location as defined by the facility The facility must create a system for updating specification sheets as needed		12.4 The facility must maintain a management system for all specification sheets and must make them readily accessible for all employees. The facility shall document changes to specification sheets and maintain the revision either in the Unit Safety File or in the facility's designiated location for the specification sheets of components.	System in place - some pieces of equipment missing specification sheets
12.5 The facility shall test Safety instrumented functions according to the period used in the SIL calculations	12.5 20	eptade	12.5 MI PR 555 - Emergency Shutdowns & Interlocks MI PR 556 - Control Systems	12.5	Each SIS must have an accompanying SIL calculation • Each SIL calculation shall be done by an individual trained in performing SIL calculations.		The facility must document all SISs on an interlock Matrix The SIL tovets shall be documented on the interlock Matrix and the supporting calculations shall be readily available The SIL calculations must include the underlying assumptions as well as the name of the individual performing StL calculations, along with documentation of there certification(s)	No Sit. calculations using default frequency identified in our procedures PR-555 and DRC 11-33 appendix 14. Interlock testing on VCU BMS behind schedule
12.6 All historical repairs and inspections shall be maintained onsite For all equipment considered a layer of protection as listed in PHAs	12.6 Å6	cuptable	12.6 PR 512 (11.1)	12.4	Create a central location for all historical repair and Inspection records		12.6 Historical maintenance records should be readily available to all employees	
12.7 All Inspections shall be documented using an inspection form and the form shall include the following: - Date of inspection - Name of inspector - Equipment identifier - Type of test - Test results	12.7 %	APISUS	12.7 29 CFR 1910.119()(4)(v) PR 512 (11.1) MJ PR 551 - Storage Yanks and Pressure Vessls MJ PR 552 - Piping Systems MJ PR 553 - Rotating Equipment MJ PR 554 - Prossure Rollef Devices MJ PR 555 - Emergency Shutdowns and Interlocks MJ PR 556 - Control Systems	12.	The facility must note all of the required information for each inspection or test		12.7 The facility should create inspection and testing forms for the different types of equipment and components and use these forms to document inspections and testing. The facility shall maintain all completed documents in the Unit Safety File or in the designated area for component records.	
12.8 inspection personnel must be trained in the area of work	12.8 A 6	eepta (le	12.8 29 CFR 1910:119(j)(3) PR 512 (11.1)	12.	8 Documentation must indicate that inspectors and repair personnel are trained in: Overview of the process and its materds Procedures applicable to the employee's Job tasks	A	12.8 The facility must maintain documentation of the inspector's qualifications along with the inspection forms	

Mechanical Integrity
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Requirem	ent	Status		Applic	able Standards	Guide	lines	Crite	ria for Implementation	Comments
12.9	All new equipment must be tested and added to the MI program prior to use	12.9	Needs Improvement	12.9	29 CFR 1930,119(j)(6) PR 512 (11.1)	12.9	All new equipment must be tosted and the results reviewed prior to use The test results must be documented The MI must be updated to include the new equipment and the inspection frequencies must be determined according the the manufacturer's reconvenentiations	12.	The facility shall document that new pieces of equipment are tested prior to use and added to the MI Program The MI Program should have a management system in place to ensure that all new items are added to the program prior to use	Documentation of initial testing missing or insdequate on three projects - Redisigned VCU, New Sulfur Tank, and Bargo Vent System
	The facility must have a procedure for addressing system or equipment deficiencies and assigning responsibilities for those responsible for correcting those deficiencies. The plan must include a statement prohibiting the deficient equipment/system from being used prior to the deficiency being corrected.	12.10	Aceptable	12.10	29 CFR 1910.119(j)(5) PR 512 (11.1)	12.10	The procedure should include target dates for resolving system and equipment deliciencies. - The procedure should also require defective equipment be taken out of service	12.1	Of the facility must document the procedure for resolving system and equipment deficiencies, as well as defining responsibilities for those responsible. The facility shall maintain documentation showing the date that the system/equipment was taken out of service, how the issue was resolved, and the date that it was brought back on-line.	fixed immediately or not for historical records
12,11	All tools, parts, and other materials required for maintenance must be readily available and in good condition	12.11	Acceptable	12.11	29 CFR 1910.119()(6)(III) PR 512 (11.1 & 11.9)	12.11	Create a system where all required tools, mateirals, and parts are continually repienished	12.1	The facility must create a system documenting the continual replacement of all necessary pacts, materials, and tools	
	All work orders should be linked to the MOC system to ensure that all work orders requiring a MOC have a MOC	12.12	Acceptable	12.12	PR 514	12.12	All work orders must be reviewed to ensure that all MOC regulrements are met, if applicable	12.1	2 The facility shall maintain documentation showing the prioritization of word orders and the review of work orders for MOC applicability	Life of work order - training document showing operation supervisor is responsible ensuring MOC is issued before changes are made.
12.13	Test and inspect equipment according to the defined requirements and frequencies	12.13	Acceptable	12.13	29 CFR 1910.119(j)(6)(iii) PR 512 (11.1)	12.13	Ensure each piece of equipment, and its components, included in the MI Program is inspected and tested as stated in the MI Program	12.1	The facility must document and maintain all inspection and testing records in the Unit Safety File or in the designated area for components	
12.14	Assign responsibility over the MI program	12.14	Acceptable	12.14		12.14	The facility must assign a responsible person /people over the MI Program	12.1	The facility must document MI Program responsibility(ics)	
	The facility must maintain records for idled or decommissioned equipment - Documentation must remain ensite for as long as the equipment is located at the facility.	12.15	Acceptable	12.15	PR 512 {11.1} -> 29 CFR 1910.119(e)(7) -> 1910.119(d)(1)	12.15	All equipment records must be maintained for all idled or decommissioned equipment, including records documenting the idling/decommissioning	12.1	The facility shall document all reasons for idling/decommissioning equipment, and continue to maintain inspection records	
	All applicable employees must have appropriate training, including training in the MI Program and the hazards of the process. In addition, refresher training must be done on a regular basis.	12.16	Acceptable	12.16	29 CFR 1910.119(j)(3) PR \$12 (11.1)	12.16	All employees responsible for inspections, testing, or preventative/protective maintenance must be trained at a defined frequency and the training documented	12.1	The facility shall maintain records of the training documents and the means to assess the employee's understanding of the training. The training shall include the Jollowing: Nama Oute Subject matter Results of assessment Joh awailification.	
	Electrical single line diagrams must exist for electrical systems (Instrumentation/shutdown devices)	12.17	Acceptable	12.17	MI PR 556 - Control Systems	12.17	Maintain single line diagrams of all electrical equipment	12.1	The facility shall maintain current electrical single line diagrams The facility shall make all diagrams readily available	

Mechanical integrity Page 20 of 28

NA PEIMP FSA

Name:	Houston	Date:	9/4/2012							
Element:	Work Permits								, , , , , , , , , , , , , , , , , , , ,	
Requirem	ent	Status		Applica	able Standards Guide	lines		Criter	ia for Implementation	Comments
13.1	Site has written procedures and/or permits conforming to regulatory and policy requirements for: - Hot Work - Lockout / Tagout - Confined Space Entry - Une or vessel entry - Elevated Work - Control over entrance into the facility - Crane operations near chemical and power lines - Execusation and Trenching - Work on energized ("live") electrical circuits	13.1	contain	13.1	PR 513	procedures to	must be developed with supporting rail of the fisted topics. must be maintained for a minimum of		The facility must maintain and make available completed permits. The facility shall have permits for, at a minimum, the past year The facility must provide current procedures for each listed topic. Permits currently in use must be completed per the corresponding procedure	
13.2	Each employee must be trained in the procedure(s) for each permit	13.2	Creshin) la	13.2	13.7	Z Maintain doo	mentation of all work permit training		The facility shall provide documentation that all comployees have been trained in all of the listed work parmits, if applicable . The facility shall document the training via copies of the training materials and completed sign-in sheets and/or completed assessments.	Training conducted on an annual basis
	Maintain a system for ensuring that manufacturing employees are notified when work is completed by maintenance or contractors	13.3	ng-eptable	13.3	13.3	procedure for	half be developed explaining the notifying manufacturing of completed maintenance or contract employees	13.3	The facilities shall demonstrate the use of the procedure during the implementation of permits	
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Work Permils

Name:	Houston	Date:	9/4/2012		-				
Blement:	Incident Investigation								
		Status		Applicable Standards	Guide	lines	Crit	eria for Implementation	Comments
	A management system for the incident investigation process has been established and includes the following elements: - Written procedure - Action Hem tracking database - Nethods for communicating results of incident investigations to affected employees and contractors		Acceptable Accept	14.1 79 CFR 1910.119(m)(5) 29 CFR 1910.119(m)(6) PR 515	14.1	The management system must include a written procedure that includes the following: Definitions of "process incidents" and "near misses" Personnel responsibilities Reporting requirements All incidents are investigated using a causal tree or similar method to document the events and the primary causes of the incident Leadership requirements Training requirements Action tracking method Means of communication to affected employees Incident investigation report requirements Incident severity ranking, based on impact to health, safety, and the emirorment The management system must also include a database for tracking actions and a system for communicating results		4.1 The facility shall maintain a current written procedure that includes all of the required elements. The facility shall demonstrate the effectiveness of the management system in the following ways: (a) Evidence that action items are tracked to completion using Manufacturing Solutions or a similar database. (b) Evidence that the results of incident investigations are communicated to affected employees and contractors through traning sign-in sheets.	
	All process incidents and significant near misses, with a severity or potential severity of modium and others at the discretion of the site, must be investigated, and the investigation initiated within 48 hours - Including near misses and reliability incidents	14.2	Acceptable	14.2 29 CFR 1910.119(m)(2) PR 515	14.2	A process incident is any event that results in or could possibly result in fires, explosions, hazardous chemical releases, damage to equipment, or injuries	1.	4.2 The facility shall document all investigations in along with the incident using action tracking database (Manufacturing Solutions or similar) - The database shall show that the investigation was shifted within 48 hours of the event.	
	All incident investigations must include the following elements: - A team consisting of individuals involved in the incident and a trained team header. - Incident investigation report that includes: - Incident date - Date investigation began - Description of incident - Factors that contributed - Record of recommendations - List of all team members along with his/her respective qualifications - Incident severity rankings	14.3	Needa Improvement	14.3-29 GFR 1930.119(m)(4) PR S15	14.3	All incident investigations must be reviewed by a learn with the following qualifications: (a) Team leader trained in the incident investigation procedure (b) Team member knowledgeable in the process (c) A contractor, if a contractor was involved in the incident inciden	1	The facility shall show that all incidents include all of the required elements by documenting all aspects of the investigation in the action tracking database [Manufacturing Solutions or similar]	Action items not tracked
14.4	incidents must be discussed at safety or team meetings	14.4	Acceptable	14.4 DRC OS	14.4	Discuss all applicable incidents at safety or team meetings	1	4.4 The facility shall document when incidents are reviewe with applicable employees via sign-in sheets	
14.5	All Incidents must be analyzed for trends on an annual basis	14.5	Acceptable	14.5	14.5	Incidents, including near misses and observations, must be analyzed for trends and action/improvement items created Key trends must be communicated to employees	1	The facility shall document trend analysis and action/improvement items The facility must document communication of trends to employees via sign-in sheets	
	Site-records;-investigates;-analyzes-and-freeks-safety-system frips-or-activations	14.6		14.6	14.6		1	4.6 The faellity shall document all safety system trips or octivations and shall make the information available upon toquest his includes files defuge, etc.	
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Incident Investigation

Name:	Houston	Date:	9/4/2012		11				
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siement	Emergency Planning and Response								
Requireme	ent	Status		Applicable Standards	Guide	lines	Criter	ria for Implementation	Comments
	The Emergency Response Plan must include the following: - Consideration of consequences of releases of hazardous materiality and procedures for handling small releases. - Employee training - Emergency drills, including frequency - Notification procedures for the initial response to emergencies, including checklist describing priorities, calling 911, sounding alarms, calling in employees on off hours, etc. - Procedures for communicating emergencies - Documentation of coordination between the facility and local agencies	15.1	Aceptals	15.1 29 CFR 1910.119(n) PR 516 (15.2)	15.1	The Emergency Response Plan must include all of the required elements The facility must document the consequences of different sconarios resulting in the release of hazardous, toxic, flansmable, or reactive, materials. -The procedure must also include the handling of small releases	15.:	The facility shall ensure that the Emergency Response Plan Includes all of the required elements : Each element must be documented	
	Establish a repsonsible person for the Emergency Response Plan	15.2	Azzeptetle	15.2 29 CFR 1910.38(c)(6)	15.2		15.3	The facility shall establish a person responsible for the maintenance of the site Emergency Response Plan that includes the following: Site emergency response management - implementation of the plan - Improving and updating the plan	
	Determination has been made whether the plant is also subject to the hazardous waste and emergency response provisions contained in 29 CFR 1310.120 (a), (c) and (d), Hazardous Waste Operations and Emergency Response. Morg.: If there is a conflict or overlap between the two provisions (1910.38 and 1910.120), then the one which is more protective of employee safety and health has been deemed to apply.	15.3	Ayeptade	15.3 29 CFR 1910.119(n) PR 516 (15.1)	15.3	Review 29 CFR 1910.120 sections (a), (p), and (q) and determine applicability	15.	3 The facility shall document the applicability determination, include justification for whether the facility is or is not covered under the standard 1. This determination shall be included in the Emergence Response Plan	
	Employees must be trained in the details of the Emergency Response Plan	15.4	Acceptable	15.4 29 CFR 1910.38[e) PR 586 (15.2)	15.4	Maintain all emergency response training documentation for all employees - Training must include emergency recognition and prevention	15,	The facility must maintain all Emorgency Response Plat training documents/prosentations, as well as training sign-in sheets or signed training chocklists Training in entergency recognition and prevention should inleade the kinds of emergencies that can occur at the satility, recognising operathis emergencies, and monitoring devices to detect emergencies	Verify follow-up records for amployous missing initial training
	Emergencies must be communicated to Corporate HSE and GBU management	15.5	Acceptable	15.5 DRC 05 (5.2)	15.5	All emergencies must be communicated to GBU and Corporate HSE management	15.	5 The facility must document communication of emergencies to GBU and Corporate HSE management via email or Manufacturing Solutions	
15.6	Emergency drills are conducted at minimum annual frequency	15.6	Acceptable	15.6	15.6		15.	6 The facility shall document and make available all drill Information	
	Emergency response equipment is maintained and easily accessible in the event of an emergency	15.7	Acceptable	15.7 PR 516 (15.2)	15.7	Maintain all emergency equipment in good working condition All emergency equipment should be located in an area that is easily accessible in the event of an emergency	15.	7 The facility shall maintain documentation of inspection and maintenance of emergency response equipment	

Emergency Response Plans

Name:	Houston	Date:	9/4/2012		,					
Element:	Compliance Audits									
Requirem	ent	Status		Аррисав	le Standards	Guide	lines	Criteri	a for Implementation	Comments
	Compliance audits to evaluate conformance to the requirements of the PIMP program are to be conducted at a minimum triennial frequency. Copies of the two most recent compliance audits are maintained onsite.	16.1	Acertable	16.1 29 PR	CFR 1910.119(o)(1) 518	16.1	An audit schedule is in place to evaluate compliance with the Process liazard Management Program This schedule is at least every three years for OSHA covered units. Maintain the two most recent compliance audits.		The facility shall maintain the audit schedule for future audits including the date of the fast audit. The facility will maintain the most recent TWO copies of the compliance audit results.	
16.2	Written compilance audit reports are written and communicated with plant management and appropriate personnel	16.2	Acceptable	16,2 29 PR	CFR 1910.119(o)(3) 518	16.7	Document all compliance audits in a report form and review with management and all affected employees		The facility shall document that all compliance audit reports are reviewed with plant management and affected employees	
16.3	All action Items and findings are discussed with plant management and all findings are documented and tracked to completion	16,3	Acceptable	16.3 29 PR	CFR 1910.119{0}{4} 518	16.5	The site management must review each audit finding and document actions that will be taken to close each finding -Treese actions must be documented in a database such as Manufacturing Solutions and tracked to completion		The facility shall provide documentation showing that all action Itoms are added to an action tracking database and that each Item Is tracked to completion	
	Audits should include reviewing previous findings and "closed" action items/findings to ensure proper completion	16.4	Needs Improvement	16.4 29 PR	CFR 1910.119(o)[5] 518	16.4	Review action items and findings from other audits, incident investigations, PHAs, MOCs, etc. to ensure that all findings are closed and that "closed" items are properly completed.		The facility shall document the review of findings and "closed" action Items in an audit report	All items not corrected from 2009 audit

Compliance Audits

: Houston	Date: 9/4/2012				
ent: Trade Secrets					
	<u> </u>				Comments
rement .	Status	Applicable Standards	Guidelines	Criteria for Implementation	Continents
17.1 Applicable information is made available to employees without regard to Trade Secrets when completing compiling Process Safety Information for review in Process Safety	17.1 Acceptable	17.1 29 CFR 1910.119(p) PR 519	Make all applicable information available for review during PRA studies, incident investigations, or any other review that could include trade secrets.		No trade secrets have been kept from employees.

Trade Secrets

lame:	Houston	Date:	9/4/2012					
lement:	Risk Management Plan	-1						Comments
equirem	ent	Status		Applicable Standards	Guide	lines	Criteria for Implementation	Commens
18.1	Determine the applicability of RMP at the facility	18.1	Acceptable	18.1 40 CFR 68.10 PR 520	18.1	Determine whether any RMP chemicals are present at the facility above the threshold quantities	18.1 Documentation that all chemicals have been reviewed for RMM applicability - Documentation should be reviewed on a regular basis	Coverage for RMP is required for the following chemical stored on site: \$03, multiple grades of oleum and liquid hazardous wastes.
	An individual has been assigned responsibility for the RMP program at the facility	18.2	Acceptable	18.2 40 CFR 68.15(b)	18.2	A person must be assigned responsibility for the RMP program that has an understanding of the regulation and its requirements	18.2 Documentation of RMP responsibilities	Organization chart for RMP responsibilities. George Garan designated as the authorized preparer of the RMP.
18.3	Program Level must be determined	18.3	Acceptable	18.3 40 CFR 68.11 PR 520	18.5	Determine Program Level using the guidelines available from the EPA (Level 1, 2, or 3)	18.3 Documentation must be maintained onsite with the determination of program levels and all supporting documentation	Lovel 3
18.4	All required RMP information must be submitted within the required timeframes	18.4	Acceptable	18.4 40 CFR 68.150 40 CFR 68.190 PR 520	18.4	The items listed below must be submitted and copies maintlaned onsite: - Submission of the initial notification of coverage under the RMP Standard - Submission/Standard - Submission/update of RMP coverage within (a) three years of a new chenical being listed by the EPA, (b) 6 months of a change requiring a new PIAs, (c) 6 months of a change requiring a new PIAs, (c) 6 months of a change requiring a feature of fisher consequence analysis where the distance increases or decreases by a fector of 2 (d) within 6 months of a change to the Program Lovel - Recertifications submitted within 5 years of the most recent submission - Emergency Response Plans submitted to LEPC and local Fix Department - Updates shall be submitted on time	required information has been submitted on time - All submitted documents must be available for review	Original submission - 8/8/2007 Updated - 6/1/2009 Plan to be updated by 12/6/12 to address ofeum release that occurred on 6/9/12
18.5	Inform surrounding community of coverage under the Risk Management Plan standard	18.5	Av-aptable	18.5 40 CFR 68.210 PR 520	18.	Maintain documentation that RMP coverage was communicated to the surrounding community	community informing them of their RMP coverage, the	Has been accomplished through original industry public relations program and is discussed in the Houston Area Citizens Advisory Panel by plant management
18.0	File applicable RMP documentation with the PUBLIC???	18.6	Acceptable	18.6 40 CFR 68.210	18.	Submit applicable RMP documentation to the FBI	18.6 The facility shall maintain documentation of the submittal to the FBI by maintaining copies of the information submitted and signed return receipts from the FBI	Original submission - 8/8/2007 Updated - 6/1/2009 Plan to be updated by 12/8/12 to address cleum release that occurred on 6/9/12
18.7	RMP covered facilities must coordinate their Emergency Response Plans with the Fire Department and the Local Emergency Planning Commission (LEPC)	18.7	Acceptable	15.7 40 CFR 68.12(b)(3) PR S2O	18.	Coordinate all emergency planning activities for the RMP covered material(s) with the LEPC and the Fire Department	Fire Department and the LEPC	On a yearly basis, the Houston plant hosts fire departmen personnel that would respond to an event in the plant. A copy of the ERP has been given to the fire department's HAZMAT station. The other fire stations will wait for the HAZMAT station, to entergencies for chemicals covered under RMP. The last fire department to under covered during the ments of 4/12. Safety Specialist attends LEPC meeting 6x per year.

Name: Houston	Date:	9/-1/2012								
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Element: General Requirements	Ц			ļi			 			
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Requirement	Status		Applic	able Standards	Guide	lines	(L)	nten	a for Implementation	Comments
19.1 THERE ARE NO OTHER GENERAL REQUIREMENTS THAT	19.1		19.1		19.1		-	19.1		
APPLY TO THE FACILITATED SELF ASSESSMENT	13.1		****							

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Blement	Total Questions	Acceptable	Naces Improvement	Umpreceptionie									
Safety File Management System	7	5	2	0									
Employee Participation	3	3	0	0									
Process Safety Information - Chemicals	7	6	1	0									
Process Safety Information - Technology	7	5	2	0									
Process Safety Information - Equipment	11	4	6	1 .									
Process Hazard Analysis (PHA)	11	8	3	0									
Standard Operating Procedures	4	1	2	1									
Training	7	4	3	0									
Contractors	7	6	1	0									
Pre-Startup Safety Review	10	5	4	1									
Management of Change (MOC)	11	9	2	0									
Mechanical Integrity	17	14	3	0									
Work Permits	3	3	0	0									
Incident Investigation	5	4	1	0									
Emergency Response Plans	7	7	0	0									
Compliance Audits	4	3	1	0									
Trade Secrets	1	1	0	0									
Risk Management Plan	7	7	0	0									
Total	129	95	31	3									

Total Score Page 28 of 28

Section III - ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
- 5. Operator Training Records
- 6. Compliance Audits
- 7. Exit Briefing Sign-In Sheet
- 8. Hot Work Permits
- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

3:00 Pm-4/24/13 *EXIT BRIEFING *

USHERRONDA PHELPS, US. EPA, REGION 6

FLOUD DEKETSON, POHODIA

CECIET BANAN PROLESS SAFETY

William Mi-Connell Plant Monager

Jim COSEH OPS MGZ

Section III – ATTACHMENTS

- 1. Process Description and corresponding Process Flow Diagrams
- 2. Current RMP Submittal
- 3. Facility Management System
- 4. Operating Procedures and Certifications
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- 9. Process Chemistry (CBI) and Maximum Intended Inventory (CBI)

Cogistics





MC#<u>//33</u> LB#_@3

BURNING - WELDING - HOT WORK PERMIT

NO BURNING, WELDING, OR OPEN FLAME WORK MAY BE PEROFRMED UNTIL THIS PERMIT HAS BEEN COMPLETED, CHECKED AND SIGNED

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UN	UNITACCATION LOGISTICS HOT 976							
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II.				YES	NO			
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2.	HAVE ALL FLA FROM THIS ARI	MMABLE MATERIAL: EA?	S BEEN REMOVED			*	· · · · · · · · · · · · · · · · · · ·	
3.	IS PURGING/FO	RCED VENTILATION	NEEDED?		2		Da 20 20 1	
4.	CONTINUOUS N	ONITORING REQUIR	ED?					
5.	HAS PROPER PP	E BEEN DISCUSSED &	k ISSUED?	D.		-44		
	(see PPE section o	on back)					SIGNED	
111.				YES	NO			
ALL WELDING / CUTTING EQUIPMENT IN GOOD CONDITION? Condition					П			
2.	2. HAS A FLAMMABILITY GAS TEST BEEN PERFORMED?					QUALIF	TED TO SIGN	
3.	3. HAVE ALL FLOOR / WALL OPENINGS & GRATINGS BEEN COVERED?						NCE SUPERVISOR OR SIGNEE	
4,	HAS FLOOR BEE NECESSARY?	EN SWEPT OR WET DO	OWN IF					
5.	AREABARRICAI	DED?) [2]			
6.	IS A FIRE WATC	H REQUIRED?				Sept.	111	
7.	7. IS FIRE EXTINGUISHER ABAILABLE AND NEAREST WATER SOURCE LOCATED?					Total 1	GNED	
8.	HAS PROPER PP	E BEEN DISCUSSED A	ND ISSUED?			<u>"</u>		
	(see PPE section or	n back)						
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Per	sonal Protective Equipment Required	(jo	int responsibility of Ope	erations & Maintenance)			
	Welding Hood		Welding Jacket	Welding Goggi S/Face shield			
	Welding Gloves		Chemical Protective Suit	Chemical Splash Hood			
	Respiratory Protection (specify type)						
			YES NO	PERCONS AUTHORIZED TO PERFORM WORK			
V.			YES NO	Cota Smallwood			
BEF	ORE USING PERMIT, READ ALL OF ABO	VE I	NFORMATION				
1.	1. HAVE ALL ASPECTS OF JOB BEEN CONSIDERED WITH SUPERVISOR?						
2.	HAS PROPER PPE BEEN DISCUSSED AT (See PPE section above)	ND IS	SUED?	FIREWATCH SIGNATURE			
	RETURN PERMIT TO THE CUSTODIAN UPON COMPLETION OF JOB FOR RETENTION When the custodian upon completion of Job For Retention						
VI.							
	BURNING – WELDING HOT WORK PERMIT						
	A FIRE WATCH IS REQUIRED WHENEVER HOT WORK IS REQUIRED ON A BARGE, TREATMENT SERVICES AREA,						
	OR WHEN FLAM	1M	ABLE MATERI	ALS HAVE NOT BEEN			
	REMO	VE	D 35 FT. FROM	THE AREA.			
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II		<i></i>	YES	NO		
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2.	HAVE ALL FLAMMABLE MATERIALS BEEN REMOFROM THIS AREA?					
3.	IS PURGING/FORCED VENTILATION NEEDED?				112	
4.	CONTINUOUS MONITORING REQUIRED?			Q	- セカラ	
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	ete.					
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2.	HAS A FLAMMABILITY GAS TEST BEEN PERFORMED!					D TO SIGN
3.	HAVE ALL FLOOR / WALL OPENINGS & GRATING BEEN COVERED?					E SUPERVISOR OR GNEE
4.	HAS FLOOR BEEN SWEPT OR WET DOWN IF NECESSARY?					
5.	AREABARRICADED?				. 11.	11
6.	IS A FIRE WATCH REQUIRED?		e /		##5.	1/1/
7.	IS FIRE EXTINGUISHER ABAILABLE AND NEARES WATER SOURCE LOCATED?	T			SIG	NED NED
8.	HAS PROPER PPE BEEN DISCUSSED AND ISSUED?		Ø	П		
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Personal Protective Equipment	nt Required (joint responsibility of Operat	ions & Maintenance)
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Welding Gloves	Chemical Protective Suit	Chemical Splash Hood
Respiratory Protection (specif	y type)	

	Respiratory Protection (specify type)			
V.		YES	NO	PERSONS ALTHORIZED TO PERFORM WORK
BEF	FORE USING PERMIT, READ ALL OF ABOVE INFORMATION	1	ζ,	ahr
1.	HAVE ALL ASPECTS OF JOB BEEN CONSIDERED WITH SUPERVISOR?			
2.	HAS PROPER PPE BEEN DISCUSSED AND ISSUED? (See PPE section above)	Ø		FIREWATCH SIGNATURE
	TURN PERMIT TO THE CUSTODIAN UPON COMPLETION JOB FOR RETENTION	Ą		KSolis
Vi.	THE AREA IN WHICH WORK WAS PERFORMED IS INSPEC CUSTODIAN, AND ACCEPTED BY THE CUSTODIAN PRIOF RELEASING MAINTENANCE FROM THE MASTER CARD.		THE	CUSTODIAN (QUERATIONS SUPERVISOR OR DESIGNEE)

BURNING – WELDING HOT WORK PERMIT

A FIRE WATCH IS REQUIRED WHENEVER HOT WORK
IS REQUIRED ON A BARGE, TREATMENT SERVICES AREA,
OR WHEN FLAMMABLE MATERIALS HAVE NOT BEEN
REMOVED 35 FT. FROM THE AREA.

RCS# 1836321

Rev. 03/28/2011

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Phodia	0	MC#LB#
NO BURNING, WELDI THIS PERMIT DATE UNIT/LOCATION TIME START TIME FINISHED (cst.) VO BURNING, WELDI THIS PERMIT THAT A C K CO TOTAL	WELDING – HOT WOI ING, OR OPEN FLAME WORK MAY BE HAS BEEN COMPLETED, CHECKED A	DEBOERATED LOCKY
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NOTE: atmosphere must be tested every 4 hours

6. IS A FIRE WATCH REQUIRED?

WATER SOURCE LOCATED?

(see PPE section on back)

TIME

IS FIRE EXTINGUISHER ABAILABLE AND NEAREST

TIME

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8. HAS PROPER PPE BEEN DISCUSSED AND ISSUED?



Рег	sonal Protective Equipment Required (joi	nt responsibility of Oper	ations & Ma	intenance)		
41)	Welding Hood]	Welding Jacket	<u>_</u>	Welning Growes Face shield		
Ð	Welding Gloves		Chemical Protective Suit		Chemical Splash Hood		
	Respiratory Protection (specify type)						
V.			YES NO	PERSON	S AUTHORIZED TO PERFORM WORK		
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BURNING – WELDING HOT WORK PERMIT							
	A FIRE WATCH I IS REQUIRED ON A OR WHEN FLAM	E	BARGE, TREAT!	MENT SI	ERVICES AREA,		
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	(see PPE section on	back)				// (- si	GNED
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ersonal Protective Equipment Require	st tioint responsibility of Opera	
		ntions & Maintenance)
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BURNING - WELDING - HOT WORK PERMIT

NO BURNING, WELDING, OR OPEN FLAME WORK MAY BE PEROFRMED UNTIL THE BERMIT HAS BEEN COMPLETED, CHECKED AND SIGNED

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3	HAVE ALL FLOO BEEN COVERED	R/WALL OPENINGS	& GRATINGS		a		E SUPERVISOR OR GNEE
4.	HAS FLOOR BEE NECESSARY?	N SWEPT OR WET DO	WN IF	- Charles	<u> </u>		
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NOTE: atmosphere must be tested every 4 hours

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REMOVED 35 FT. FROM THE AREA.

Phodia



MC# LB#

BURNING - WELDING - HOT WORK PERMIT

NO BURNING, WELDING, OR OPEN FLAME WORK MAY BE PEROFRMED UNTIL
THIS PERMIT HAS BEEN COMPLETED CHECKED AND SIGNED

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NOTE: atmosphere must be tested every 4 hours

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Per	sonal Protective Equipment Require	d (jo	int respo	isibility o	f Ope	rations & Maintenance)
Ø	Welding Hood		Welding Ja	acket		Welding Goggles/Face shield
Ø	Welding Gloves		Chemical	Protective S	ijt	Chemical Splash Hood
	Respiratory Protection (specify type)					
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		BURNIN	IG - WELDING	G - HO'	T WOR	K PERMIT	
			WELDING, OR OPEN FL				
1.		THIS P	ERMIT HAS BEEN COM	IPLETED, C	HECKED AN	ND SIGNED	7.4
D/	TE 3-6	3-1					
UN	IT/LOCATION	2000	6) 3	00 6	PR		
	ME START	3	-000			QUALI	FIED TO SIGN
	ME FINISHED (est.)					☐ CUSTOI	DIAN (OPERATIONS
	UIPMENT TO BE WO	RKED ON:	San ba			SUPERVIS	OR OR DESIGNEE)
	ORK TO BE DONE	2.1.	Ace a	^		RHODIA	REPRESENTATIVE
.,	Han	500	444				
-		- 14					
11.				YES	NO		
1.	SPRINKLER PROTE	CTION IN SERV	TCE?		0		
2.	HAVE ALL FLAMM FROM THIS AREA?	ABLE MATERIA	ALS BEEN REMOVED				1
3.	IS PURGING/FORCE	ED VENTILATIO	N NEEDED?				/ _
4.	CONTINUOUS MON	ITORING REQU	JIRED?		0		11
5.	HAS PROPER PPE B	EEN DISCUSSE	D & ISSUED?			france	
	(see PPE section on ba	ack)					SIGNED
III.	1976			YES	NO		
1.	ALL WELDING / CU CONDITION?	TTING EQUIPM	ENT IN GOOD		П "		
2.	HAS A FLAMMABII PERFORMED?	LITY GAS TEST	BEEN				FIED TO SIGN
3.	HAVE ALL FLOOR A	WALL OPENIN	GS & GRATINGS				NCE SUPERVISOR OR ESIGNEE
4.	HAS FLOOR BEEN S	SWEPT OR WET	DOWN IF	-		No. of	
	NECESSARY?		30 ST		П	4	
5.	AREABARRICADEL)?				1.15	
6.	IS A FIRE WATCH R	EQUIRED?				1	111
7.	IS FIRE EXTINGUIS WATER SOURCE LO		E AND NEAREST			252	IGNED
8.	HAS PROPER PPE B	EEN DISCUSSEI	D AND ISSUED?				
	(see PPE section on ba						
B/			70.0			-	
1V.	JUAT	Z:4	TIME		ПМЕ	TIME	TIME
	RESULTS	RESULTS	RESULTS	nr.	SULTS	RESULTS	RESULTS
0.4	20. 7	2018	O ₂ :	O ₂ :		O ₂ :	O ₂ :
LEI		EL:	LEL:	LEL:		/2	1
A STATE	100	1770	_ LLL.	LEL:		LEL:	_ LEL:
-	INITIALS	INMALS	INITIALS	IN	ITIALS	INITIALS	INITIALS



	Welding Hood	□ Wo	elding Jacket	Welding Goggles/Face shield
	Welding Gloves	☐ Ch	nemical Protective Suit	Chemical Splash Hood
]	Respiratory Protection (specify type			
			YES NO	PERSONS AUTHORIZED TO PERFORM WORK
			4	Nott Photes
EF	ORE USING PERMIT, READ ALL O	F ABOVE INFO	RMATION	*
	HAVE ALL ASPECTS OF JOB BEE SUPERVISOR?	N CONSIDERED	O WITH	oil Lhanck
	HAS PROPER PPE BEEN DISCUSS (See PPE section above)	ED AND ISSUEL	0?	Mattilares
	URN PERMIT TO THE CUSTODI. IOB FOR RETENTION	AN UPON COM	PLETION	# Firewarch Signature
	V.			
	THE AREA IN WHICH WORK WAS CUSTODIAN, AND ACCEPTED BY RELEASING MAINTENANCE FRO	THE CUSTODIA	AN PRIOR TO	CUSTODIAN (OPERATIONS SUPERVISOR OR DESIGNIE)
				Designuss
			G – WEL ORK PEI	DING
	НО	TW	ORK PEI	DING
	HO	T WO	ORK PEI	DING RMIT EVER HOT WORK
	HO A FIRE WATC	T WO	ORK PEI Quired whene ge, treatmen	DING

Rev. 03/28/2011

Reg II





MC# N/A

	# F	BURNI	NG – WELDII	NG HO	TWO		LB#/N
		NO BURNING	, WELDING, OR OPEN PERMIT HAS BEEN CO	FLAME WOL	RK MAY BE	PEROFRMED UNIT	
U TI TI E(NIT/LOCATION ME START _ T ME FINISHED (Regan Regan 100 est.) 100 BE WORKED ON:	TI 93 PT hale or		+1	OUAT CUSTO SUPERVI	LIFIED TO SIGN DDIAN (OPERATIONS SOR OR DESIGNEE) A REPRESENTATIVE
1. 2. 3. 4. 5.	HAVE ALL FI FROM THIS A IS PURGING/I CONTINUOUS	AREA? FORCED VENTILATION S MONITORING REQU PPE BEEN DISCUSSE	ALS BEEN REMOVED ON NEEDED? JIRED?				SIGNED
1. 2. 3. 4. 4. 5. 66. 77.	HAS A FLAMM PERFORMED? HAVE ALL FL BEEN COVERI HAS FLOOR B NECESSARY? AREABARRIC. IS A FIRE WAT IS FIRE EXTIN WATER SOURCE	OOR / WALL OPENIN ED? EEN SWEPT OR WET ADED? TCH REQUIRED? GUISHER ABAILABL CE LOCATED? PPE BEEN DISCUSSED	BEEN GS & GRATINGS DOWN IF E AND NEAREST	VES d	NO C	MAINTEN, D	FIED TO SIGN ANCE SUPERVISOR OR ESIGNEE
\$	RESULTS	1:06	RESULTS		IME	TIME	TIME
EL:	D.9 N INITIALS	O ₂ : 2 1 LEL: Nimals	O ₂ :	O ₂ :		RESULTS O2: LEL:	RESULTS O ₂ : LEL: INITIALS



	☐ Welding Jacket	Welding Goggles/Face shield
☐ Welding Glovés	☐ Chemical Protective Suit	Chemical Splash Hood
Respiratory Protection (specify type)		De la contraction de la contra
ν,	YES NO	
	YES NO	PERSONS AUTHORIZED TO PERFORM WORK
BEFORE USING PERMIT, READ ALL OF	ABOVE INFORMATION	All Talles
HAVE ALL ASPECTS OF JOB BEEN	/ /*	may correctly.
SUPERVISOR?	CONSIDERED WITH	
BAS PROPER PRE DEEM DISCUSSION		77. data and a second s
HAS PROPER PPE BEEN DISCUSSED (See PPE section above)	AND ISSUED?	
ETURN PERMIT TO THE CUSTODIAN	IPON COMPLETION	FIREWATCH SIGNATURE
F JOB FOR RETENTION	OT ON COMPLETION	I low frielle
THE AREA IN WHICH WORK WAS PE	ERFORMED IS INSPECTED BY THE	
CUSTODIAN, AND ACCEPTED BY TH RELEASING MAINTENANCE FROM T	IECTETOOMAN no ton mo i A	M CROW
		CUSTODIAN (OPERATIONS SUPERVISOR OR
		DESIGN(E)
*		
RIID	ALBIA ALIBIA	TAXXXX
BURI	NING - WEL	DING
	5	
	NING – WEL ' WORK PER	
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НОТ	WORK PER	RMIT
НОТ	WORK PER	RMIT
HOT	5	EMIT VER HOT WORK

REMOVED 35 FT. FROM THE AREA.

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ResII

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# 1	1 11 ((11 (



MC# NA

	IOUIU					LB#_
	BURNII	NG - WELD	ING – HO	OT WO	RK PERMIT	,
	NO BURNING,		N FLAME WO	RK MAV D	E DEDOEDMED INT	
II. 1. SPRINKLER I 2. HAVE ALL FI FROM THIS A 3. IS PURGING/I 4. CONTINUOUS	R.2 Scr D700 est) 1900 BE WORKED ON: TO NE LELL RED PROTECTION IN SERV	LIS BEEN REMOVE IN NEEDED?	YES 0	NO DO DO	QUAI	LIFIED TO SIGN DDIAN (OPERATIONS SOR OR DESIGNEE) A REPRESENTATIVE
(see PPE section		0 & ISSUED?	A			SIGNED
2. HAS A FLAMM PERFORMED? 3. HAVE ALL FLO BEEN COVERE	OOR / WALL OPENING	EEN S & GRATINGS	YES D D S	NO	☐ MAINTENA	FIED TO SIGN NCE SUPERVISOR OR ESIGNEE
IS FIRE EXTING WATER SOURC	CH REQUIRED? GUISHER ABAILABLE EE LOCATED? PE BEEN DISCUSSED /		E E		Sus V	OS 7 US GNED LUIS AMADOR
UBOO	TIME	TIME	TII	ME	TIME	TIME
RESULTS 29	RESULTS O ₂ :	RESULTS O ₂ :	RESU O ₂ :	JLTS	RESULTS O ₂ :	RESULTS O ₂ :
CH CH	LEL:	LEL:	_ LEL:		LEL:	LEL:



Personal Protective Equipment Welding Hood	_		P		
Welding Gloves		Welding Jacket Chemical Protective	e s		Welding Goggles/Face shield
Respiratory Protection (specify		Chemical Projective	Suit		Chemical Splash Hood
· ·		YES	NO	PERSONS	AUTHORIZED TO PERFORM WORK
					a Thomas
BEFORE USING PERMIT, READ A	.I. OF ABOVE IN	FORMATION		1 , .	andre
. HAVE ALL ASPECTS OF JOB SUPERVISOR?	BEEN CONSIDE	TED WITH			
HAS PROPER PPE BEEN DISC (See PPE section above)	USSED AND ISS	JED?			
ETURN PERMIT TO THE CUSTO F JOB FOR RETENTION	DDIAN UPON CO	OMPLETION		FI	REWATCH SIGNATURE
THE AREA IN WHICH WORK V CUSTODIAN, AND ACCEPTED RELEASING MAINTENANCE F	BY THE CUSTO	DE GOLDD TO		CUSTODIAN	OPERATIONS SUPERVISOR OR DESIGNEE)
BU	RNI	VG - V	Æ	LDIN	G
H	OT W	ORK :	PE	RMI'	
A FIRE WAT	CH IS RE	QUIRED W	HEN	IEVER H	OT WORK
IS REQUIRED (
OR WHEN FI					
					AOT REEM
RE	MOVED 3	5 FT. FROM	A TH	E AREA.	